

# Adsorptive Filtration of Carbon Dioxide from Wet Gases Utilizing Microfibrous Filter Media Entrapped $K_2CO_3$

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## Introduction

Present commercial  $CO_2$  removal units utilize a physical solvent of alkanolamine, such as monoethanolamine (MEA), diethanolamine (DEA), and methyldiethanolamine (MDEA). These technologies require large units and high regeneration energy requirement, while exhibiting solvent and equipment degradation. Thus, the development of a new material for a cost-effective filtration with high  $CO_2$  adsorption capacity is needed.

In this paper, a microfibrous entrapped sorbent is developed for  $CO_2$  removal from flue gas. A microfibrous carrier consisting of 4 and 8  $\mu m$  (dia.) metal fibers is utilized to entrap 150-250  $\mu m$  (dia.) activated carbon particulates (ACP).  $K_2CO_3$  is then loaded onto the support by pseudo-incipient wetness at various loadings by varying the solution concentration. The adsorption capacity of  $CO_2$  at various  $K_2CO_3$  loadings was investigated as shown in Figure 1. The nano-dispersed nature of  $K_2CO_3$  combined with the use of small support particulates promotes high  $K_2CO_3$  utilization, high contacting efficiency, and high accessibility of  $K_2CO_3$ . At equivalent bed volumes,  $K_2CO_3$ /ACP entrapped materials provide longer breakthrough times for  $CO_2$  removal compared to packed beds of  $K_2CO_3$  pellets.

At 87% relative humidity, maximum capacity at room temperature based on total weight of adsorbents is found to be around 0.037 g  $CO_2$  with optimal loading of 30 wt.%  $K_2CO_3$  for packed beds corresponding to 33% utilization of impregnated  $K_2CO_3$  as shown in Figure 2. With equivalent  $K_2CO_3$  loading, microfibrous entrapped  $CO_2$  sorbents show an improvement in breakthrough capacity and pressure drop. The use of

microfibrinous entrapped sorbents provides reduced external mass transfer resistance, enhanced adsorption rates, and lower amounts of heat required for regeneration. This novel adsorbent allows reduction in overall system weight and volume for continuous removal of trace CO<sub>2</sub> from gas streams with high levels of relative humidity, namely a fuel processor stream.

