

Redox characteristics of Cu-ferrite for thermochemical hydrogen production

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Abstract

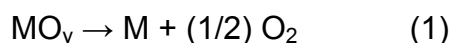
As the redox pair for thermochemical hydrogen production, Cu-ferrite was examined. Thermochemical hydrogen production process using metal oxides consisted of thermal reduction step and oxidation step by a steam as an oxidant. It was confirmed that crystal structure of Cu-ferrite was changed to metal and cation excess metal oxide during the reduction step. The reduced metal oxide reacted with steam at 800°C. It was found that the weight of the reduced Cu-ferrite was increased during reaction time, and it means the hydrogen production by water decomposition and oxidation of the reduced Cu-ferrite.

Key words: Thermochemical water-splitting, Hydrogen production, solar heat, Cu-Ferrite, Metal oxide

1. INTRODUCTION

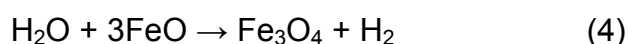
Hydrogen is an attractive fuel for the future because it is renewable as an energy resource and it is also flexible as an energy carrier. Specially, if hydrogen used as a fuel, it does not release the earth environmental pollution materials such as carbon dioxide (CO₂) and sulfur dioxide (SO₂). Therefore, if human beings desire to obtain the ultimately clean H₂ as an energy carrier, water is the only source of H₂ on the earth. However, it requires greatly high temperature (above 4000 K) to directly obtain the H₂ from the water under 1 atm. To solve this problem, the thermochemical water-splitting cycles have been proposed for the hydrogen production from the water at low temperature (Funk et al., 1966). The water-splitting method by a metal oxide using the heat energy of concentrated solar

radiation was investigated by Nakamura (Nakamura, 1977). He proposed the reactions:



The thermal decomposition of Metal oxide in the reaction (1) endothermically proceeds in air at above 2300K and 1 atm and is called the solar reaction step. However, this proposed process has problems such as materials and process technologies at the high temperature (a loss of the concentrated solar radiation) (Tofighi et al., 1980, Steinfeld et al., 1993). The reaction (2) is an exothermic reaction and the metal is reoxidized to metal oxide by water to produce hydrogen and is called the water-splitting step.

Recently, Steinfeld (Steinfeld et al., 1999) proposed the combination of the decomposition of metal oxide with natural gas such as CH₄ to decrease the process operation temperature as shown in the following reaction and are called the solar methane reforming:



Here, CH₄ is used for the activation of the metal oxide and the produced CO and H₂, which are used for the synthetic gas. However, the operating temperature of thermal decomposition of metal oxide combined with CH₄ as shown in Eq.(3) is relatively low and it has merit for the two-step water-splitting cycle, but CO₂ formation is thermodynamically more favorable at a lower temperature in CH₄-reduction of metal oxide. The choice of metal oxide in reaction (3), which determines high selectivity and reactivity for CO formation, is very important to avoid CO₂ emission.

In the thermochemical water-splitting method using the heat energy of concentrated solar radiation, the development of the metal oxide is very important for the hydrogen production by only water decomposition and not uses a fossil fuel such as methane, at low temperature. In the previous research, the authors (Park et al., 2004) reported the characteristics of Cu-ferrites and the possibility of the 2-step water-splitting cycles for the hydrogen production by only water decomposition.

In this study, Cu-ferrite was prepared as a basic metal oxide and examined for the two-step water-splitting cycles consisting of solar reduction step and the water-splitting step at low temperature of below 1173K, and evaluated the redox characteristics of the prepared Cu-ferrite.

2. Experimental

2.1. Synthesis of Cu-ferrite

The Cu-ferrite was prepared as follows. Appropriate portions of ferric nitrate solution ($\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$) and copper nitrate solution ($\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$) were dissolved in distilled water, respectively, and then mixed. The molar ratio $\text{Cu}/\text{Fe}_{\text{total}}$ in the starting solution was 2. 0.5mol KOH aq. solution was added to the mixed solution adjusting to pH 10 for co-precipitation. The co-precipitation formed was aged for 24h at the room temperature, and then the precipitation was obtained by filtering through washing with the distilled water. The products were dried at 100°C for 24h. The obtained products were sintered at 950°C in Air gas. The prepared Cu-ferrite crushed to 200 mesh size particles ($75\mu\text{m}$).

