

MPC Introduction

- Overview
 - Basic Concept of MPC
 - History
- Optimization Formulation
 - Models
 - Analytical Solution to Unconstrained Problem
- Summary
 - Limitations & a Look Ahead

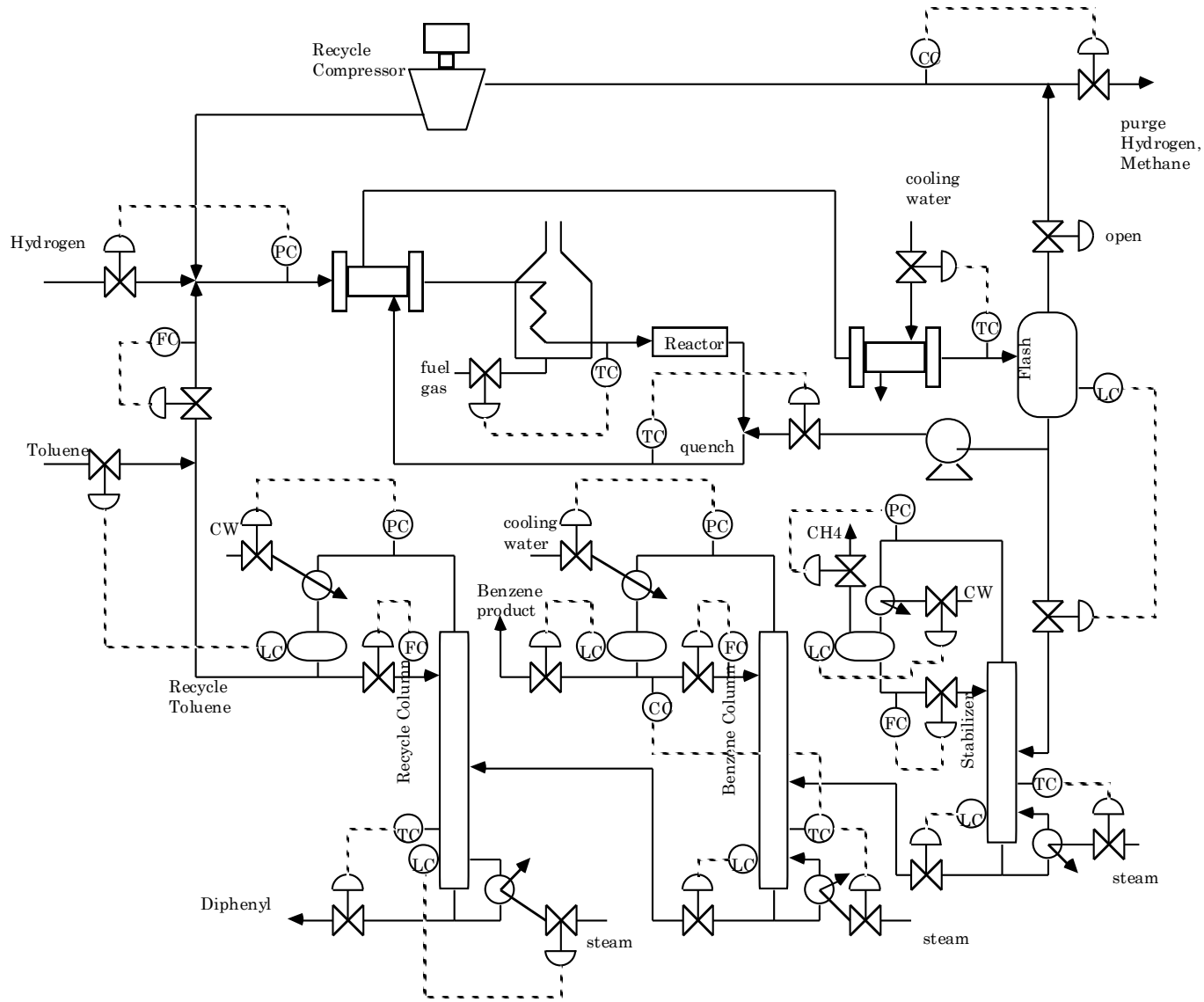
B. Wayne Bequette



Rensselaer

Chemical and Biological Engineering

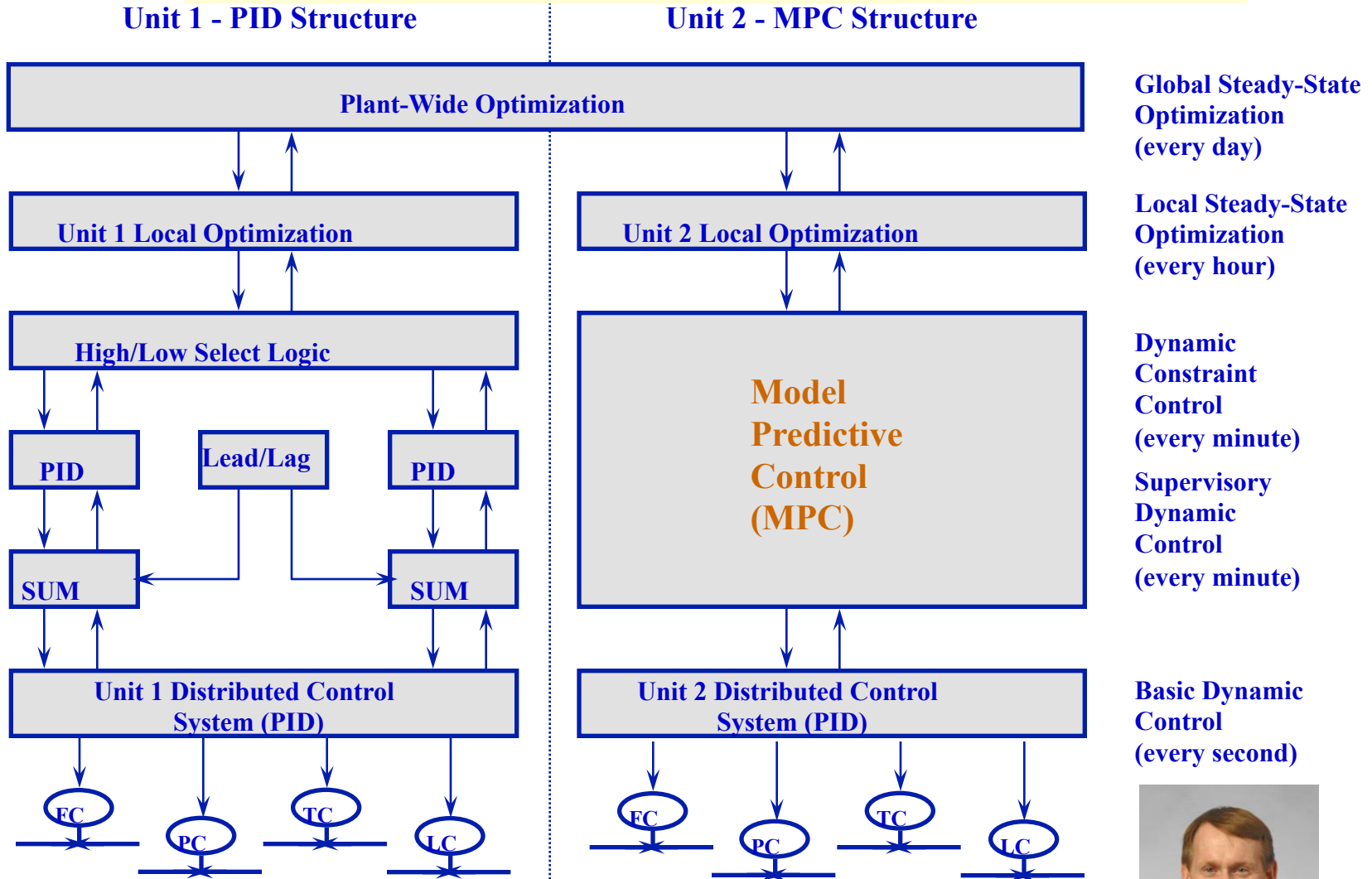
Motivation: Complex Processes



Important Issues in Petroleum Refining

- **Multivariable, Large Scale**
 - Challenge to tune individual SISO controllers
- **Operation at Constraints**
 - Anti-reset windup and other strategies for PID
- **Economic Payout for Advanced Control**
 - Economic return justifies capital and on-going maintenance costs
- **Model Predictive Control**
 - Evolved independently in the US and France refining industry

