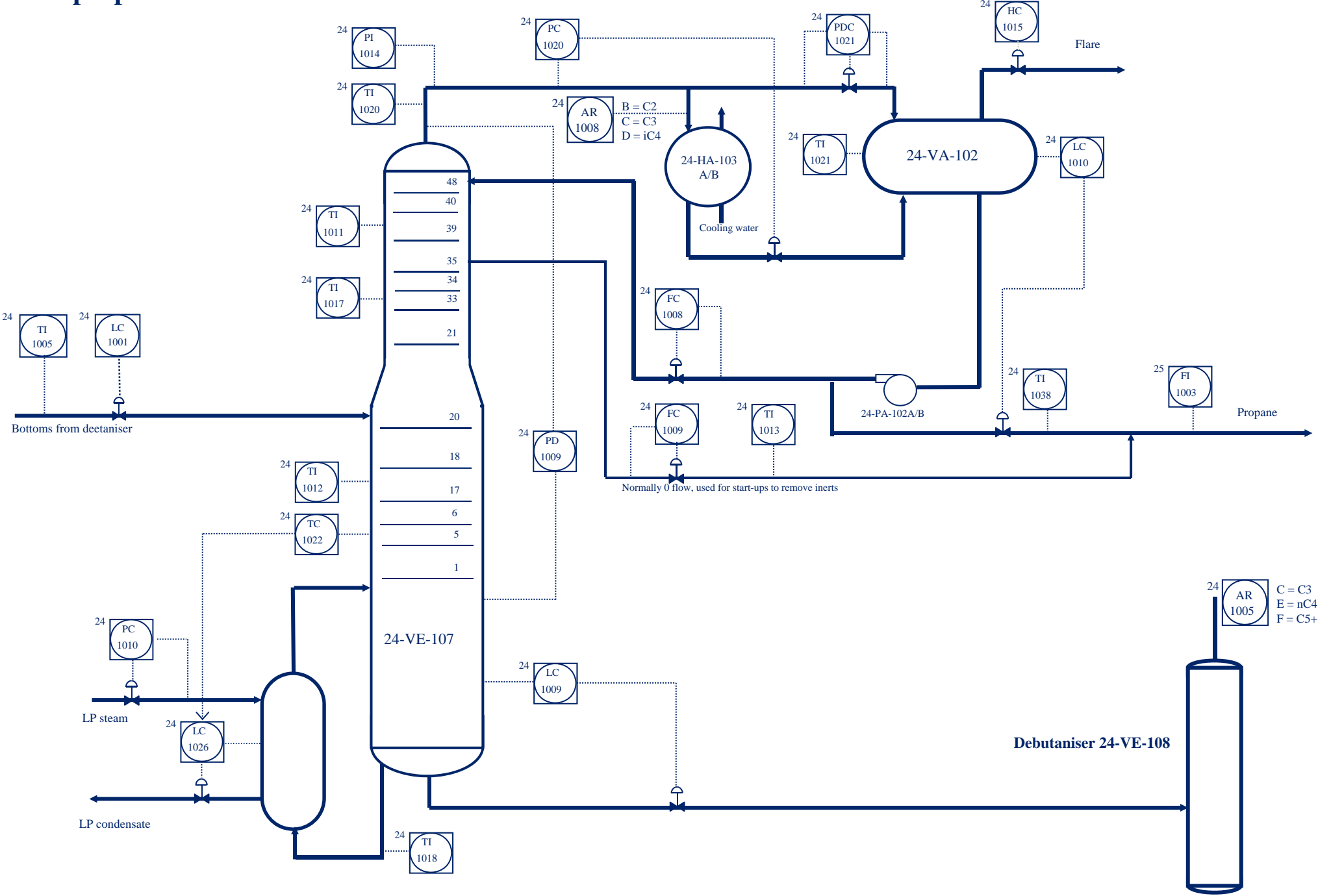


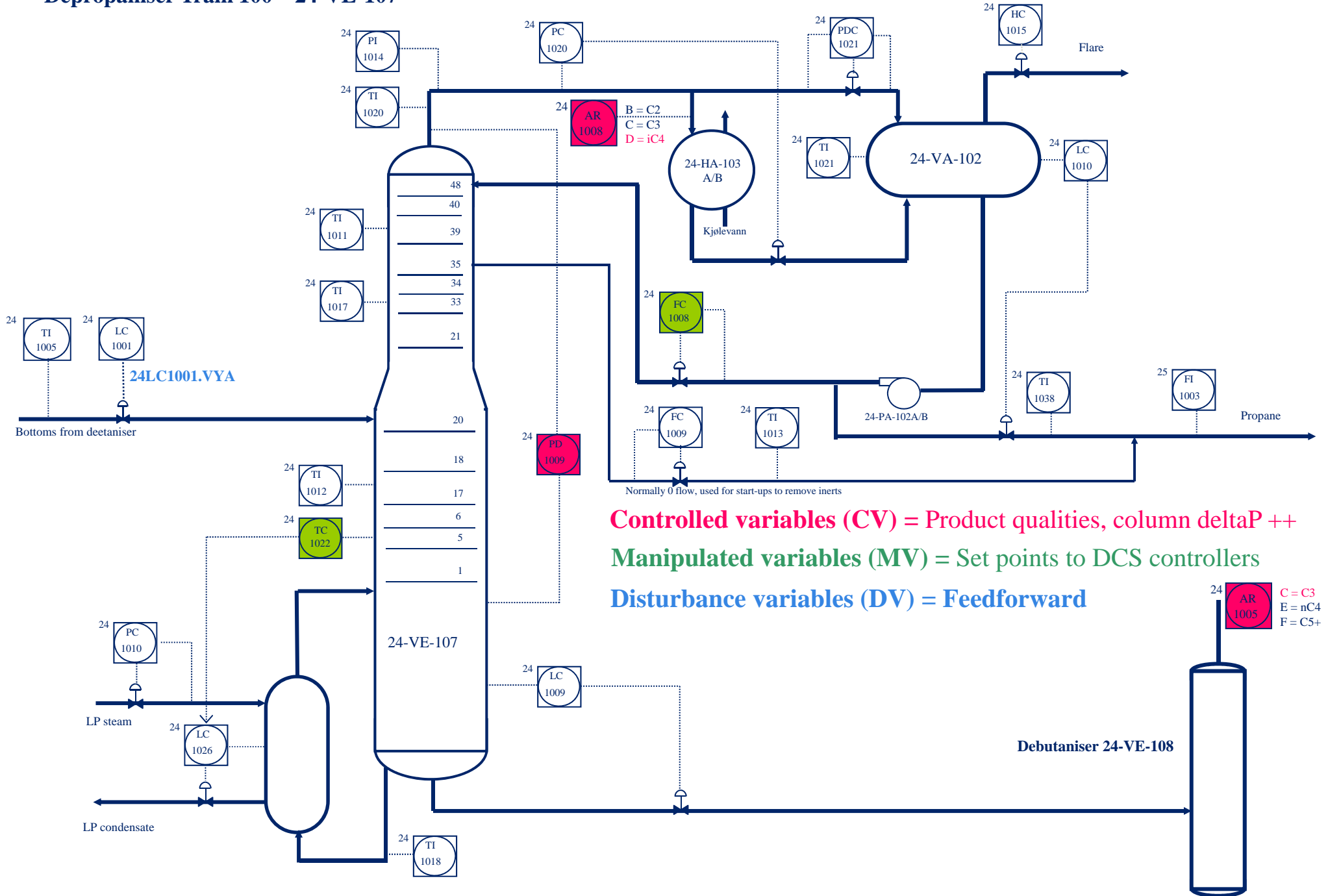
Depropaniser Train 100 – 24-VE-107



AR 1008
 B = C2
 C = C3
 D = iC4

AR 1005
 C = C3
 E = nC4
 F = C5+

Depropaniser Train 100 – 24-VE-107