The prepared Cu-ferrite was identified by X-ray diffractometry (XRD) with CuK α radiation (Rigaku, RAD-rA diffractometer).

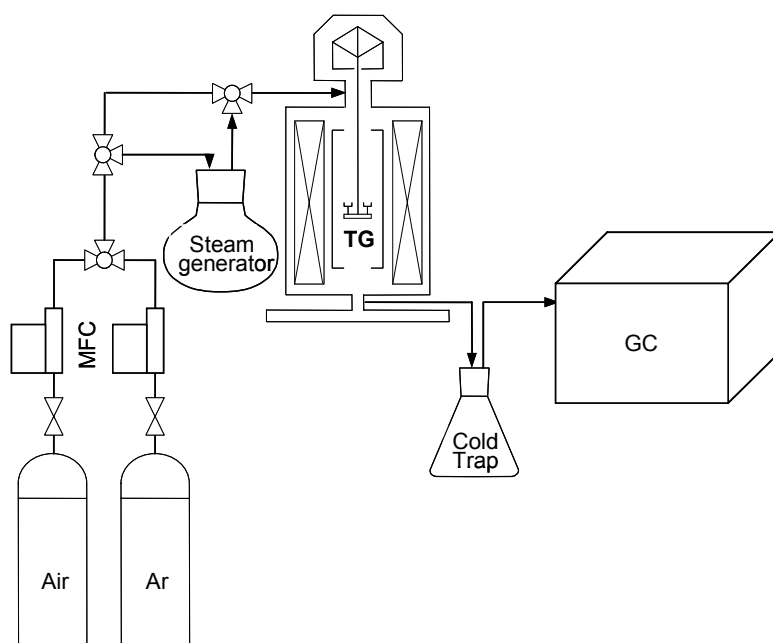
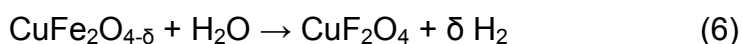


Fig.1 schematic diagram of experimental apparatus (TG reactor).

2.2. Two-step water-splitting cycles using Cu-ferrite

Fig. 1 shows a schematic diagram of experimental apparatus (TG reactor).

The prepared Cu-ferrite of 20 mg was set in an alumina sampler and placed in a furnace. The following reactions were examined for the Cu-ferrite:



Eq. (5) is referred to as solar reduction step, and Eq. (6) is referred to as the water-splitting step. The solar reduction step of Cu-ferrite was first performed. Ar gas was introduced in the reactor with flow rates of 60 ml/min. The reactor with Cu-ferrite was

heated to 900°C. After reaching to 900°C, the temperature was kept constant during each time. In this step, oxygen was released. The water-splitting step was then performed. The reactor was heated to 800°C. The steam was produced by steam generator at 250°C and mixed it with Ar gas of 60 ml/min. The reduced Cu-ferrite reacted with H₂O when passing mixed Ar/H₂O gas through the reactor, and hydrogen was produced. To determine the total weight change of metal oxide, the weight change was continuously recorded.

3. Results and discussion

3.1. Synthesis of Cu-ferrite

Fig. 2 shows the XRD pattern of the prepared Cu-ferrite.

As shown in Fig. 2, it was identified by XRD analyzer that the prepared Cu-ferrite at 950°C was crystallized as spinel-type ferrites (CuFe₂O₄) and also synthesized CuO.

