

PROMATCH

Model Reduction for Large Scale Dynamical Systems: Glass as an application

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Where innovation starts

Outline

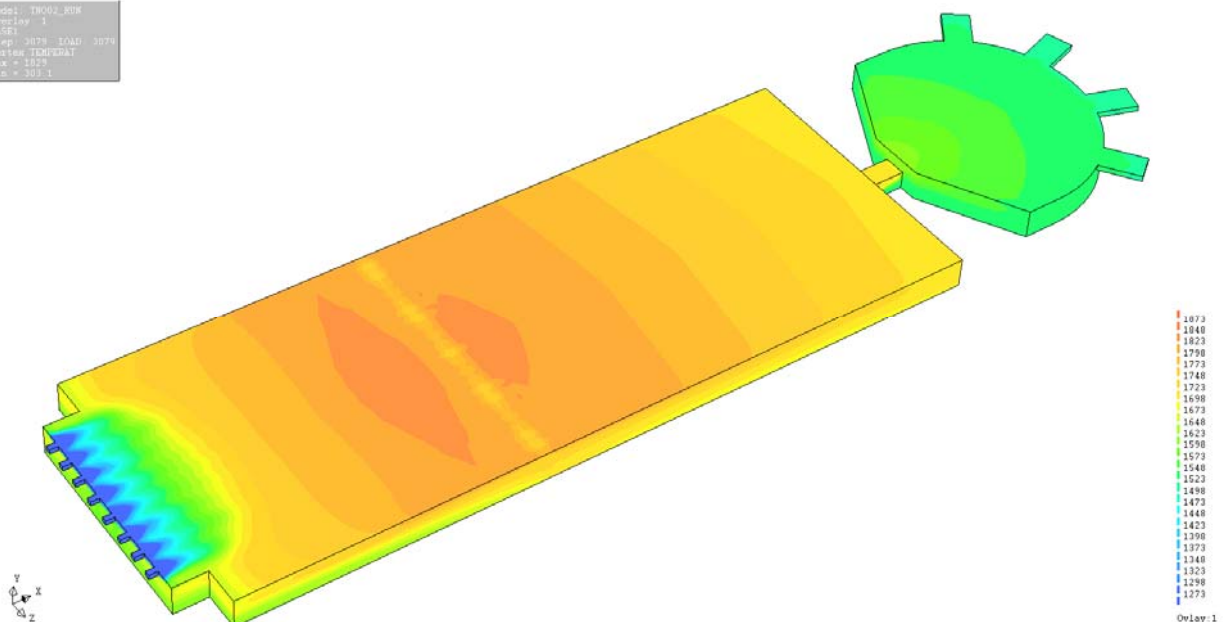
- **Motivation**
- **Glass Manufacturing**
- **Parameter Uncertainty: Corrosion**
- **Problem Formulation**
- **Model Reduction – Strategy 1**
- **Model Reduction – Strategy 2**
- **Results**
- **Conclusion**