How is MPC used?

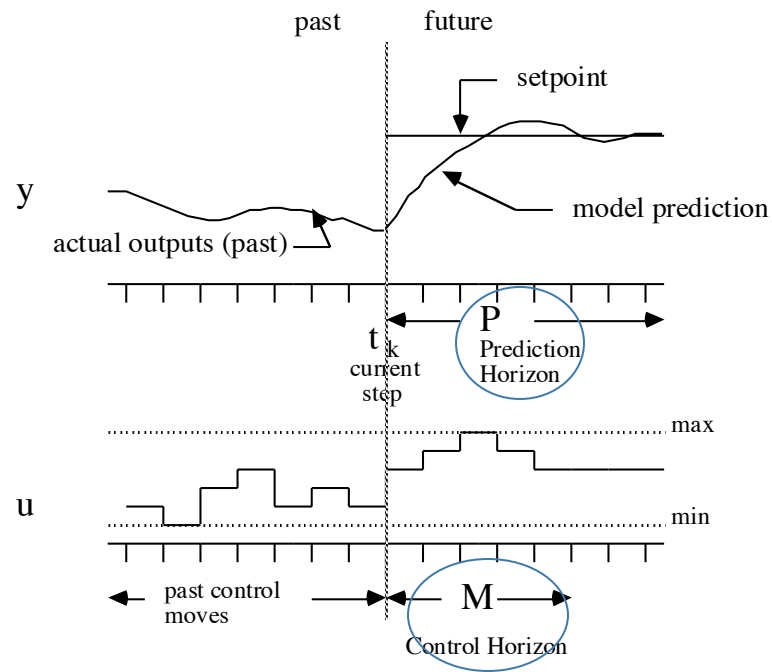


From Tom Badgwell, 2003 Spring AIChE Meeting, New Orleans



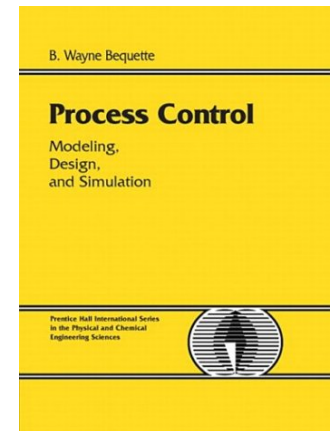
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Model Predictive Control (MPC)



Find current and future manipulated inputs that best meet a desired future output trajectory. Implement first “control move”.

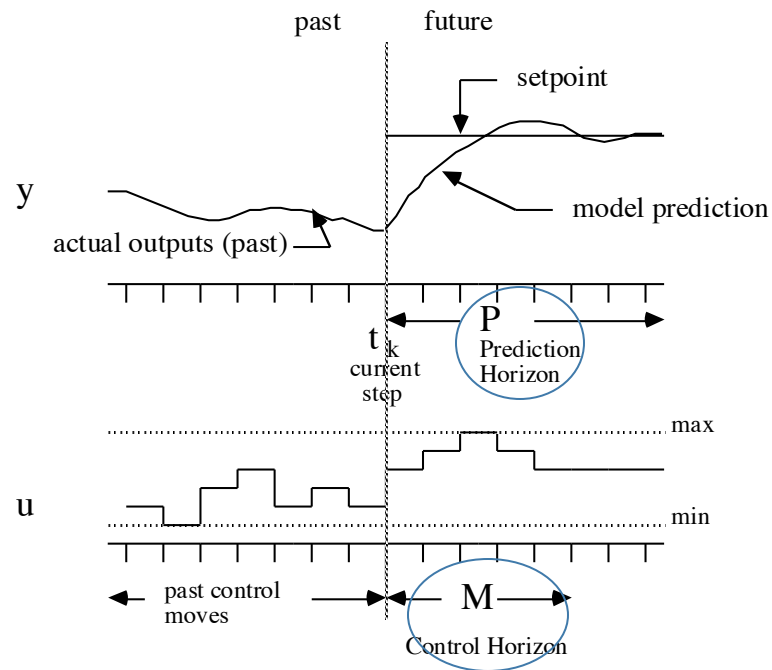
- Type of model for predictions?
- Information needed at step k for predictions?
- Objective function and optimization technique?
- Correction for model error?