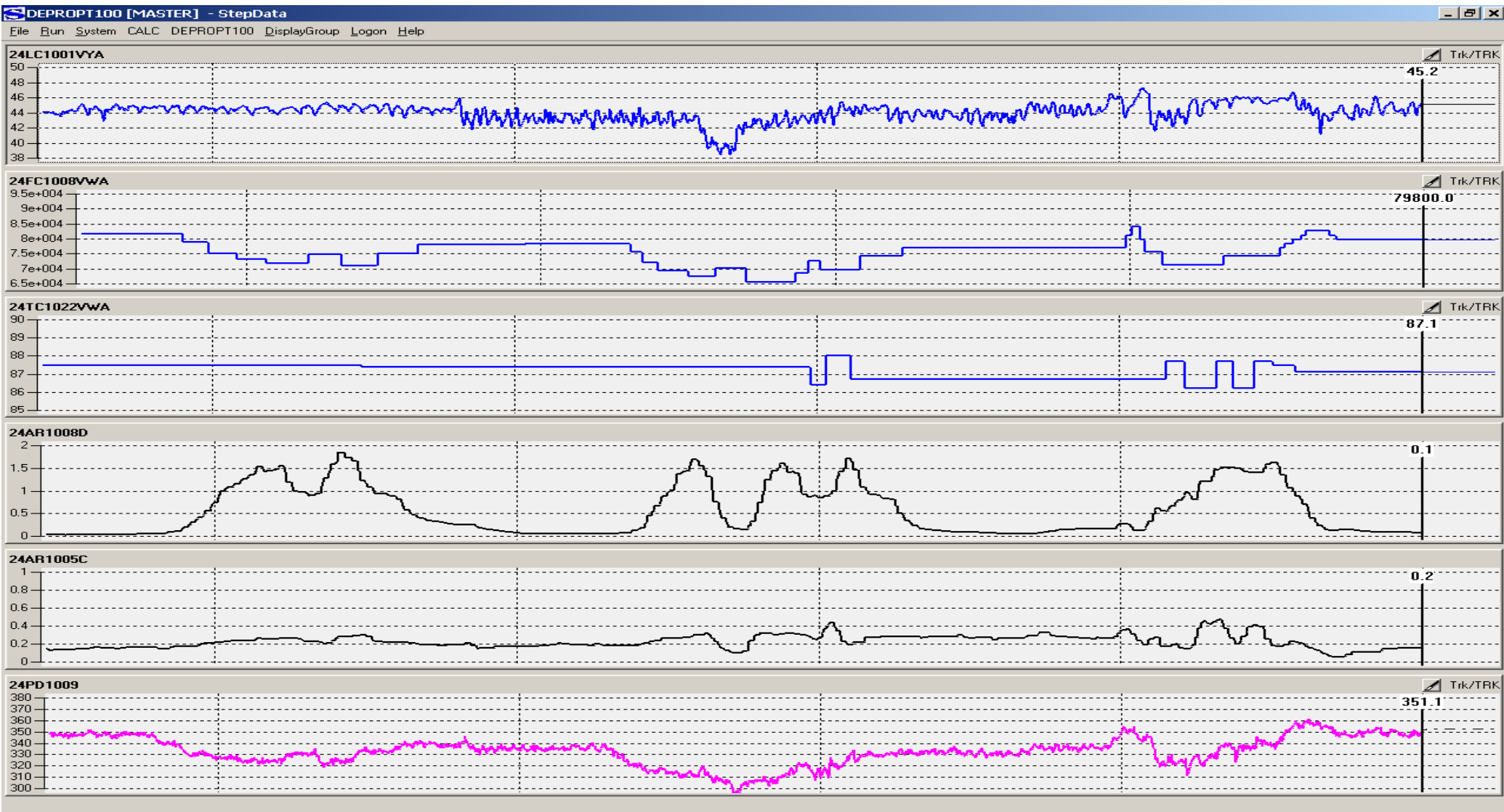


Controlled variables (CV) = Product qualities, column deltaP ++
Manipulated variables (MV) = Set points to DCS controllers
Disturbance variables (DV) = Feedforward