Motivation

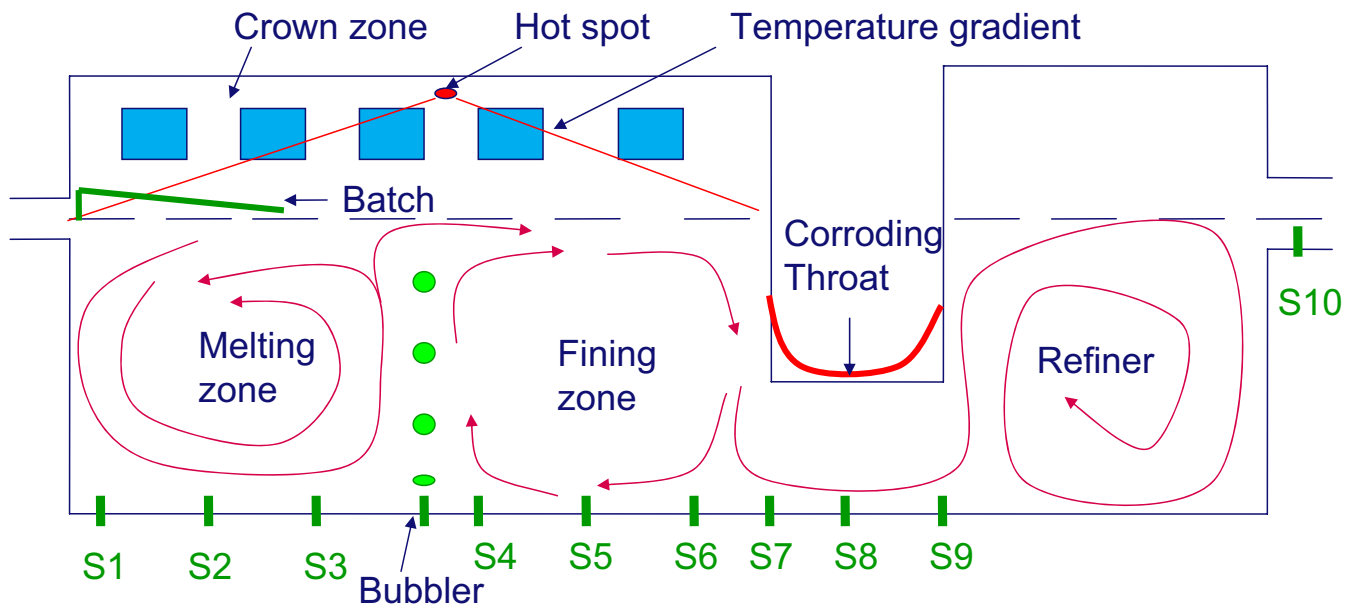
- Large Scale Systems (order $\sim 10^6$)
- Non-linear, multiphase-reactive fluid flow with parametric uncertainties
- Governed by Non-linear Navier-Stoke equations
- Modeled by Computational Fluid Dynamics (CFD) tools
- Need for computationally efficient models capturing process uncertainties

Application: Glass Manufacturing

```
Model: TMO01_R00K  
Display: 1  
CASE: 1  
Step: 3079 (LOAD_3079)  
Version: TMO01_R00K1  
Max = 1079  
Min = 303.1
```



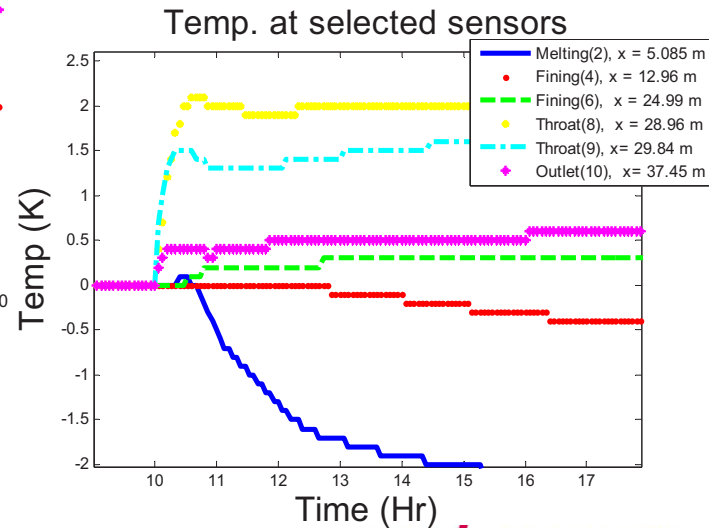
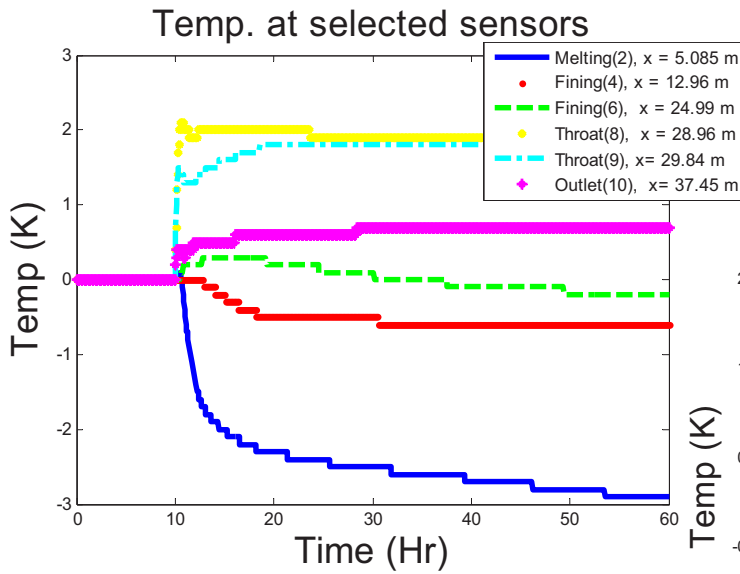
Benchmark: 2d Glass Tank



