

# $\mathcal{L}_1/Q$ Approach for efficient computation of disturbance rejection measures for feedback control <sup>☆</sup>

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## Abstract

This paper presents practical methods for computation of disturbance rejection measures, which are useful for assessing the dynamic operability of the process. Using  $\mathcal{L}_1$  optimal control theory, we consider the cases of steady-state, frequency-wise and dynamic systems. In comparison to the available methods, the proposed approach ensures that a linear, causal, feedback-based controller exists that achieves the computed bounds and the method also scales well with problem dimensions.

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## 1. Introduction

The achievable control quality (“controllability”) is limited by the plant itself, independent of the controller design algorithm. A key issue in the controllability analysis is to decide upfront if there exists a controller that can reduce the effect of disturbances to an acceptable level with the available manipulated variables. When such a controller exists, the process is said to have “operability” [6]. A closely related problem is that of “flexibility” [7]. Skogestad and Wolff [1] also introduced some measures for judging upon the disturbance rejection capabilities of the process, which is similar to the dynamic operability. All these papers considered the following issue: *Is it possible to keep the outputs within their allowable bounds for the worst possible combination of disturbances, while still keeping the manipulated variables within their physical bounds?*

In this paper, we consider the disturbance rejection measures for linear time-invariant systems. For this case, Skogestad and Wolff [1] introduced the following problems:

- (1) What is the minimum output error achievable with the bounded manipulated variables for the worst possible combination of disturbances?
- (2) What is the minimum control effort or magnitude of the manipulated variables required to obtain an acceptable output error for the worst possible combination of disturbances?
- (3) What is the largest possible magnitude of disturbances such that for the worst possible combination of disturbances upto that magnitude, an acceptable output error is achievable with the bounded manipulated variables?

These problems have been solved on a frequency-by-frequency basis for SISO systems and also approximately for MIMO systems [8,9]. Hovd et al. [2] provide an exact solution for the steady-state version of this problem, but require solving a non-convex bilinear program. Kookos and Perkins [3] present an integer programming based formulation of the steady-state version of this problem. As

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pointed by Hovd and Kookos [4], the latter formulation scales better with problem dimensions. Recently, Hovd and Kookos [4] also presented a method for calculating the upper and lower bounds on the minimum output error on a frequency-by-frequency basis. This approach, however, is computationally very demanding. In summary, the available solutions for disturbance rejection problem hold only for restrictive versions of the problem (steady-state or frequency-by-frequency) and are computationally expensive.

In this paper, we consider the same problems under the assumption that the manipulated variables are generated using a linear, causal, feedback-based controller. Note that in the original problem formulation [8,9], no such assumptions are made. An objective of controllability analysis is to judge upon the existence of controllers that can satisfy the desired performance requirements. In this sense, the restriction on the controller is necessary for practical controllability analysis. Under these assumptions, the calculation of disturbance rejection measures can be treated using  $\mathcal{L}_1$ -optimal control theory, which results in solving convex programs [10]. This approach yields the optimal controller and also scales well with problem dimensions. In this paper, we consider the steady-state, frequency-wise and dynamic cases in turn.

**Notation.** We let the linear, causal plant and disturbance models be  $G(s)$  and  $G_d(s)$ , respectively such that

$$y(s) = G(s)u(s) + G_d(s)d(s),$$

where  $y(s)$  is the output,  $u(s)$  is the input and  $d(s)$  is the disturbance. For simplicity, we use the same symbols for the signals and their Laplace transforms. We deal with peak norm of signals defined as

$$\|y(t)\|_\infty = \max_t \max_i |y_i(t)|$$

and induced  $\mathcal{L}_1$ -norm (peak to peak) of transfer matrices given as [10]

$$\|G(s)\|_{\mathcal{L}_1} = \sup_{\|u(t)\|_\infty \neq 0} \frac{\|Gu(t)\|_\infty}{\|u(t)\|_\infty} = \sup_{\|u(t)\|_\infty = 1} \|Gu(t)\|_\infty.$$

When dealing with constant real or complex valued matrices, the  $\mathcal{L}_1$ -norm reduces to the matrix 1-norm, which is defined as maximum absolute row sum. In the following discussion, we drop the frequency argument  $s$  and time argument  $t$ , where no confusion can arise. For the given matrix,  $A \in \mathbb{R}^{m \times n}$ ,  $a_v$  denotes vectorized  $A$  as

$$a_v = [A_{11} \cdots A_{1n} \cdots A_{m1} \cdots A_{mn}]^T.$$

## 2. Problem formulation

In this section, we present the mathematical formulation of the problem for calculation of disturbance rejection measures. We first consider the exact problems posed by Skogestad and Wolff [1], which are usually of theoretical interest only. Next, we formulate the same problems under

the practical assumption that the controller is rational, causal and feedback-based.