C = C3
 E = nC4
 F = C5+

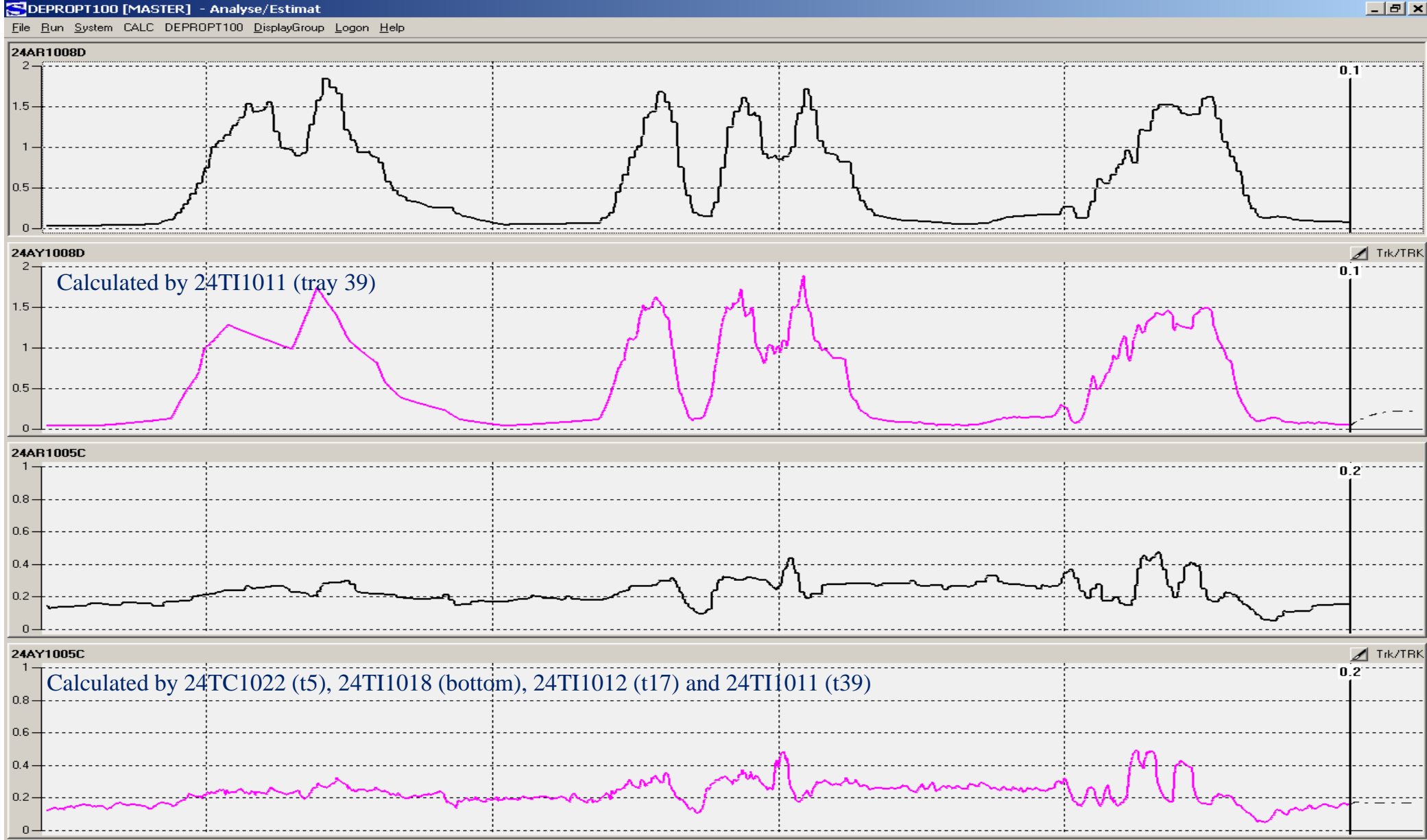
Depropaniser Train100 step testing

- 3 days – normal operation during night
