

# Phase-Transfer Catalysed Epoxidation of Soybean Oil Using Hydrogen Peroxide and Supercritical Carbon Dioxide

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Epoxidized vegetable oils are the product of vegetable oil epoxidation reactions. Since the epoxidized vegetable oil is a nonpoisonous plasticizer, it has been widely used in the plastic packaging of food and medicine. Among the various epoxidized vegetable oils, the application of epoxidized soybean oil is broader than others. Nowadays, it's the third largest category of plasticizers. However, there are serious pollution problems in most of the conventional processes of soybean oil epoxidation.

In this paper, supercritical carbon dioxide and hydrogen peroxide was used in the epoxidation for exploring a clean and efficient process. Supercritical carbon dioxide would be both a solvent and reactant in combination with aqueous hydrogen peroxide, which made the epoxidation be possible through the formation of peroxy-carbonic acid as the intermediate oxidizer.

Soybean oil epoxidation was performed in a biphasic system composed of a supercritical CO<sub>2</sub>/oil phase and an aqueous H<sub>2</sub>O<sub>2</sub> phase. The epoxidation occurred in the aqueous phase. Therefore, the transfer of soybean oil into the aqueous phase is the rate-control step. In order to increase the solubility of soybean oil in the aqueous phase, several phase transfer catalysts were used in this reaction. As shown in Fig.1, adding of NaHCO<sub>3</sub> as the stabilizer of H<sub>2</sub>O<sub>2</sub> and the phase transfer catalyst, the conversion of soybean oil increased from 1.88 % (without additives) to 12.08 % (with NaHCO<sub>3</sub> and SDBS).

The experimental results directly provided the evidence of the existence of peroxy-carbonic acid, and confirmed that peroxy-carbonic acid could make soybean oil be epoxidized. The results disclosed that the conversion and yield of the epoxidation in supercritical CO<sub>2</sub> were far more than in gaseous or liquid CO<sub>2</sub> (See Fig.2 and 3).

The highest yield of epoxidized soybean oil was obtained under the reaction conditions as 20h in CO<sub>2</sub> at 40°C and 15MPa, the molar ratio 1:2 of soybean oil to H<sub>2</sub>O<sub>2</sub>, the mass ratio 0.05:1 of NaHCO<sub>3</sub> to H<sub>2</sub>O<sub>2</sub> aqueous solution, and the mass ratio 0.01:1 of phase transfer catalyst to soybean oil.

Being different with the conventional soybean oil epoxidation processes with carboxylic acids as catalysts, in which there are a large amount of carboxylic acids in the epoxidation product and a pollution problem caused by washing the oil product to remove the residual acid, the pH value of the oil product of epoxidation in ScCO<sub>2</sub> is 6.7, that means there is nearly no acid in the product and no need to remove the acid by washing. Therefore, the proposed process in this paper could be a more environmentally benign routine for epoxidized soybean oil production.

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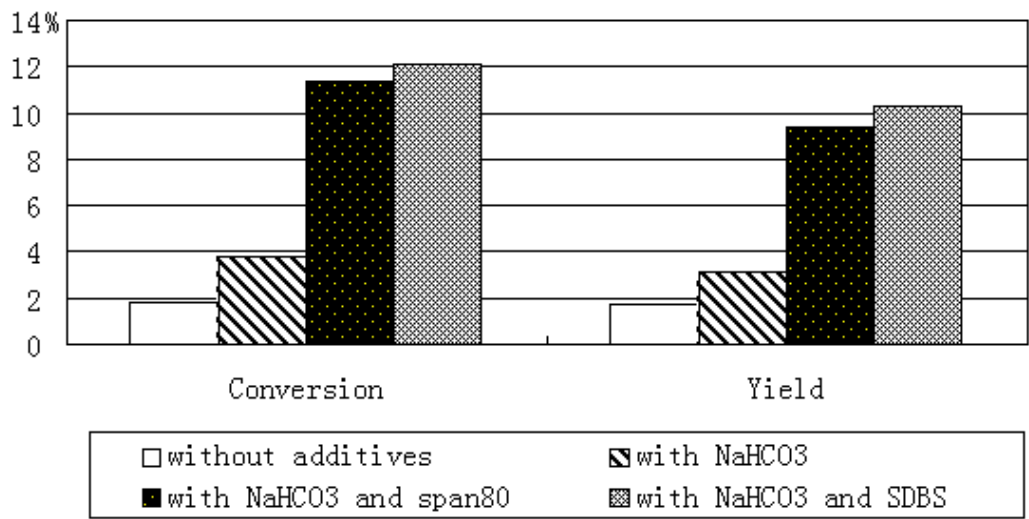


Fig. 1 Soybean oil epoxidation in ScCO<sub>2</sub> at 40 °C and 15 MPa for 20h: the enhancement effect of the phase transfer catalysts and NaHCO<sub>3</sub>