### 2.1. Original problem: Minimax approach

We consider that the model has been scaled such that the allowable magnitudes of the peak values of output error, manipulated variables and disturbances are  $\gamma_y$ ,  $\gamma_u$  and 1, respectively. A procedure for such scaling has been outlined by Skogestad and Postlethwaite [9]. Then, the three problems introduced by Skogestad and Wolff [1] require solving the following minimax optimization problems [1–3]

(1) Minimum output error:

$$\gamma_{y,\min} = \max_{\|d\|_\infty \leq 1} \min_{\|u\|_\infty \leq \gamma_u} \|Gu + G_d d\|_\infty. \quad (1)$$

(2) Required input magnitude:

$$\gamma_{u,\min} = \max_{\|d\|_\infty \leq 1} \min_{\|Gu + G_d d\|_\infty \leq \gamma_y} \|u\|_\infty. \quad (2)$$

(3) Largest allowable disturbance:

$$\begin{aligned} \gamma_{d,\max} = \max \quad & \sigma \\ \text{s.t.} \quad & \max_{\|d\|_\infty \leq \sigma} \min_{\|u\|_\infty \leq \gamma_u} \|Gu + G_d d\|_\infty \leq \gamma_y. \end{aligned} \quad (3)$$

**Remark 1.** The formulation in (3) is equivalent to finding the largest scaling for disturbances such that the achievable output error becomes  $\gamma_y$ . It may seem that the largest allowable disturbance can be found as

$$\gamma'_{d,\max} = \max_{\substack{\|Gu + G_d d\|_\infty \leq \gamma_y \\ \|u\|_\infty \leq \gamma_u}} \|d\|_\infty. \quad (4)$$

The formulation in (4), however, only finds “ $a$ ” disturbance having magnitude  $\gamma'_{d,\max}$  such that the bounds on outputs and inputs can be maintained, but does not ensure that the outputs and inputs can be kept bounded for “all” disturbances having magnitude smaller than or equal to  $\gamma'_{d,\max}$ . The subtle difference between the two different formulations in (3) and (4) is illustrated by Hovd et al. [2] using an insightful example.

Each of these problems may be formulated for the following three cases:

- (a) Steady-state
- (b) Frequency-wise
- (c) Dynamic systems

While the case of dynamic systems is general, the steady-state and frequency-wise formulations are useful for analyzing the capability of the system in asymptotically rejecting constant and sinusoidal disturbances, respectively. Nevertheless, these problems are difficult to solve due to their minimax nature and different approaches for solving the steady-state [2,3] and frequency-by-frequency

[4] versions have been proposed. In general, these approaches, however, can be computationally very demanding. The reader should also note that these problems pose no restrictions on the controller. Thus achieving these bounds may require non-causal controllers with the knowledge of future disturbances. In this paper, we provide a method for computing the solution to all the problems mentioned above. The proposed methods provide a bound (upper bound on  $\gamma_{y,\min}$  and  $\gamma_{u,\min}$  and lower bound for  $\gamma_{d,\max}$ ) for the “original” problem with no restrictions on the controller and exact solution for the case of a linear feedback-based causal controller.

**Remark 2.** The steady-state and frequency-wise cases only consider the asymptotic behavior of the closed-loop system and the issue of non-causality does not arise. For these cases, the solution obtained using the minimax approach can be practically implemented, but this may require use of online optimization-based controller.

### 2.2. $\mathcal{L}_1/Q$ approach

For regulatory control, we consider that  $u = -Ky$  (negative feedback). Though the setpoints  $r$  are considered to be zero, the results can be extended to include the case of non-zero setpoints by replacing  $y$  by  $e = y - r$  in the following discussion. Now, the following relationships hold,

$$\begin{aligned} y &= SG_d d, \\ u &= -KSG_d d, \end{aligned}$$

where  $S = (I + GK)^{-1}$  is the sensitivity function. Next, we use the Youla parametrization of all stabilizing controllers, where  $G$  is considered to be stable for simplicity. When the process is unstable, similar coprime factorization based parametrization can be used; see e.g. [9]. Parameterizing  $K$  as  $K = Q(I - GQ)^{-1}$ ,

$$\begin{aligned} y &= (I - GQ)G_d d, \\ u &= -QG_d d, \end{aligned}$$

where  $Q$  is a stable rational transfer function. Now, the three problems introduced above require solving

- (1) Minimum output error:

$$\begin{aligned} \min_Q & \|(I - GQ)G_d\|_{\mathcal{L}_1} \\ \text{s.t.} & \|QG_d\|_{\mathcal{L}_1} \leq \gamma_u. \end{aligned} \quad (5)$$

- (2) Required input magnitude:

$$\begin{aligned} \min_Q & \|QG_d\|_{\mathcal{L}_1} \\ \text{s.t.} & \|(I - GQ)G_d\|_{\mathcal{L}_1} \leq \gamma_y. \end{aligned} \quad (6)$$

- (3) Largest allowable disturbance:

$$\begin{aligned} \min_Q & \sigma \\ \text{s.t.} & \|(I - GQ)G_d\|_{\mathcal{L}_1} \leq \gamma_y \sigma \\ & \|QG_d\|_{\mathcal{L}_1} \leq \gamma_u \sigma. \end{aligned} \quad (7)$$

For  $\sigma^*$  solving the optimization problem in (7), the magnitude of the largest allowable disturbance is given as  $1/\sigma^*$ .

The formulation of these optimization problems using  $\mathcal{L}_1$ -optimal control theory is along the same lines as done by Dahleh and Diaz-Bobillo [10]. The problem of computing achievable  $\|y\|_2$  for specified disturbances (e.g. step-type) using the Youla parameterization was also considered by Swartz [11,12]. The approach taken here considers the time-domain bounds characterized by  $\|y\|_\infty$  directly and also allows for the worst possible combination of disturbances, as is relevant for computing disturbance rejection measures.