- Analyser responses are delayed – temperature measurements respond 20 min earlier



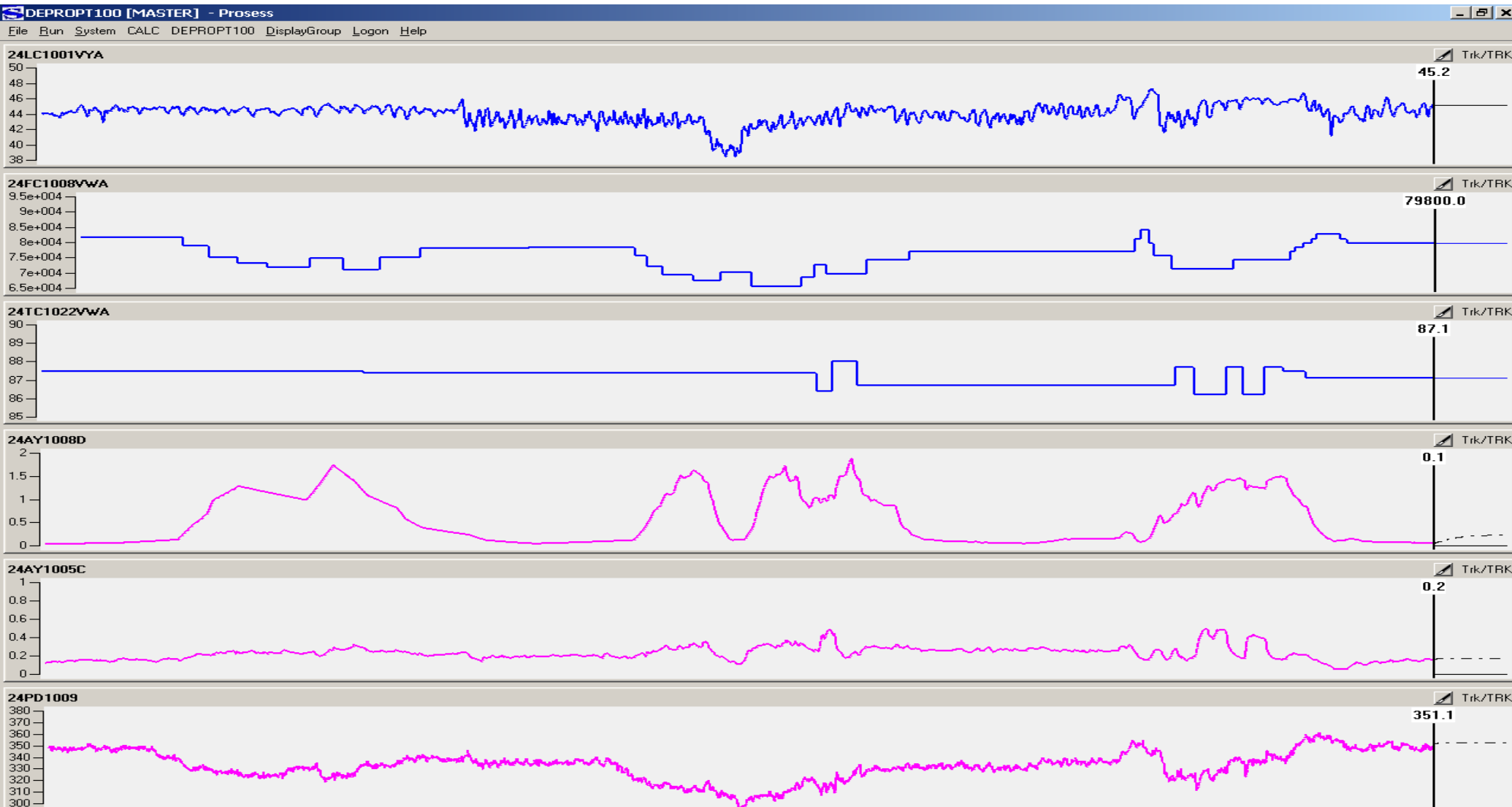
Depropaniser Train100 step testing – inferential models