Characteristic Process Properties

- **Residence Time distribution (RTD) characterised as series combination of PFR and CSTR**
- **Time scale observations:**
RTD response to glass pull rate/Color. change is 10-20 times slower than to changes in temperature (20 hr to days vs. 1/2hr to 2hr)
- **Each process phase is heterogeneous**
- **Residence time, temperature, pull/production rate, flow pattern, glass properties have interacting effects**
- **Inputs: Heat supply, stirring, bubbling, pressure, pull rate**
- **Disturbances: batch amount and composition**
- **Control variables: Temperature, Pressure, Flow**
- **Constrains: Variation in flow, Stability, Heat input**

Glass response to step change

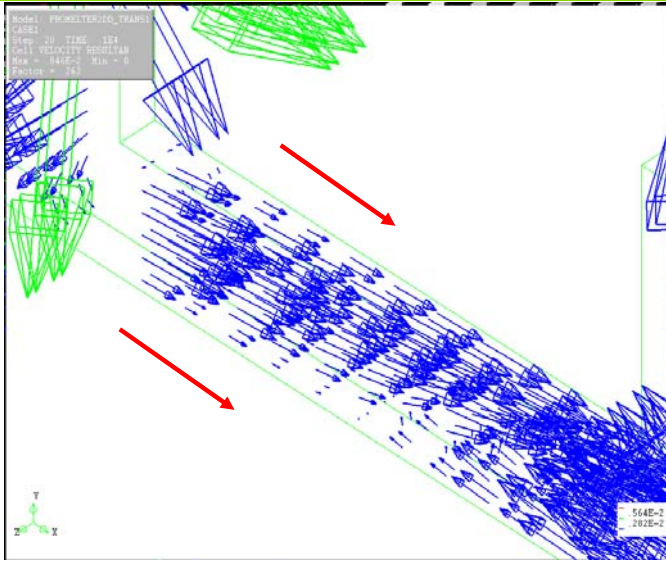


Some more challenges...

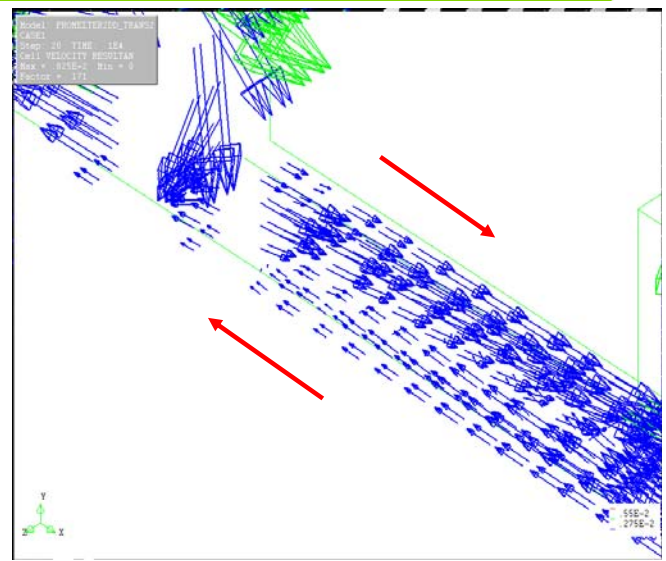
Industrial interest (**SCHOTT AG**) includes capturing uncertain phenomena in model reduction framework like:

- Parameter varying phenomena (corrosion)
- Changing material properties (batch composition)
- Reaction kinetics at micro level
- Radiation effects

Corrosion: Occurrence of back-flow



Below critical value (h^-)

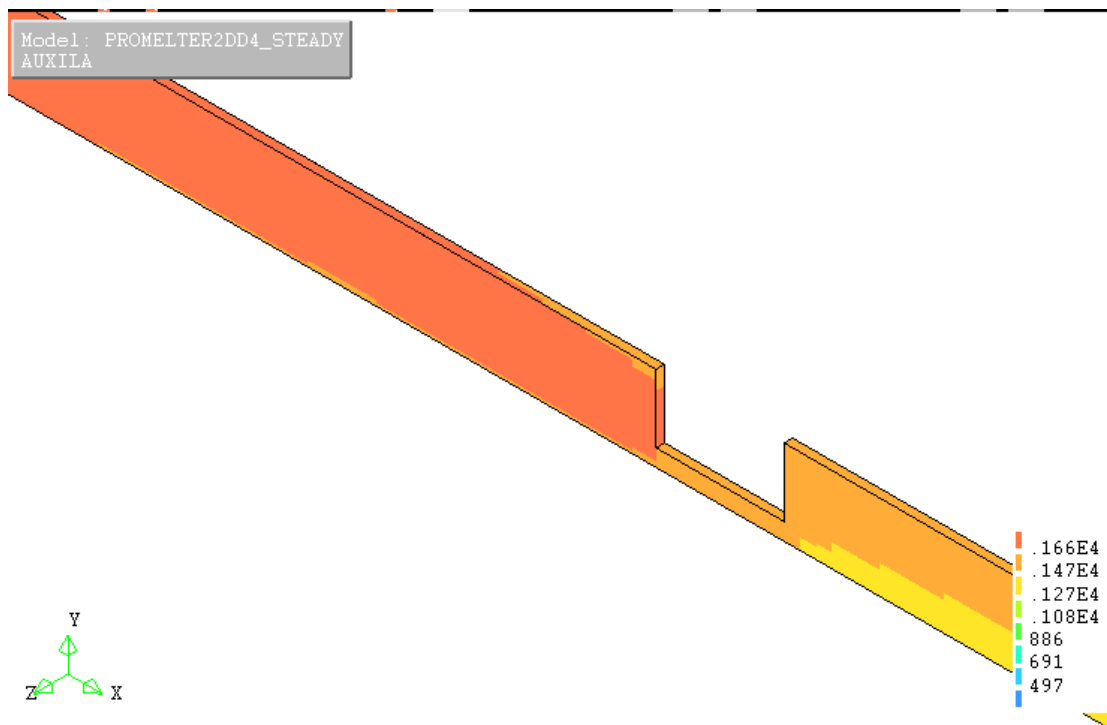


Above critical value (h^+)

Bifurcation parameter window

$$h^- < h^* < h^+ = 0.2\text{m} < h^* < 0.3\text{m}$$

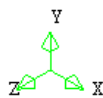
Temperature: No Corrosion, no back-flow



Temperature: With Corrosion, and back-flow

```

Model: PROMELTER2DD_STED1
CASE1
Step: 3467  LOAD: .347E4
Cell TEMPERAT
Max = 185E4  Min = 303
    
```



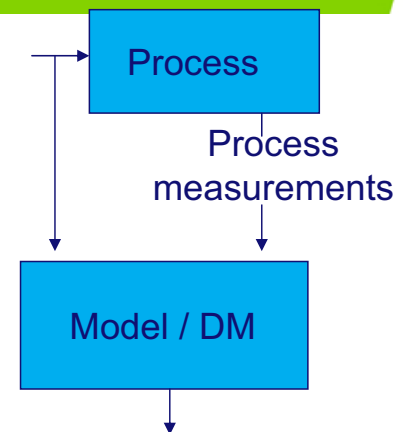
.166E4
 .147E4
 .127E4
 .108E4
 885
 691
 497