**Remark 3.** Sometimes, it is of interest to find the minimum input magnitude that provides perfect control of outputs; especially at steady-state or a non-zero frequency. When  $G$  is non-singular, an explicit solution to this problem is available in [9]. Ma et al. [13] have extended these results to rank deficient  $G$  by requiring perfect control only for disturbances lying in the controllable subspace. Ma et al. [13] define the controllable subspace  $W$  as the subspace spanned by the sign-adjusted left singular vectors corresponding to non-zero singular values of  $G$ . While no restrictions are imposed on the controller in [13], the minimum input magnitude required to achieve perfect control in the controllable subspace using a linear feedback-based controller can be computed by replacing  $G$  and  $G_d$  by  $W^H G$  and  $W^H G_d$  in the optimization problem in (6).

In the following discussion, we only consider the minimum output error problem (problem 1) in detail and the formulations for the remaining two problems can be obtained similarly. Before dealing with the dynamic systems, we first deal with the steady-state and frequency-dependent versions of disturbance rejection problems. The reason for detailed discussion of the steady-state version of the problem is that its formulation is similar to the corresponding formulation for discrete-time dynamic systems, which facilitates the introduction of more involved expressions later in this paper.

#### 2.2.1. Steady-state

We recall that for constant matrices, the  $\mathcal{L}_1$ -norm reduces to the matrix 1-norm. Now, let  $Q$  be vectorized as

$$q_v = [Q_{11} \cdots Q_{1n_y} \cdots Q_{n_u n_y}]^T.$$

Then,  $\|QG_d\|_1 \leq \gamma_u$  is equivalent to

$$-\alpha_v \leq (I_{n_u} \otimes G_d^T) q_v \leq \alpha_v, \quad (8)$$

$$(I_{n_u} \otimes 1_{n_d}) \alpha_v \leq \gamma_u \cdot 1_{n_u}, \quad (9)$$

where  $\otimes$  is the Kronecker tensor product and  $1_{n_u}$  is an  $n_u$  dimensional column vector of 1's. Similarly,  $\|G_d - GQ G_d\|_1 \leq \gamma_y$  is equivalent to

$$-\beta_v \leq (G_d)_v - (G \otimes G_d^T) q_v \leq \beta_v, \quad (10)$$

$$(I_{n_y} \otimes 1_{n_d}) \beta_v \leq \gamma_y \cdot 1_{n_y}. \quad (11)$$

In (8) and (10),  $\alpha_v \in \mathbb{R}^{n_u n_d}$  and  $\beta_v \in \mathbb{R}^{n_y n_d}$  bound the absolute values of the elements of  $QG_d$  and  $(G_d - GQG_d)$ , respectively. Similarly, in (9) and (11), the sum of the absolute values of the elements of each row (arising due to matrix 1-norm) of  $QG_d$  and  $(G_d - GQG_d)$  are bounded by  $\gamma_u$  and  $\gamma_y$ , respectively. Define  $x = [q_v^T \ \alpha_v^T \ \beta_v^T \ \gamma_y^T]^T$ . Then, in the standard linear program form the minimum output error is determined by solving

$$\begin{aligned} \min_x \quad & [0 \ 0 \ 0 \ 1]x \\ \text{s.t.} \quad & \begin{bmatrix} I_{n_u} \otimes G_d^T & -I & 0 & 0 \\ -I_{n_u} \otimes G_d^T & -I & 0 & 0 \\ 0 & I_{n_u} \otimes 1_{n_d} & 0 & 0 \\ -G \otimes G_d^T & 0 & -I & 0 \\ G \otimes G_d^T & 0 & -I & 0 \\ 0 & 0 & I_{n_y} \otimes 1_{n_d} & -1_{n_y} \end{bmatrix} x \leq \begin{bmatrix} 0 \\ 0 \\ \gamma_u \cdot 1_{n_u} \\ -(G_d)_v \\ (G_d)_v \\ 0 \end{bmatrix} \\ & [-\infty \ 0 \ 0 \ 0] \leq x \leq \infty. \end{aligned}$$

The above linear program is sparse with  $(n_u n_y + n_u n_d + n_y n_d + 1)$  variables and  $(2(n_u n_d + n_y n_d) + n_u + n_y)$  constraints. In this paper, we use Tomlab/Cplex [14] for solving this program. Note that for finding the required input magnitude, one only needs to change the roles of  $\gamma_u$  and  $\gamma_y$  in the above formulation.

### 2.2.2. Frequency-wise

We next consider the calculation of minimum output error on a frequency-by-frequency basis. As compared to the steady-state case, the additional complication is that the matrix 1-norm requires calculation of absolute values, which is non-linear for complex scalars in terms of its real and imaginary parts. To overcome this difficulty, Hovd and Kookos [4] suggest under and overestimating the peak norms of various signals using polyhedral approximations. Such an approximation, however, increases the computational requirements considerably, especially when the approximation error is required to be small. In the following discussion, we show that under the  $\mathcal{L}_1/Q$  approach, the calculation of minimum output error can be posed as a convex program. The formulation is based on the observation that though non-linear, the absolute value of a complex scalar can be bounded using a linear matrix inequality (LMI) [15].