- Combined process measurements → predicts product qualities well



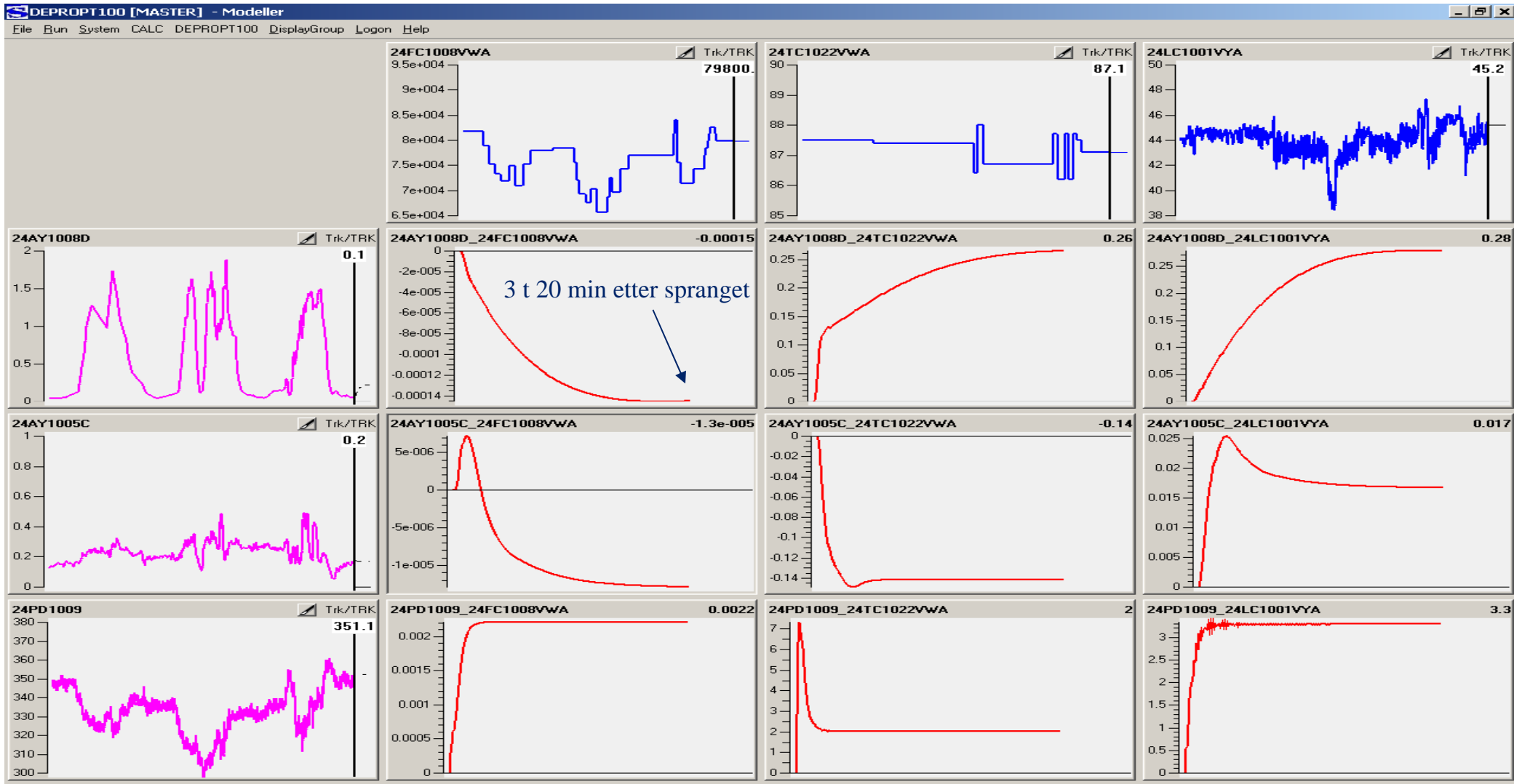
Depropaniser Train100 step testing – CV choice