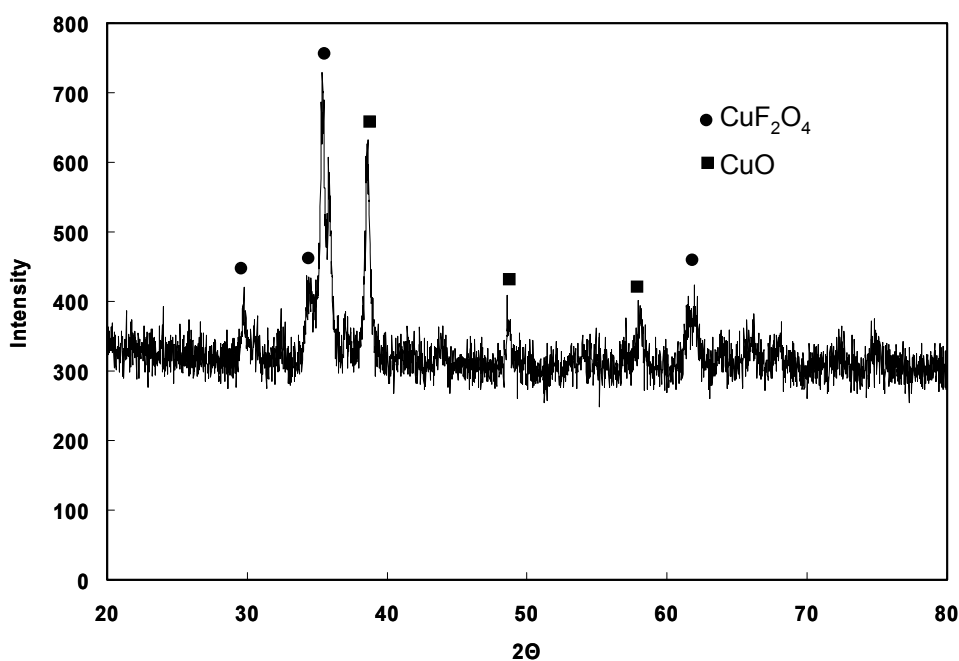


Fig.2 XRD pattern of the prepared Cu-ferrite.

The median particle size of Cu-ferrite analyzed by Particle Size Analyzer 22 (Fritsch Co.) was 25 μm.

3.2 Two-step water-splitting cycles using Cu-ferrite

3.2.1. Solar reduction step

Fig. 3 shows the relationship between the weight change and the time.

With an increase of reaction time, the weight of Cu-ferrite decreased, and then that above 16 minutes was constant. The released gas might be oxygen which confirmed the previous work (Park et al., 2004).

The δ value shown in Eq. (5) was 0.91. This value was the almost same $1/2 O_2$.

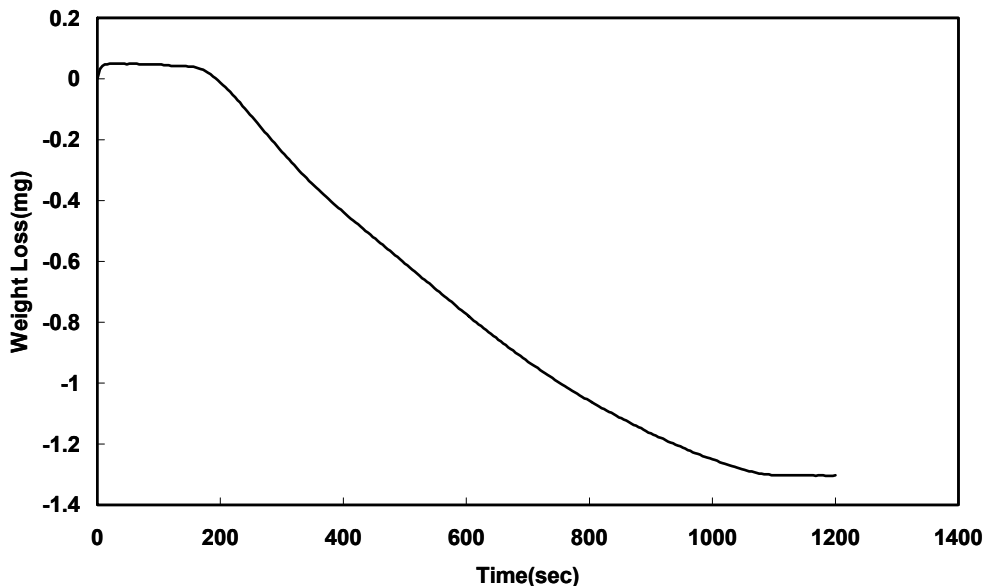


Fig.3 The relationship between the weight change and the time.

From those results, it is supposed that the reaction time of solar reduction step was suitable within 20 minutes to release the oxygen from Cu-ferrite.