We recall that the vectorized format of  $QG_d$  is given as  $(I_{n_u} \otimes G_d^T)q_v$ . Let  $[(I_{n_u} \otimes G_d^T)]_{i*}$  denote the  $i$ th row of  $(I_{n_u} \otimes G_d^T)$ . Then the magnitude of the elements of  $QG_d$  can be bounded as

$$\begin{aligned} & |[(I_{n_u} \otimes G_d^T)]_{i*} q_v| \leq [\alpha_v]_i \\ & \iff |a_i + jb_i| \leq [\alpha_v]_i \\ & \iff [a_i \ b_i][a_i \ b_i]^T \leq [\alpha_v]_i^2 \\ & \iff \begin{bmatrix} [\alpha_v]_i & a_i & b_i \\ a_i & [\alpha_v]_i & 0 \\ b_i & 0 & [\alpha_v]_i \end{bmatrix} \geq 0, \end{aligned} \quad (12)$$

where the last equivalence is obtained using Schur complement lemma [15]. Here

$$\begin{aligned} a_i &= \text{Re}[(I_{n_u} \otimes G_d^T)]_{i*} \text{Re } q_v - \text{Im}[(I_{n_u} \otimes G_d^T)]_{i*} \text{Im } q_v, \\ b_i &= \text{Re}[(I_{n_u} \otimes G_d^T)]_{i*} \text{Im } q_v + \text{Im}[(I_{n_u} \otimes G_d^T)]_{i*} \text{Re } q_v. \end{aligned}$$

Similarly, the magnitude of the elements of  $(G_d - GQG_d)$  can be bounded using the following LMI

$$\begin{bmatrix} [\beta_v]_j & c_j & d_j \\ c_j & [\beta_v]_j & 0 \\ d_j & 0 & [\beta_v]_j \end{bmatrix} \geq 0, \quad (13)$$

where

$$\begin{aligned} c_j &= \text{Re}[(G_d)_v]_j - \text{Re}[(G \otimes G_d^T)]_{j*} \text{Re } q_v + \text{Im}[(G \otimes G_d^T)]_{j*} \text{Im } q_v, \\ d_j &= \text{Im}[(G_d)_v]_j - \text{Re}[(G \otimes G_d^T)]_{j*} \text{Im } q_v - \text{Im}[(G \otimes G_d^T)]_{j*} \text{Re } q_v. \end{aligned}$$

Now, by defining  $z = [\text{Re } q_v^T \ \text{Im } q_v^T \ \alpha_v^T \ \beta_v^T \ \gamma_y^T]^T$ , the problem requires solving

$$\begin{aligned} \min_z \quad & [0 \ 0 \ 0 \ 0 \ 1]z \\ \text{s.t.} \quad & \begin{bmatrix} 0 & 0 & I_{n_u} \otimes 1_{n_d} & 0 & 0 \\ 0 & 0 & 0 & I_{n_y} \otimes 1_{n_d} & -1_{n_y} \end{bmatrix} z \leq \begin{bmatrix} \gamma_u \cdot 1_{n_u} \\ 0 \end{bmatrix} \\ & (12) \text{ for } i = 1, 2, \dots, n_u n_d \\ & (13) \text{ for } j = 1, 2, \dots, n_y n_d \\ & [-\infty \ -\infty \ 0 \ 0 \ 0] \leq z \leq \infty. \end{aligned}$$

In this paper, we use the software package Tomlab/PenSDP [14] using the interface Yalmip [16] for solving this semi-definite program.

### 2.2.3. Dynamic systems

For continuous-time systems, the computation of  $\mathcal{L}_1$ -norm is difficult and the problems involving this norm are almost exclusively solved using discretized models. For the discrete-time univariable system  $g(z^{-1})$ , the  $\mathcal{L}_1$ -norm is given as

$$\|g(z^{-1})\|_{\mathcal{L}_1} = \sum_{i=1}^{\infty} |g_i|,$$

where  $g_i$  is the  $i$ th impulse response coefficient and  $z^{-1}$  is the backshift operator. In practice, finite impulse response (FIR) models are used and a method for selecting the order of the FIR model is given by Dahleh and Diaz-Bobillo [10]. For the multivariable system  $G(z^{-1})$  with  $n_y$  outputs and  $n_u$  inputs, the  $\mathcal{L}_1$ -norm is

$$\|G(z^{-1})\|_{\mathcal{L}_1} = \left\| \begin{bmatrix} \|G_{11}(z^{-1})\|_{\mathcal{L}_1} & \cdots & \|G_{1n_u}(z^{-1})\|_{\mathcal{L}_1} \\ \vdots & \cdots & \vdots \\ \|G_{n_y 1}(z^{-1})\|_{\mathcal{L}_1} & \cdots & \|G_{n_y n_u}(z^{-1})\|_{\mathcal{L}_1} \end{bmatrix} \right\|_1.$$

With this minor detour, we next formulate the linear programming problem that can be used for calculating the minimum output error. We consider that for  $G(z^{-1})$  and  $G_d(z^{-1})$ , FIR models of order  $N$  are used, whereas the order

of FIR model of  $Q(z^{-1})$  is  $N_Q$  with  $N_Q \leq N$ . Note that the order of the decision variable  $Q(z^{-1})$  is difficult to determine *a priori* and in practice,  $N_Q$  can be increased sequentially, until convergence.