Problem statement

For any of the following systems-

$$\begin{aligned}
 &\sum_{h_1} : f(x, y, z, T, Velocity, \dots, h = h_1) \\
 &\sum_{h_2} : f(x, y, z, T, Velocity, \dots, h = h_2) \\
 &\sum_{h_3} : f(x, y, z, T, Velocity, \dots, h = h_3) \\
 &\dots \\
 &\dots \\
 &\sum_{h_n} : f(x, y, z, T, Velocity, \dots, h = h_n)
 \end{aligned}$$

Operating conditions



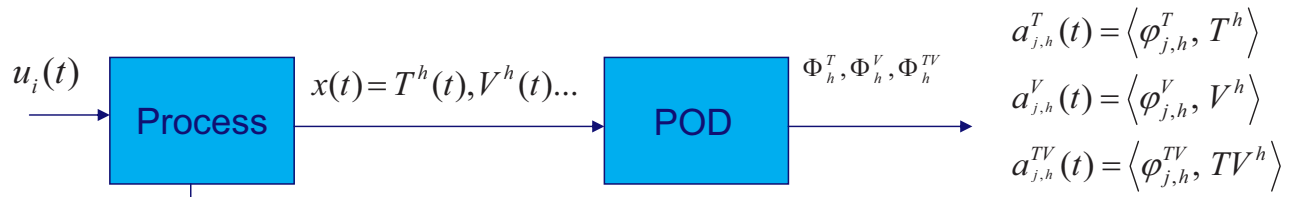
Faster model capturing uncertainty!!

Q: Given few measurements and some system knowledge, can one find a reliable computationally efficient model under the influence of corrosion ?

A: Full Model (CFD) + Model Reduction (POD) + System Identification + Dynamic Detection Mechanism/LPV approximation

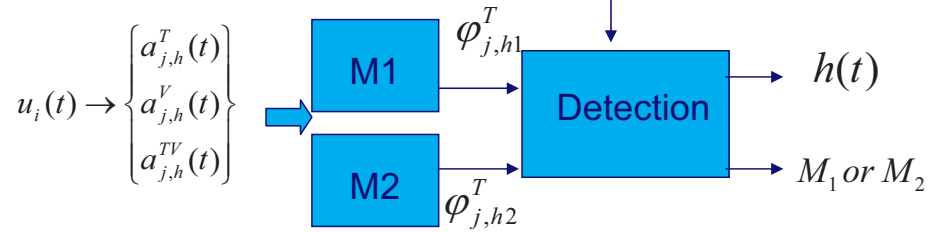
Model Reduction Strategy – 1, Hybrid Detection

- Step 1 (for $h_1=0.2, h_2=0.3$)