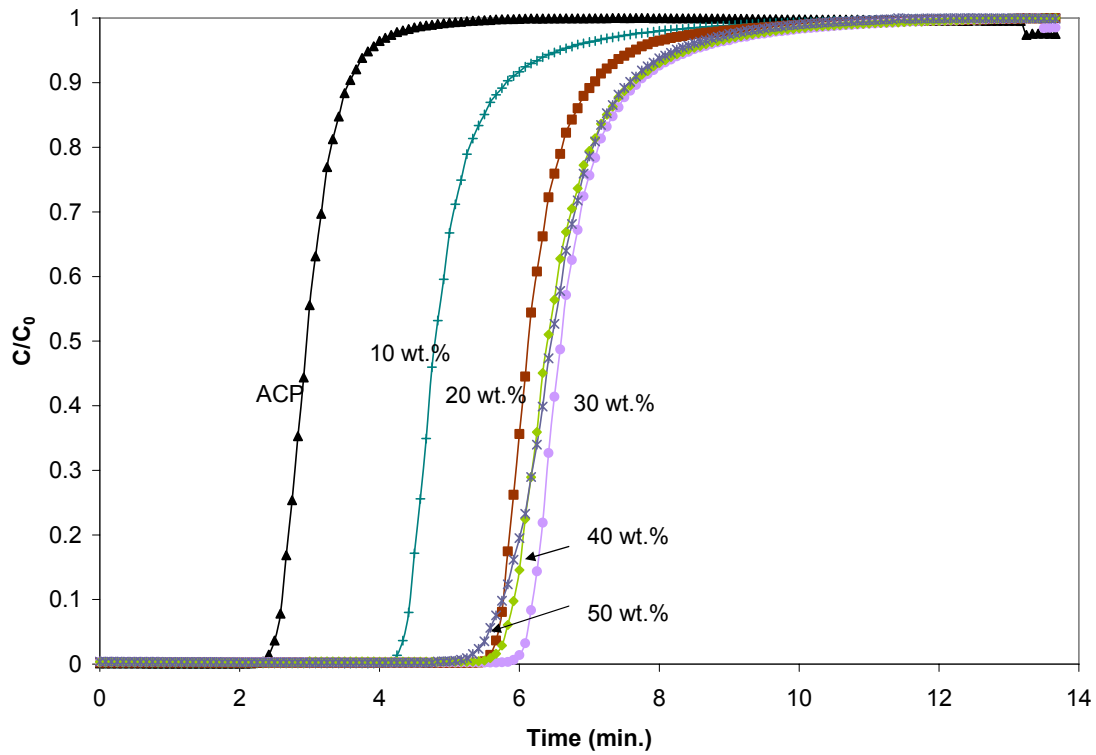


Figure 1: Effect of  $K_2CO_3$  loading on CO<sub>2</sub> adsorption performance studies of ACP supported  $K_2CO_3$ . Data were derived from using 1.5% CO<sub>2</sub> in He.

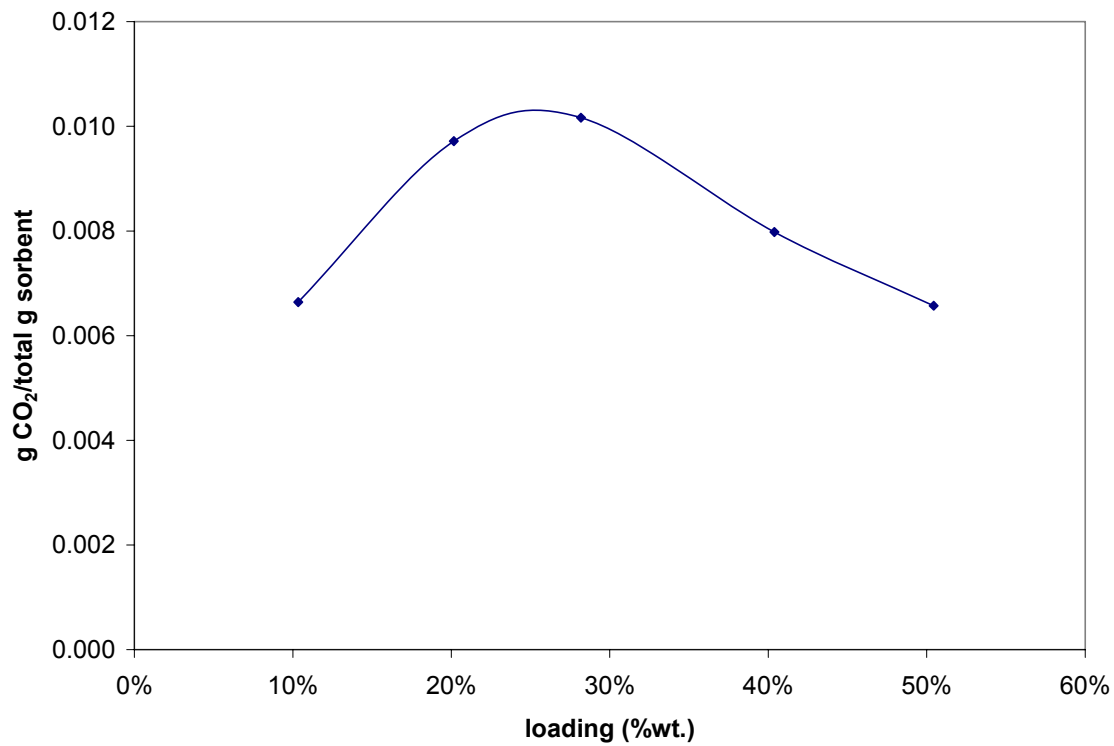


Figure 2: Relationship between adsorption capacity of CO<sub>2</sub> and K<sub>2</sub>CO<sub>3</sub> loading