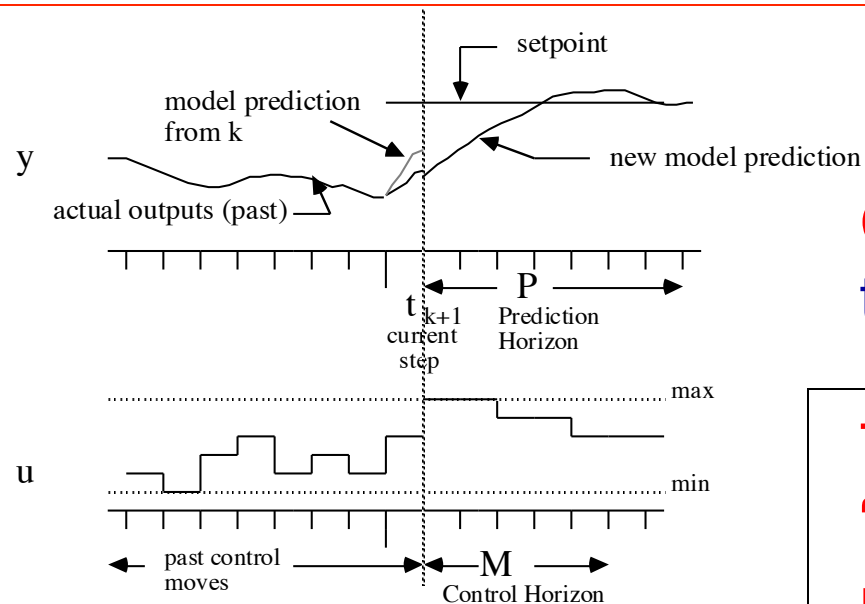
Chapter 16

B. Wayne Bequette

Model Predictive Control (MPC)



Find current and future manipulated inputs that best meet a desired future output trajectory. Implement first “control move”.



At next sample time:

Correct for **model mismatch**, then perform new optimization.

This is a major issue – “disturbances” vs. model uncertainty

MPC History



Charlie Cutler

- Intuitive
 - Basically arose in two different “camps”
- Dynamic Matrix Control (DMC)
 - 1960’s and 1970’s – Shell Oil - US

Cutler, C. R. Ph.D. Thesis, University of Houston, Houston, 1983.
Cutler, C. R.; Ramaker, B. L. *Proc. Am. Control Conf. San Francisco 1980*, WP5-B (also presented at 83rd National AIChE Meeting, Houston, 1979).

- Related to techniques developed in France (IDCOM)
- Large-scale MIMO
- Formulation for constraints important

Model Predictive Heuristic Control:
Applications to Industrial Processes*

J. RICHALET,† A. RAULT,† J. L. TESTUD† and J. PAPON†

Automatica, Vol. 14, pp. 413–428 (1976)

- Generalized Predictive Control (GPC)
 - Evolved from adaptive control
 - Focus on SISO, awkward for MIMO

Clarke, D. W., C. Mohtadi and P. S. Tuffs (1987a).
Generalized predictive control—I. The basic algorithm.
Automatica, **23**, 137–148.