For posing this problem as a standard linear program, we need to vectorize the impulse response coefficients of  $Q(z^{-1})G_d(z^{-1})$  and  $G_d(z^{-1}) - G(z^{-1})Q(z^{-1})G_d(z^{-1})$ . For this purpose, it is useful to represent these impulse response coefficients using matrix notation. The impulse response coefficients of  $Q(z^{-1})G_d(z^{-1})$  are given as

$$\begin{bmatrix} (QG_d)_1 \\ (QG_d)_2 \\ \vdots \\ (QG_d)_N \end{bmatrix} = \begin{bmatrix} Q_1 & 0 & \cdots & \cdots & 0 \\ Q_2 & Q_1 & \cdots & \cdots & 0 \\ \vdots & \vdots & \ddots & \vdots & 0 \\ 0 & \cdots & Q_{N_Q} & \cdots & Q_1 \end{bmatrix} \begin{bmatrix} G_{d,1} \\ G_{d,2} \\ \vdots \\ G_{d,N} \end{bmatrix}$$

which can be vectorized as

$$\begin{bmatrix} I_{n_u} \otimes G_{d,1}^T & 0 & \cdots & 0 \\ I_{n_u} \otimes G_{d,2}^T & I_{n_u} \otimes G_{d,1}^T & \cdots & 0 \\ \vdots & \vdots & \ddots & 0 \\ I_{n_u} \otimes G_{d,N}^T & \cdots & \cdots & I_{n_u} \otimes G_{d,(N-N_Q+1)}^T \end{bmatrix} \begin{bmatrix} (Q_1)_v \\ (Q_2)_v \\ \vdots \\ (Q_{N_Q})_v \end{bmatrix} \quad (14)$$

where

$$(Q_i)_v = [Q_{i,11} \cdots Q_{i,1n_y} \cdots Q_{i,n_u n_y}]^T.$$

Similarly, impulse response coefficients of  $G_d(z^{-1}) - G(z^{-1})Q(z^{-1})G_d(z^{-1})$  can be vectorized as

$$\begin{bmatrix} (G_{d,1})_v \\ (G_{d,2})_v \\ \vdots \\ (G_{d,N})_v \end{bmatrix} = \begin{bmatrix} G_1 \otimes G_{d,1}^T & 0 & \cdots & 0 \\ G_1 \otimes G_{d,2}^T + G_2 \otimes G_{d,1}^T & G_1 \otimes G_{d,1}^T & \cdots & 0 \\ \vdots & \vdots & \ddots & 0 \\ \sum_{i=1}^N G_i \otimes G_{d,(N-i+1)}^T & \cdots & \cdots & \sum_{i=1}^{N-N_Q+1} G_i \otimes G_{d,(N-N_Q-i+2)}^T \end{bmatrix} \begin{bmatrix} (Q_1)_v \\ (Q_2)_v \\ \vdots \\ (Q_{N_Q})_v \end{bmatrix} \quad (15)$$

Using the vectorized impulse response coefficients in (14) and (15), and manipulations similar to (8)–(11), the problem of calculating the minimum output error for dynamic systems is same as the steady-state case with  $N(n_u n_d + n_y n_d) + N_Q n_u n_y + 1$  variables and  $(2N(n_u n_d + n_y n_d) + n_u + n_y)$  constraints. The steady-state case was handled in Section 2.2.1 and the details are not repeated.

**Remark 4.** When the process has unstable zeros, these zeros give rise to interpolation constraints. The interpolation constraints ensure that there are no unstable pole-zero cancelations and thus internal stability is maintained. When the closed-loop system is internally unstable, some of the signals become unbounded (e.g.  $u$ ), while others may

remain within bounds (e.g.  $y$ ). In this paper, we do not explicitly include the interpolation constraints, as the signals are bounded by finite  $\gamma_y$  and  $\gamma_u$ . In some limiting cases of theoretical interest (e.g. cheap control), there is no finite upper bound on the magnitudes of some signals and interpolation constraints need to be taken into account. This problem can also be approximately handled by using large but finite values for  $\gamma_y$  or  $\gamma_u$  in the proposed approach.

### 3. Examples

In this section, we consider a number of process examples taken from the literature to illustrate the concepts discussed in this paper. Some of these examples were earlier considered using the minimax formulation in [2–4].

**Example 5.** We first discuss the calculation of minimum output error for blown film extruder earlier considered by Hovd et al. [2]. This process has 15 inputs, 15 outputs and 15 disturbances, where the steady-state gain matrices of  $G$  and  $G_d$  are circulant matrices with  $G$  being rank deficient. The disturbance model  $G_d$  is parameterized by  $k, r$ , which defines the spatial correlation among different variables.