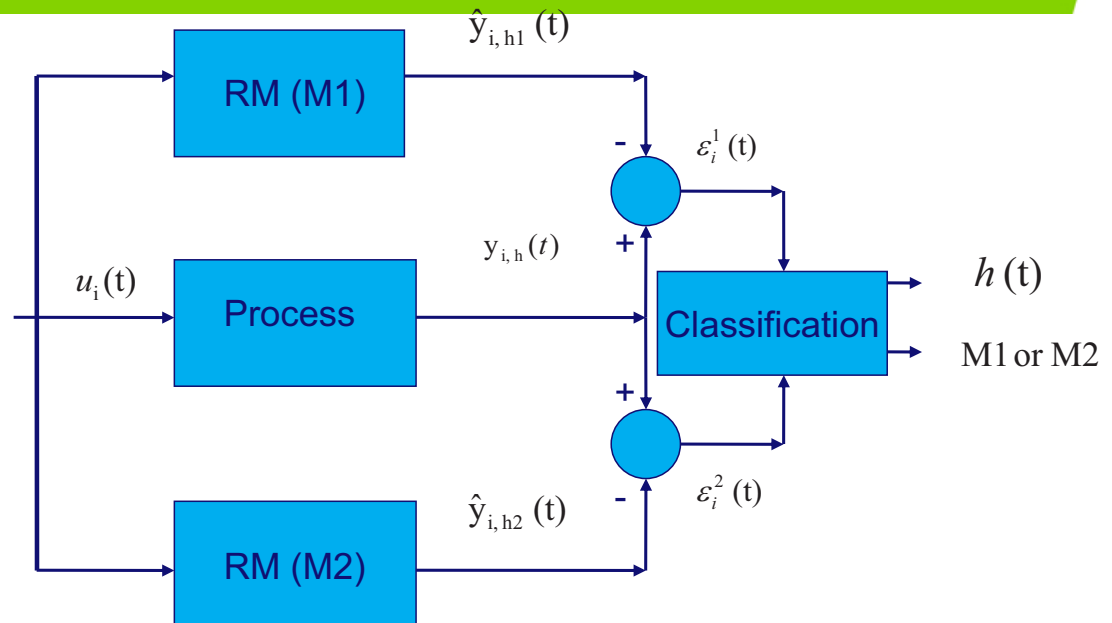


- Step 2 :