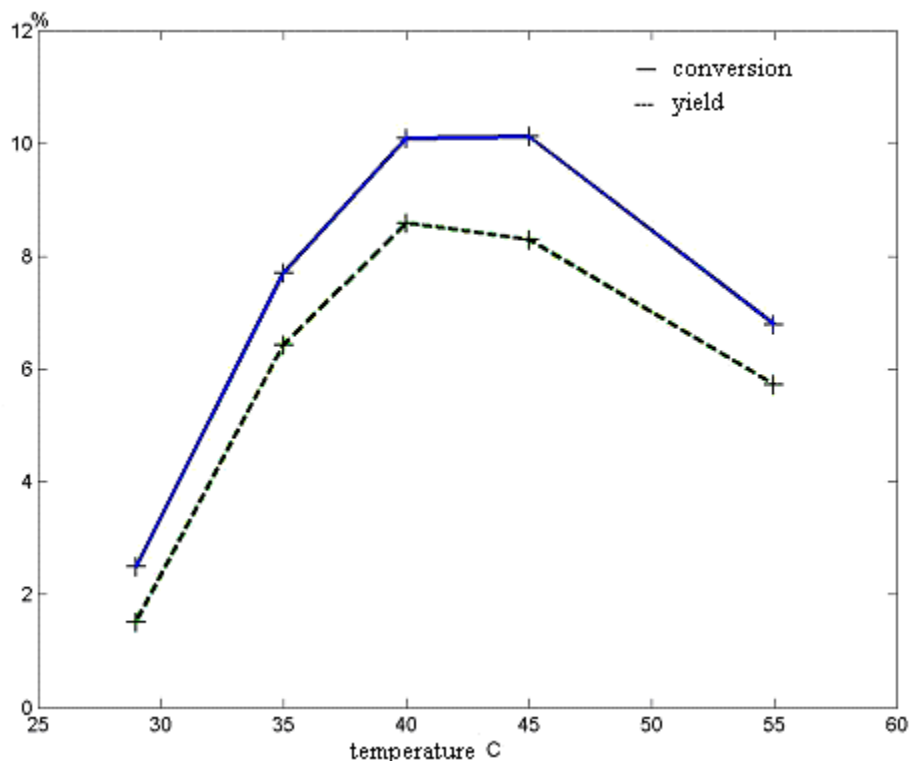


Fig. 2 Effect of reaction temperature on the epoxidation  
 Reaction was conducted for 12h at 15MPa. The volume ratio of soybean to H<sub>2</sub>O<sub>2</sub> solution was 1:1; the mass ratio of NaHCO<sub>3</sub> to H<sub>2</sub>O<sub>2</sub> solution is 0.05:1; the mass ratio of PEG1000 to soybean oil is 0.01:1.

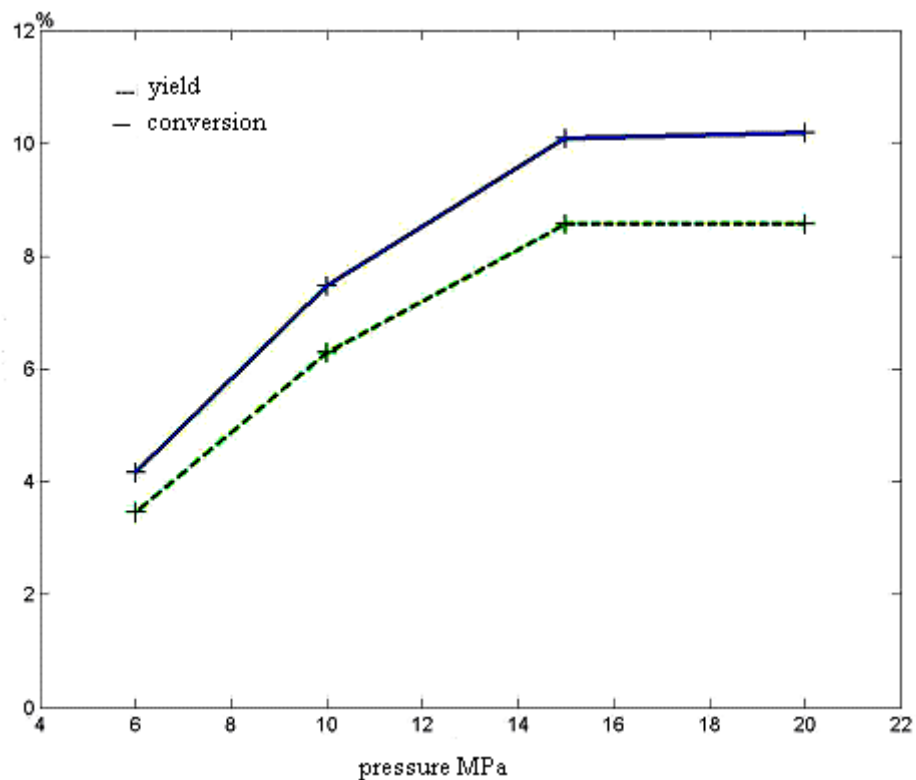


Fig. 3 Effect of reaction pressure on the epoxidation

Reaction was conducted for 12h at 40°C. The volume ratio of soybean to H<sub>2</sub>O<sub>2</sub> solution was 1:1; the mass ratio of NaHCO<sub>3</sub> to H<sub>2</sub>O<sub>2</sub> solution is 0.05:1; the mass ratio of PEG1000 to soybean oil is 0.01:1.