The minimum output error calculated using the bilinear formulation by Hovd et al. [2] and the  $\mathcal{L}_1/Q$  approach are shown in Table 1, where  $\gamma_u = 1$ . Hovd et al. [2] do not impose any restrictions on the controller structure and the controller that achieves the bounds presented by them can be a nonlinear or online optimization-based controller. In comparison, the  $\mathcal{L}_1/Q$  approach provides the optimal linear controller that achieves the practical bounds. The results in Table 1 show that there is no significant performance loss in using a linear feedback-based controller as compared to an online-optimization based or nonlinear controller for this process, at least for asymptotic rejection of constant disturbances. We also point out that the  $\mathcal{L}_1/Q$  approach requires at most 3 s for solving the different cases on a Pentium IV 3.2 GHz PC, showing computational efficiency.

For this process, it is not possible to achieve perfect control due to non-invertibility of  $G$ , even when arbitrarily large input variations are allowed. For example, for  $k = 1, r = 0.7$ , the minimum output error calculated using  $\mathcal{L}_1/Q$  approach is 0.241, when  $\gamma_u = 3.429$  and increasing  $\gamma_u$  does not reduce  $\gamma_y$  further indicating a fundamental limitation. Though not possible for all disturbance directions, perfect control can be achieved for disturbances

Table 1  
Comparison for minimum output error for blown film extruder (steady-state)

Case	Bilinear [2] (online optimization)	$\mathcal{L}_1/Q$ approach (this work) (linear feedback)
$k = 1, r = 0.7$	0.783	0.783
$k = 1, r = 0.3$	0.894	0.935
$k = 0.5, r = 0.3$	0.382	0.409

confined to their controllable subspace with inputs having magnitude equal to or larger than 15.303 [13]. Ma et al. [13] do not impose any restrictions on the controller. For this problem, however, a linear feedback-based controller provides same level of performance as the unrestricted controller showing that linear feedback-based controller is optimal; see also Remark 3.

**Example 6.** Next, we consider the calculation of largest allowable disturbance for the Tennessee Eastman process [17]. This example was earlier considered by Kookos and Perkins [3], where the original process was stabilized using a subset of variables. The stabilized process has 5 outputs, 5 inputs and 7 disturbances. The steady-state gain matrices for the stabilized process are available in [3].

The magnitude of the largest allowable disturbances computed using the integer programming formulation [3] are compared with the corresponding values calculated using the  $\mathcal{L}_1/Q$  approach for different combinations of disturbances in Table 2. Note that due to the practical assumption of a linear feedback-based controller, the allowable disturbance magnitude calculated using the  $\mathcal{L}_1/Q$  approach is lower than the minimax formulation, which allows for non-linear and online optimization-based controllers. In all cases, the disturbance magnitude calculated using the two alternate approaches is reasonably close. The integer programming formulation requires about 0.5 s for solving this problem for the different disturbance scenarios [3]. In comparison, the  $\mathcal{L}_1/Q$  approach requires at most 0.03 s for the different cases on a Pentium IV 3.2 GHz PC, showing computational efficiency and better scalability. We also note that the largest difference between the two approaches is seen, when only disturbance  $d_6$  is considered. It can be shown easily that for a single disturbance, the minimax and  $\mathcal{L}_1/Q$  formulations are identical for the steady-state case. Then, the apparent difference is due to the typographical errors in [3].

**Example 7.** The previous two examples dealt with steady-state case only. Here, the usefulness of formulations for frequency-wise computation and dynamic systems is illustrated using fluid catalytic cracker (FCC) process earlier considered by Hovd and Kookos [4]. The unscaled dynamic model for this process is given by Wolff [8]. In this paper, we use the following scaling matrices such that the allowed disturbance magnitude is 1.

Table 2  
Comparison for largest allowable disturbances for Tennessee Eastman process (steady-state)

Case	Integer programming [3] (online optimization)	$\mathcal{L}_1/Q$ approach (this work) (linear feedback)
$d_1-d_7$	0.392	0.385
$d_1$	0.601	0.601
$d_2$	1.273	1.273
$d_6$	1.302	1.231
$d_7$	3.368	3.368
$d_1, d_2, d_7$	0.393	0.386

$$D_y = \text{diag}(3 \quad 2 \quad 3);$$

$$D_u = \text{diag}(3 \quad 30 \quad 4.75 \times 10^{-4}); \quad D_d = \text{diag}(5 \quad 5 \quad 4).$$

For this process, perfect control is possible at steady-state using a linear rational controller. Hovd and Kookos [4] made a similar observation using an integer programming formulation. Thus, there is no limitation in using a linear controller, at least at steady-state.

Next, we consider the frequency-wise computation of minimum output error. Hovd and Kookos [4] presented lower and upper bounds on minimum output error using polyhedral approximations. The minimum output error calculated using the  $\mathcal{L}_1/Q$  approach, and the lower and upper bounds computed by Hovd and Kookos [4] are shown in Fig. 1, where the close proximity of the solution obtained using  $\mathcal{L}_1/Q$  approach and Hovd and Kookos's lower bound should be noted. Note that the  $\mathcal{L}_1/Q$  approach gives an exact value if we require the controller to be linear, causal and feedback-based, but it provides an upper bound on the minimum output error in comparison to the minimax formulation. This happens as in  $\mathcal{L}_1/Q$  approach, the controller and hence the manipulated variables are restricted, but the disturbances are still allowed to take all possible values (as the minimax formulation). This shows that for the FCC process, the lower bound computed by Hovd and Kookos [4] is tighter in comparison to the upper bound.