Clarke, D. W., C. Mohtadi and P. S. Tuffs (1987b).
Generalized predictive control—II. Extensions and interpretations.
Automatica, **23**, 149–160.

Objective Functions

Quadratic Objective Function, Prediction Horizon (P) = 3,
Control Horizon (M) = 2

$$J = (r_{k+1} - \hat{y}_{k+1})^2 + (r_{k+2} - \hat{y}_{k+2})^2 + (r_{k+3} - \hat{y}_{k+3})^2 + w\Delta u_k^2 + w\Delta u_{k+1}^2$$

3 steps into future

2 control moves

Weight

General Representation of a Quadratic Objective Function

$$J = \sum_{i=1}^P (r_{k+i} - \hat{y}_{k+i})^2 + w \sum_{i=0}^{M-1} \Delta u_{k+i}^2$$

**With linear models, results in analytical solution
(w/o constraints)**

Alternative Objective Functions

Penalize u rather than Δu

$$J = \sum_{i=1}^P (r_{k+i} - \hat{y}_{k+i})^2 + w \sum_{i=0}^{M-1} u_{k+i}^2$$

Will usually result in “offset”

Sum of absolute values (results in LP)

$$J = \sum_{i=1}^P |r_{k+i} - \hat{y}_{k+i}| + w \sum_{i=0}^{M-1} |\Delta u_{k+i}|$$

Existing LP methods are efficient, but solutions hop from one constraint to another

Models

- State Space
- ARX (auto-regressive, exogenous input)
- Step Response
- Impulse (Pulse) Response

- Nonlinear, Fundamental (First-Principles)
- ANN (Artificial Neural Networks)
- Hammerstein (static NL with linear dynamics)
- Volterra
- Multiple Model

Discrete Linear Models used in MPC

$$x_{k+1} = \Phi x_k + \Gamma u_k$$

State Space

$$y_k = Cx_k$$

Some texts/papers have different sign conventions

$$y_k = -a_1 y_{k-1} - a_2 y_{k-2} - \dots - a_n y_{k-n} +$$
$$b_0 u_k + b_1 u_{k-1} + b_2 u_{k-2} + \dots + b_m u_{k-m}$$

Input-Output
(ARX)