$$y_i^T(t, h), y_i^V(t, h)$$



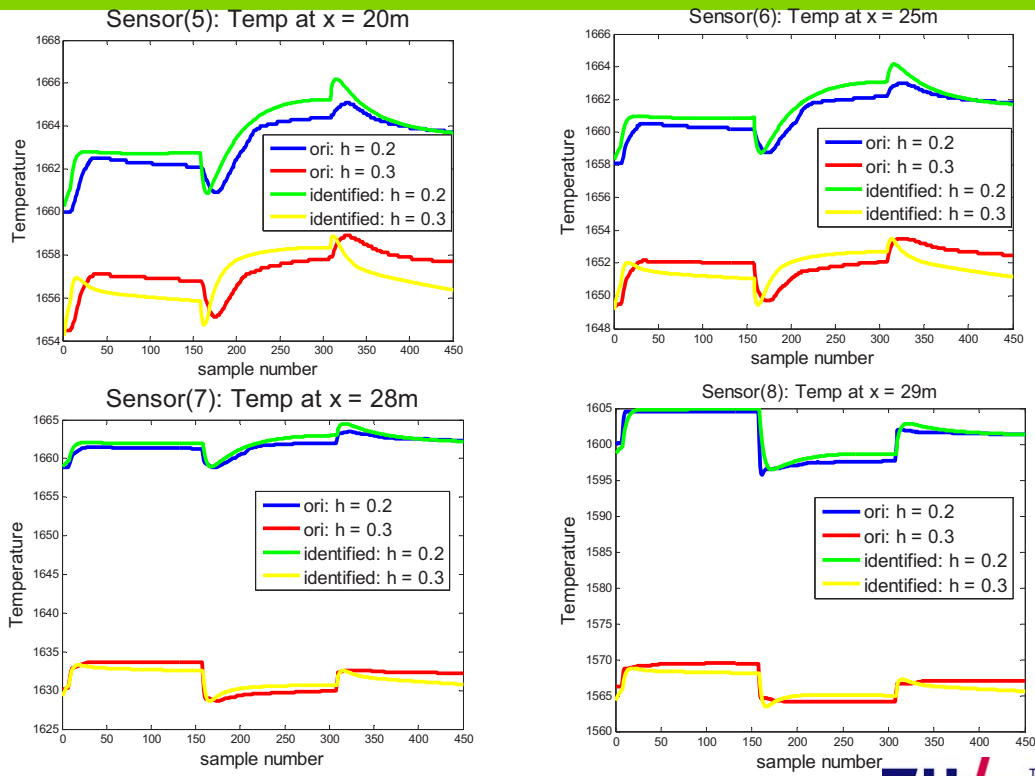
Detection Mechanism



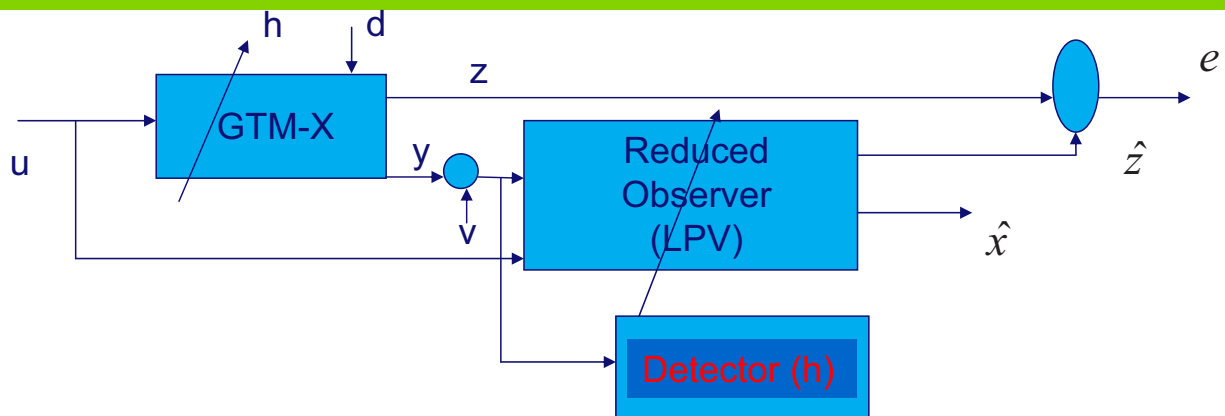
Assumption : Process bifurcation parameter is above or below critical value.

Disadvantage: For small difference and substantial noise presence can lead to wrong result.

Results: Strategy 1, Detection



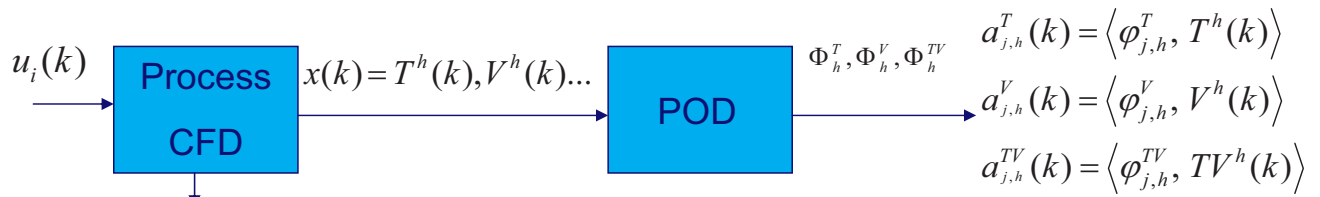
Strategy 2: LPV SID model/Observer



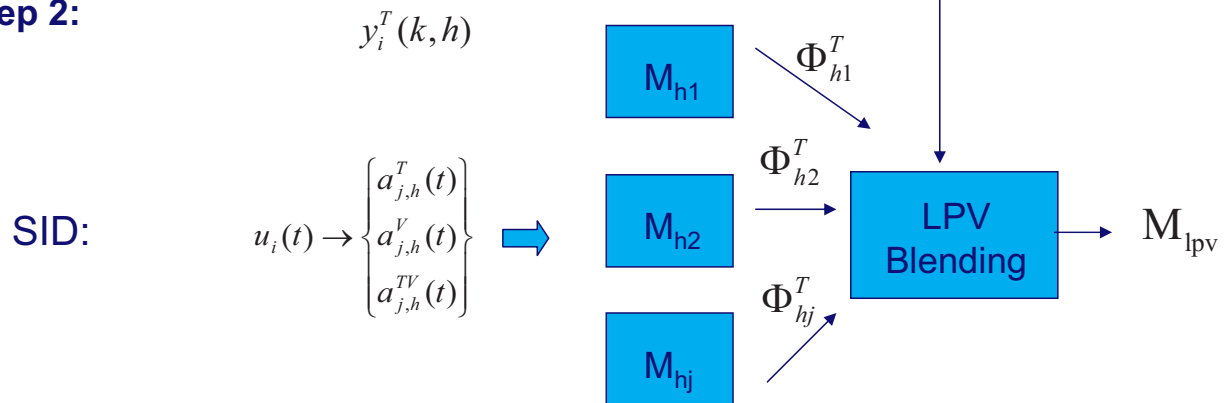
Detector (h): A dynamic or static map to detect the throat height from knowledge of plant (GTM-X) outputs