Finally, we consider the dynamic case. The continuous-time model is discretized using a sampling time of 2 min, for which FIR models having order  $N = 150$  suffice. The order of the Youla parameter  $Q$  is increased sequentially and no further improvements are seen for  $N_Q \geq 18$ . This results into a sparse linear program with 2863 variables and 5406 constraints. The variation of minimum output error for different values of  $\gamma_u$  is shown in Fig. 2. It is interesting to note that the minimum output error reduces sharply for

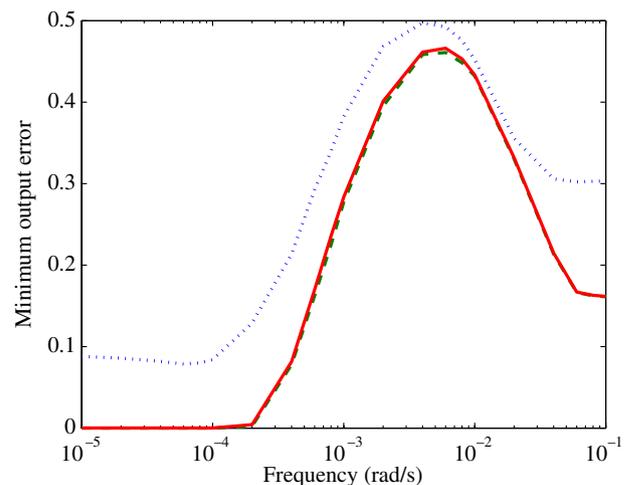


Fig. 1. Comparison of  $\mathcal{L}_1/Q$  approach (solid) with upper (dots) and lower (dashed) bounds calculated by Hovd and Kookos [4] for FCC process (frequency-wise).

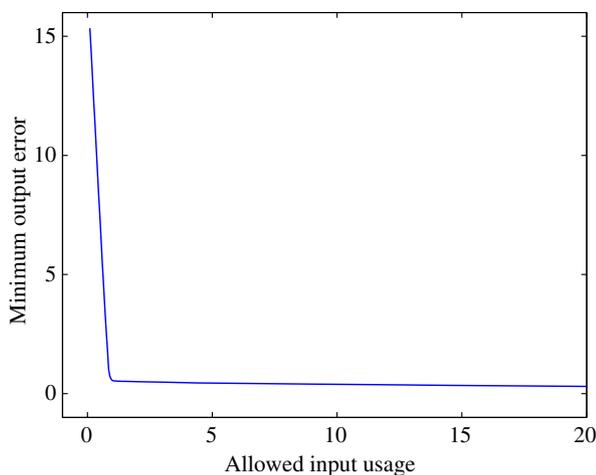


Fig. 2. Trade-off between  $\|y\|_\infty$  and  $\|u\|_\infty$  for the FCC process (dynamic case).

small increments in  $\gamma_u$  initially, but requires much larger increments in  $\gamma_u$  for similar reductions, as we get closer to the perfect control case. For example, when  $\gamma_u$  is increased from 0.5 to 1, minimum output error decreases from 7.4 to 0.55. However, decreasing the minimum output error from 0.1 to 0.05 requires increasing  $\gamma_u$  from 112.61 to 138.34 (not shown in Fig. 2).

**Example 8.** To demonstrate the effect of non-minimum phase zeros on the minimum output error, we consider

$$G(z^{-1}) = \frac{0.05}{1+a} \frac{1+az^{-1}}{1+0.5z^{-1}+0.25z^{-2}};$$

$$G_d(z^{-1}) = \frac{0.5z^{-1}}{1+0.5z^{-1}},$$

where  $G(z^{-1})$  has a zero at  $z = -a$  (non-minimum phase for  $a \geq 1$ ). The process gain has been scaled by the factor  $(1+a)$  such that it remains constant for all values of  $a$ . For this process, we use  $N = 300$  and  $N_Q = 25$ . The variation of minimum output error with the location of the zero for  $\gamma_u = 1$  is shown in Fig. 3. For this case, the minimum output error only shows minor variations with zero location indicating that the non-minimum phase zero puts no serious limitations and the performance is primarily limited by the bound on the manipulated variable.

When  $\gamma_u$  is increased to 100, the minimum output error remains close to 0.5 for minimum phase  $G(z^{-1})$ . In this case, the performance is limited by the unit time delay. By canceling the controller-dependent terms, as is usually done in minimum variance control literature [18], it can be analytically shown that 0.5 is the optimal value for minimum output error for the cheap control case. For non-minimum phase  $G(z^{-1})$ , the minimum output error is much larger as compared to the minimum phase  $G(z^{-1})$  indicating that the limitation is due to unstable zero. It shall also be noted that when the zero recedes away from the unit disc, the limitation due to unstable zero decreases, as is usually the case [9].