- Product quality predictors, with slow corrections from analyser
 - Can control even if the analyser is out of service, automatic analyser fault detection
 - Removes a 20 min feedback delay



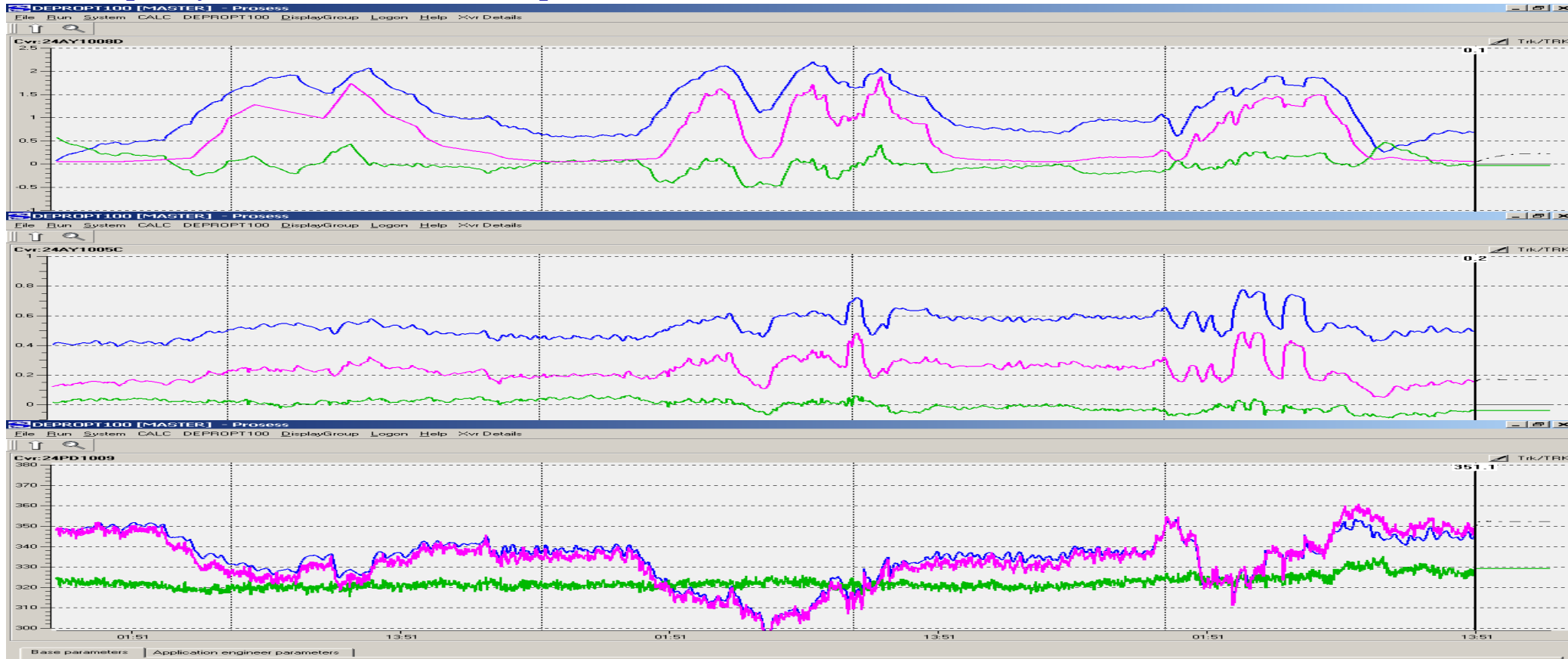
Depropaniser Train100 step testing – Dynamic responses/models

- The dynamic models (red) are step responses, made from step-test data
 - Models from 24FC1008VWA show the 3 CV responses to a reflux set point increase of 1 kg/h
 - Models from 24TC1022VWA show the CV responses to a temperature set point increase of 1 degree C
 - Models from 24LC1001VYA (DV) show the CV responses to an output increase of 1%.