Strategy 2: LPV SID model/Observer

- Step 1:



- Step 2:



LPV Identification - Spline based

RO-LPV can be considered as weighted blend of Reduced Order models

$$y(t) = \alpha_1(w)[\hat{G}_1^1(q)u_1(t) + \dots + \hat{G}_m^1(q)u_m(t)] \\ + \alpha_2(w)[\hat{G}_1^2(q)u_1(t) + \dots + \hat{G}_m^2(q)u_m(t)] \\ + \alpha_3(w)[\hat{G}_1^3(q)u_1(t) + \dots + \hat{G}_m^3(q)u_m(t)] + v(t)$$

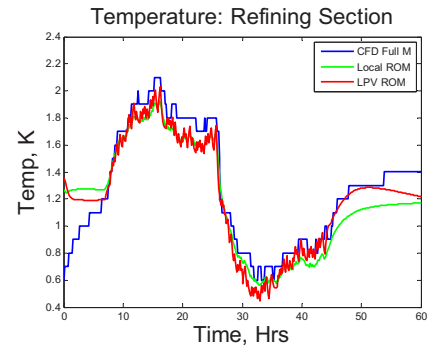
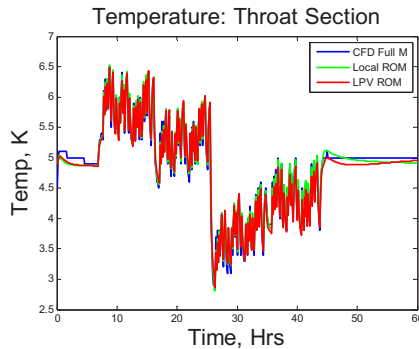
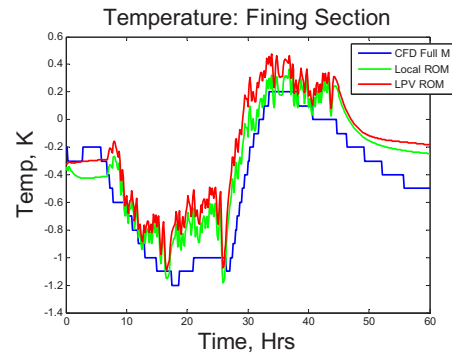
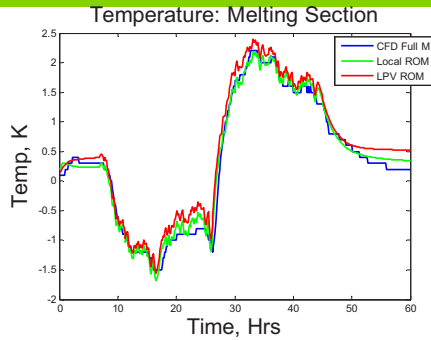
Where w is the scheduling parameter and the weightings α_i are parameterized as cubic splines

$$\alpha_1(w) = \beta_1^1 + \beta_2^1 w + \sum_{j=2}^{m-1} \beta_{j+1}^1 |w - k_j|^3$$

LPV identification \approx Spline parameter Identification

Use least square for parameter identification

Results: Strategy 2, RO-LPV



Conclusions

- **Computationally efficient model can be obtained for Large Scale Dynamical Systems in easy way. These models can be used for online control and optimization purpose.**
- **Process uncertainty can be incorporated in the model reduction framework.**
- **Nonlinear identification and exploitation of distributed nature of the process in model reduction can be very useful!**

Thank You!!