



























(a) The balances "mass in = mass out" for total mass and sugar mass are $E_1 + E_2 = F_1$. $E_2 = \pi F_2$

 $F_1\,+\,F_2\,=\,F;\;\;F_1\,=\,x\,F$

Note that the mixing process itself has no dynamics. Linearization yields

 $dF_1 + dF_2 = dF: \ dF_1 = x^* dF + r \quad ax$ With $u_1 = dF_1, u_2 = dF_2, y_1 = dF$ and $y_2 = dx$ we then get the model

$$y_1 = u_1 + u_2 y_2 = \frac{1 - x^*}{F^*} u_1 - \frac{x^*}{F^*} u_2$$

where $x^* = 0.2$ is the nominal steady-state sugar fraction and $F^* = 2$ kg/s is the nominal amount. (b,c) The transfer matrix then becomes

$$G(s) = \begin{pmatrix} 1 & 1\\ \frac{1-x^*}{F^*} & -\frac{x^*}{F^*} \end{pmatrix} = \begin{pmatrix} 1 & 1\\ 0.4 & -0.1 \end{pmatrix}$$

(d) The corresponding RGA matrix is (at all frequencies)

$$\Lambda = \begin{pmatrix} x^* & 1 - x^* \\ 1 - x^* & x^* \end{pmatrix} = \begin{pmatrix} 0.2 & 0.8 \\ 0.8 & 0.2 \end{pmatrix}$$

For decentralized control, it then follows from pairing rule 1 ("prefer pairing on RGA elements close to 1") that we should pair on the off-diagonal elements; that is, use u_1 to control y_2 and use u_2 to control y_1 . (e) This corresponds to using the largest stream (water, u_2) to control the amount $(y_1 = F)$, which is reasonable from a physical point of view. Also note that the RGA-elements are always between 0 and 1 for this process, and the RGA-elements are all 0.5, corrresponding to "switching" the pairings, when $x^* = 0.5$, which is when the two feed streams are equal.