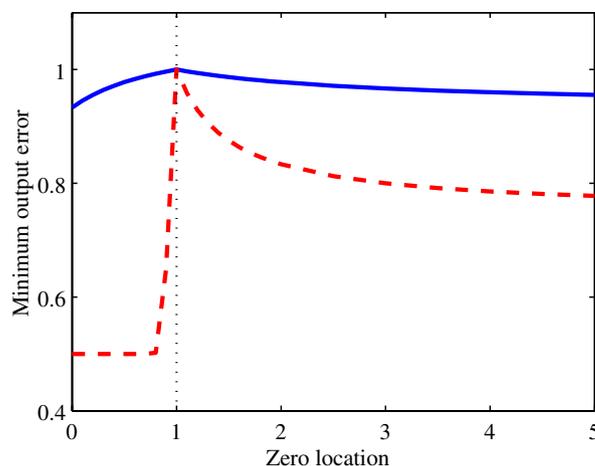


Fig. 3. Minimum output error as a function of zero location for non-minimum phase process with  $\|u\|_\infty \leq 1$  (solid) and  $\|u\|_\infty \leq 100$  (dash).

#### 4. Conclusions

We used a Youla parametrization and  $\mathcal{L}_1$  optimal control based ( $\mathcal{L}_1/Q$ ) approach for practical and efficient computation of the disturbance rejection measures proposed by Skogestad and Wolff [1]. The approach taken in this paper is numerical and explicit (and possibly approximate) characterization of the limitations on the achievable output performance with bounded inputs is an issue for future research. To this end, the reader is referred to [13], where explicit conditions for judging the feasibility of perfect control are derived.

For the various numerical examples considered in this paper, it is found that a linear feedback-based controller can provide nearly the same level of performance as an online-optimization-based controller for asymptotic rejection of constant and sinusoidal disturbances. In general, however, the use of a linear feedback-based controller can be conservative. Future research will focus upon extending the results of this paper to online-optimization-based controllers, e.g. model predictive controllers.

#### References

- [1] S. Skogestad, E.A. Wolff, Controllability measures for disturbance rejection, in: Proceedings of IFAC Workshop on Interactions between Process Design and Process Control, London, UK, 1992, pp. 23–29.
- [2] M. Hovd, D.L. Ma, R.D. Braatz, On the computation of disturbance rejection measures, *Ind. Eng. Chem. Res.* 42 (2003) 2183–2188.
- [3] I.K. Kookos, J.D. Perkins, On the efficient computation of disturbance rejection measures, *Comput. Chem. Eng.* 27 (2003) 95–99.
- [4] M. Hovd, I.K. Kookos, Calculating dynamic disturbance rejection measures, in: Proceedings of 16th IFAC World Congress, Prague, Czech Republic, 2005.
- [5] V. Kariwala, S. Skogestad, Computational approach for adjudging feasibility of acceptable disturbance rejection, Presented at AIChE annual meeting, Cincinnati, OH, USA, paper 9b (October 2005).
- [6] C. Georgakis, D.R. Vinson, S. Subramanian, D. Uzturk, A geometric approach for process operability analysis, in: P. Seferlis, M.C. Georgiadis (Eds.), *The Integration of Process Design and Control*,

- Computer-Aided Chemical Engineering, vol. 17, Elsevier, Amsterdam, Netherlands, pp. 96–126 (Chapter A4).
- [7] R.E. Swaney, I.E. Grossman, An index for operational flexibility in chemical process design, Part I: formulation and theory, *AIChE J.* 32 (1985) 621–630.
- [8] E.A. Wolff, Studies on control of integrated plants, Ph.D. Thesis, Norwegian University of Science and Technology, Trondheim, Norway (July 1994).
- [9] S. Skogestad, I. Postlethwaite, *Multivariable Feedback Control: Analysis and Design*, first ed., Wiley, Chichester, UK, 1996.
- [10] M.A. Dahleh, I.J. Diaz-Bobillo, *Control of uncertain systems, A Linear Programming Approach*, Prentice-Hall, Englewood Cliffs, NJ, 1995.
- [11] C.L.E. Swartz, A computational framework for dynamic operability assessment, *Comput. Chem. Eng.* 20 (4) (1996) 365–371.
- [12] C.L.E. Swartz, The use of controller parameterization in the integration of design and control, in: P. Seferlis, M.C. Georgiadis (Eds.), *The Integration of Process Design and Control*, Computer-Aided Chemical Engineering, vol. 17, Elsevier, Amsterdam, Netherlands, 2004, pp. 239–263 (Chapter B3).
- [13] D.L. Ma, J.G. VanAntwerp, M. Hovd, R.D. Braatz, Quantifying the potential benefits of constrained control for a large scale system, *IEE Proc. Control Theory Appl.* 149 (2002) 423–432.
- [14] K. Holmström, A.O. Göran, M.M. Edvall, *User's Guide for TOMLAB v4.0*, Tomlab Optimization, San Diego, CA, USA, 2005.
- [15] S. Boyd, L.E. Ghaoui, E. Feron, V. Balakrishnan, *Linear Matrix Inequalities in System and Control Theory*, SIAM, Philadelphia, USA, 1994.
- [16] J. Löfberg, YALMIP: A toolbox for modeling and optimization in MATLAB, in: *Proceedings of the CACSD Conference*, Taipei, Taiwan, 2004. Available from: <<http://control.ee.ethz.ch/~joloef/yalmip.php>>.
- [17] J.J. Downs, E.F. Vogel, A plant-wide industrial process control problem, *Computers Chem. Eng.* 17 (1993) 245–255.
- [18] B. Huang, S.L. Shah, *Performance Assessment of Control Loops: Theory and Applications*, Springer, London, UK, 1999.