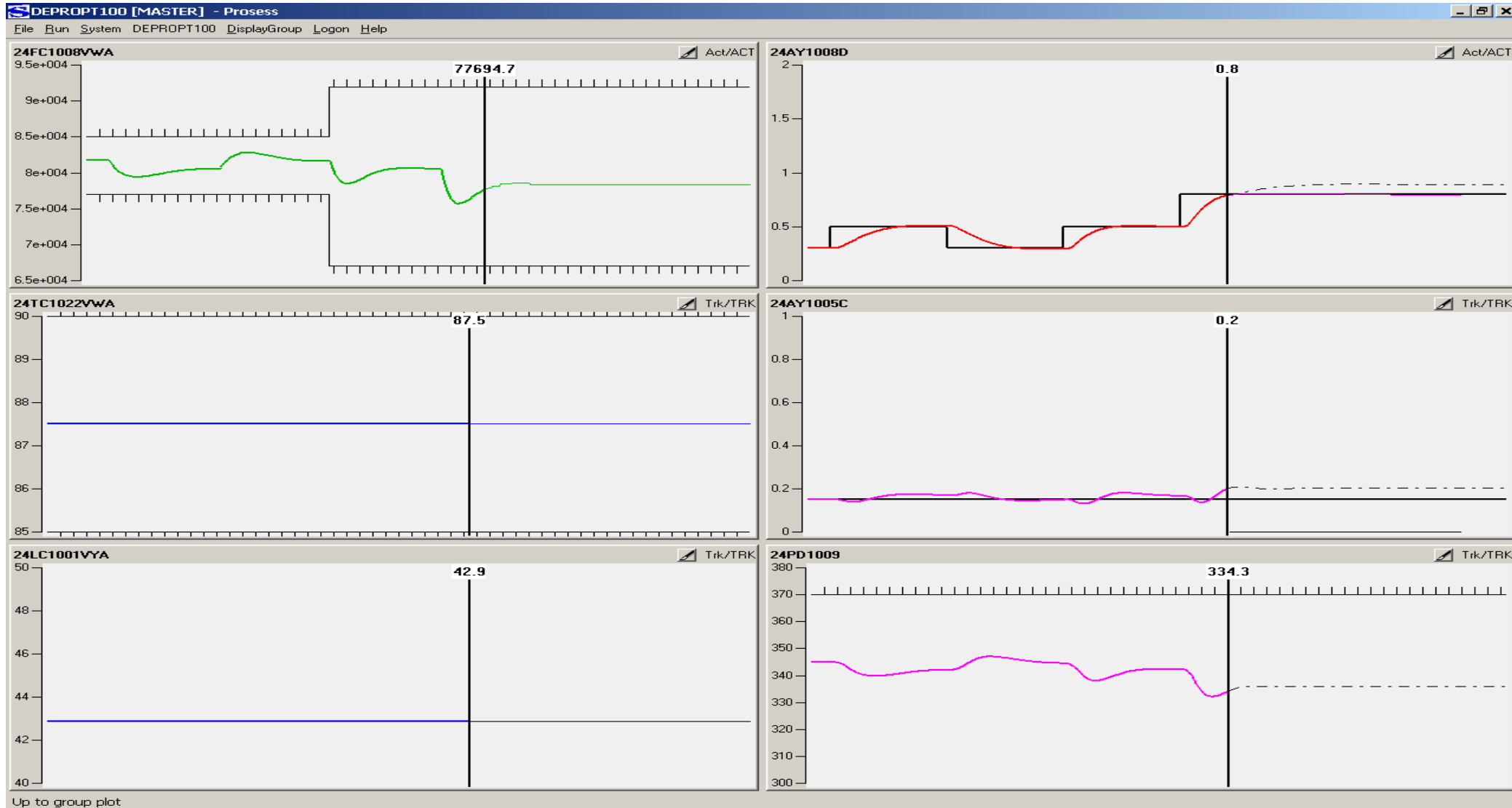
Depropaniser Train100 step testing – Dynamic responses/models

- Match between measured CV's (pink) and modelled step responses (blue) fairly good, green is model error.
 - Assumed linear responses, i.e. a reflux change of 1 kg/h gives the same product quality response whether the impurity is 0.1% or 2%. This is not correct, and the application will use logarithmic product quality transformations to compensate for the nonlinearities.