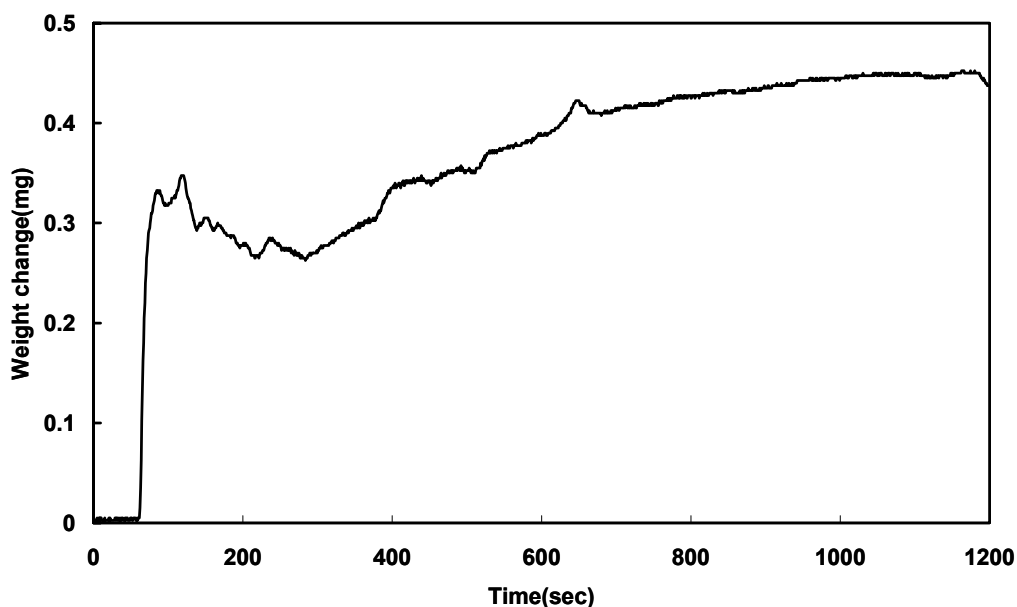


Fig.4 The relationship between the weight change and the time.

3.2.2. Water-splitting step

Fig. 4 shows the relationship between the weight change and the time.

With an increase of reaction time, the weight of the reduced Cu-ferrite increased, and then that above 20 minutes was constant. The released gas might be hydrogen which confirmed the previous work (Park et al., 2004).

The δ value shown in Eq. (6) was 0.32. This value was the almost same 0.32 H₂.

From those results, it is supposed that the reaction time of water-splitting step was suitable about 20 minutes to produce the hydrogen from the reduced Cu-ferrite.

It is expected from above results that the 2-step water-splitting cycles for the hydrogen production using Cu-ferrite might be possible as shown in Eq.(5) and (6).

For the further study, it is necessary to clarify the stability of the prepared Cu-ferrite by the repetition experiments of two-step water-splitting cycles for a long life time and evaluate the thermal efficiency.

4. Conclusions

(1) The Cu-ferrite was prepared as a basic metal oxide for the two-step water-splitting cycles consisting of solar reduction step and water-splitting step using the solar heat.

(2) All steps were carried out at relatively low temperature below 1173K. In the solar reduction step, it was confirmed that oxygen release from the prepared Cu-ferrite thermally progressed within reaction time of 20 minutes. The δ value shown in Eq. (5) was 0.91.

(3) The water-splitting step was carried out after the solar reduction step. The δ value shown in Eq. (6) was 0.32.

(4) The 2-step water-splitting cycles for the hydrogen production using Cu-ferrite might be possible as shown in Eq.(5) and (6).

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Literature Cited

Funk, J.E., R.M. Reinstrom, "Energy Requirements in the Production of Hydrogen from Water", *I&EC Process Design and Development*, **5**, 336 (1966).

Nakamura, T., "Hydrogen Production from Water Utilizing Solar Heat at High Temperature", *Solar Energy*, **19**, 467 (1977).

Tofighi, A., F.Sibieude, "Note on the Condensation of the Vapor Phase above a Melt of Iron

- Oxide in a Solar Parabolic Concentrator”, *Int. J. Hydrogen Energy*, **5**, 375 (1980).
- Steinfeld. A., M.Schubnell, “Optimum Aperture Size and Operating Temperature of a Solar Cavity-Receiver”, *Solar Energy*, **50**, 19 (1993).
- Steinfeld. A., S. Sanders, R. Palumbo, “Design Aspects of Solar Thermochemical Engineering”, *Solar Energy*, **65**, 43 (1999).
- Park, C.-S., I.-T. Seo, J.-M. Kim, S.-H. Lee, G.-J. Hwang, “Study on the Hydrogen Production using the Metal Oxide (Cu-Ferrite)”, *Trans. Korean Hydrogen and New Energy Soc.*, in press (in Korean).