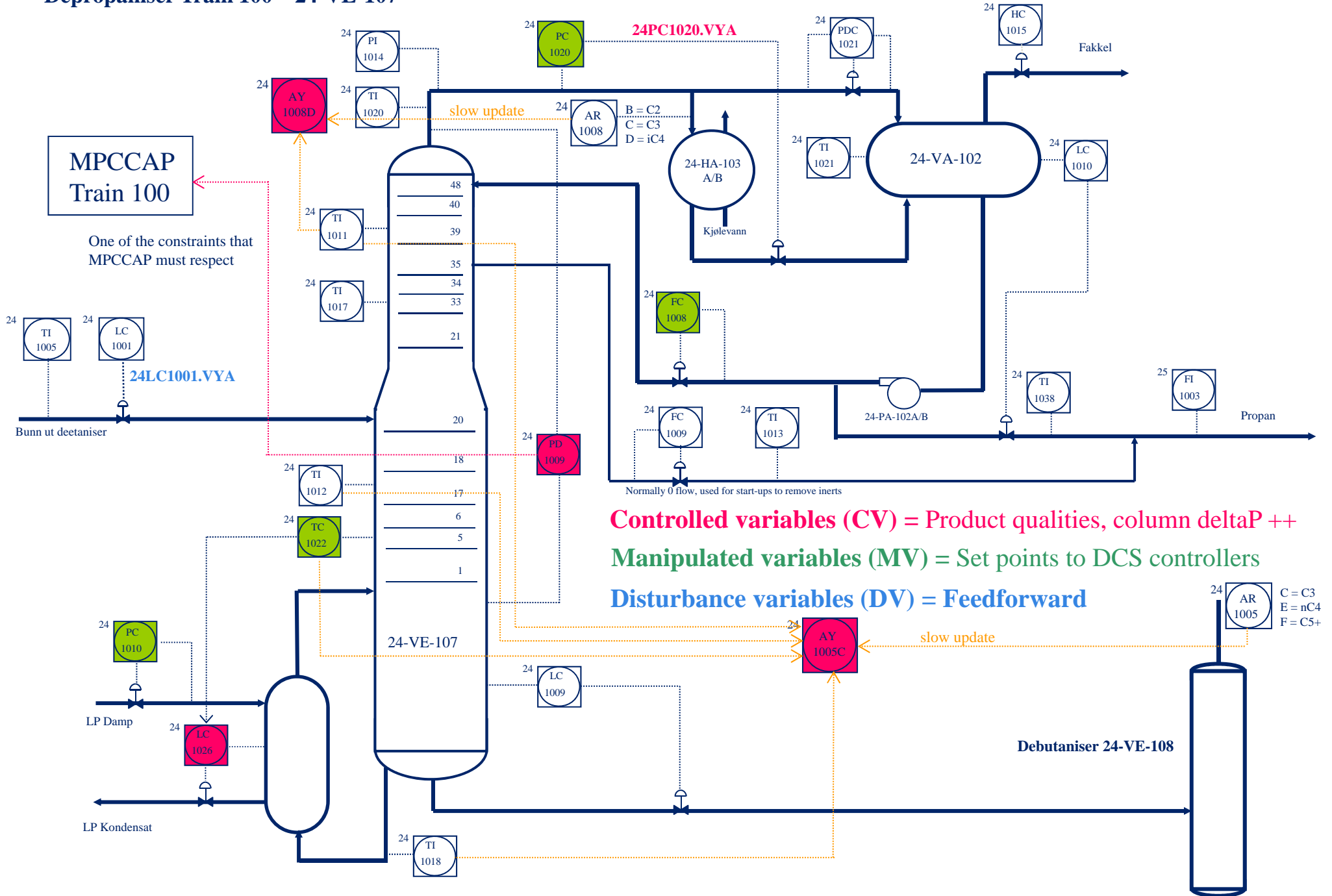
Depropaniser Train100 MPC – controller activation

- Starts with 1 MV and 1 CV – CV set point changes, controller tuning, model verification and corrections
- Shifts to another MV/CV pair, same procedure
- Interactions verified – controls 2x2 system (2 MV + 2 CV)
- Expects 3 – 5 days tuning with set point changes to achieve satisfactory performance



Depropaniser Train100 MPC – further development

- Commissions product quality control January 2004, i.e. MPC manipulates reflux and tray 5 temperature SP to control top and bottoms product quality.
- Product quality predictors will be evaluated and recalibrated if necessary.
- If boil-up constraints:
 - **MV**: steam pressure SP 24PC1010.VWA, **CV**: boiler level SP 24LC1026.VWA with high/low limits.
- If limited LP steam (plant-wide):
 - Specify max acceptable impurity in both ends (CV SP) (10-15% reduced steam consumption)
 - Marginal: **MV**: column pressure (24PC1020.VWA), **CV**: pressure controller output (24PC1020.VYA) with high/low limits. Low MV ideal value that decreases pressure against output limitation (1-3% reduced steam consumption)
- If Train 100 capacity test gives column flooding:
 - **CV**: column differential pressure, with high limit.
 - Specify max acceptable impurity in both ends (10-15% increased capacity compared to normal product purity)
 - Adjust feed flow (by adjusting Train 100 feed) against differential pressure high limit (see below)
- 2005/2006: Capacity control for Train 100 to push feed continuously against one or more processing constraints.
- Resources for continuous MPC maintenance important



MPCCAP
Train 100

One of the constraints that
MPCCAP must respect

Controlled variables (CV) = Product qualities, column deltaP ++
Manipulated variables (MV) = Set points to DCS controllers
Disturbance variables (DV) = Feedforward

C = C3
E = nC4
F = C5+