usually $b_0 = 0$

$$y_k = \sum_{i=1}^{\infty} s_i \Delta u_{k-i}$$

Step Response

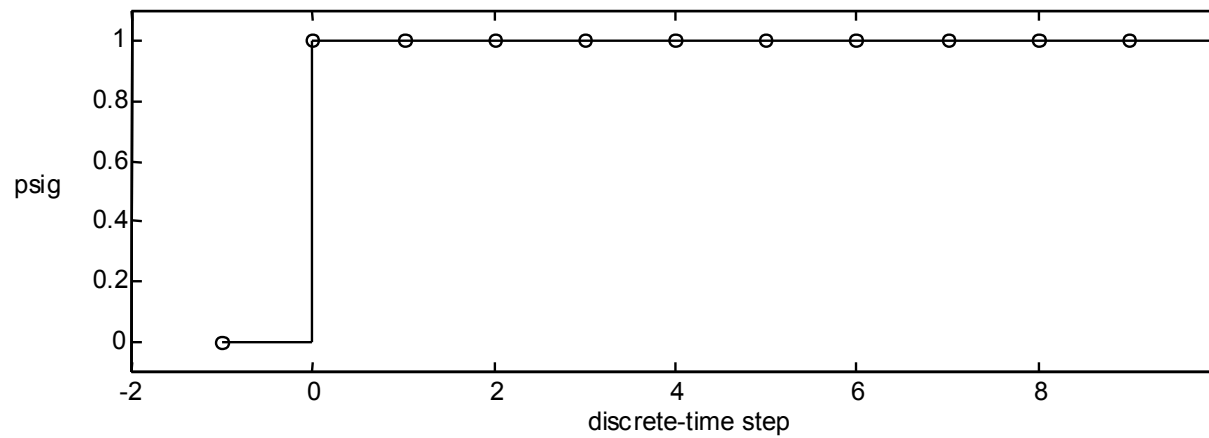
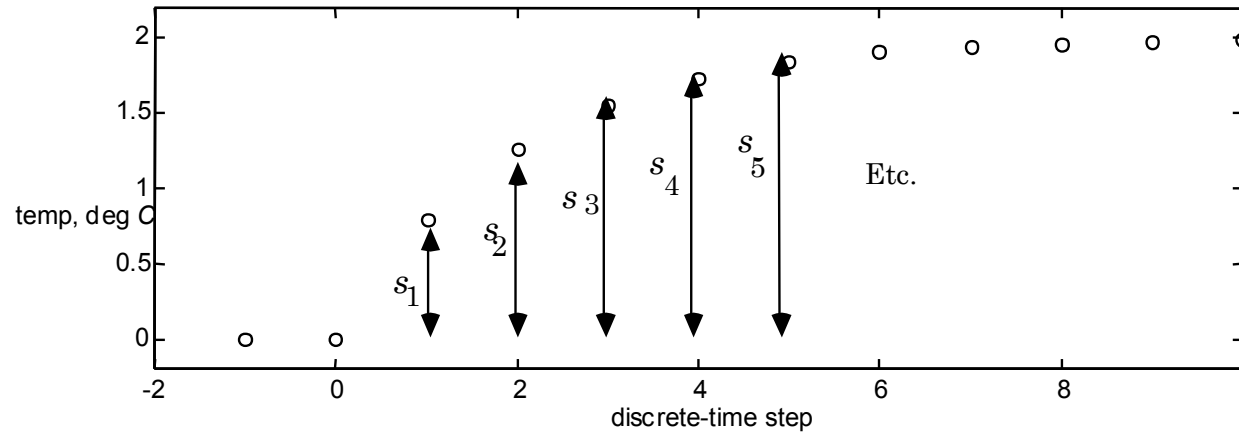
$$= s_1 \Delta u_{k-1} + \dots + s_N \Delta u_{k-N} + s_{N+1} \Delta u_{k-N-1} + \dots + s_{N+\infty} \Delta u_{k-\infty}$$

$$y_k = \sum_{i=1}^{\infty} h_i u_{k-i}$$

Impulse Response

$$= h_1 u_{k-1} + \dots + h_N u_{k-N} + h_{N+1} u_{k-N-1} + \dots + h_{N+\infty} u_{k-\infty}$$

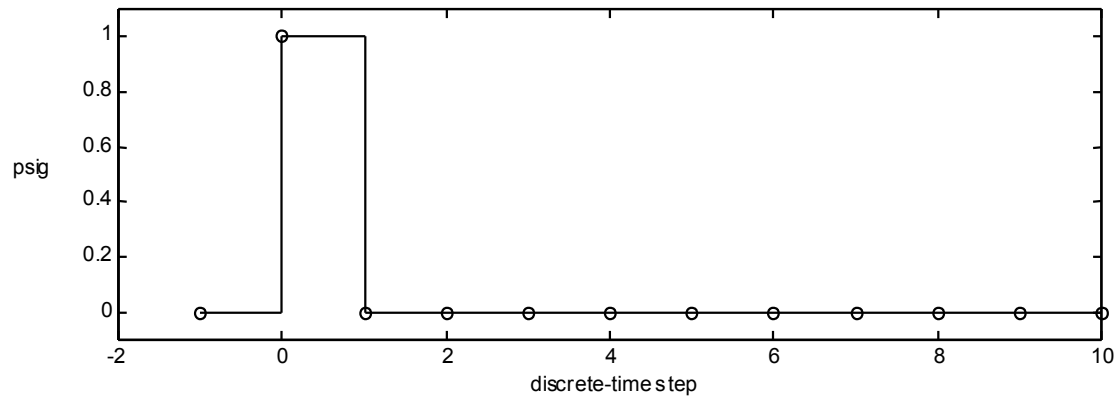
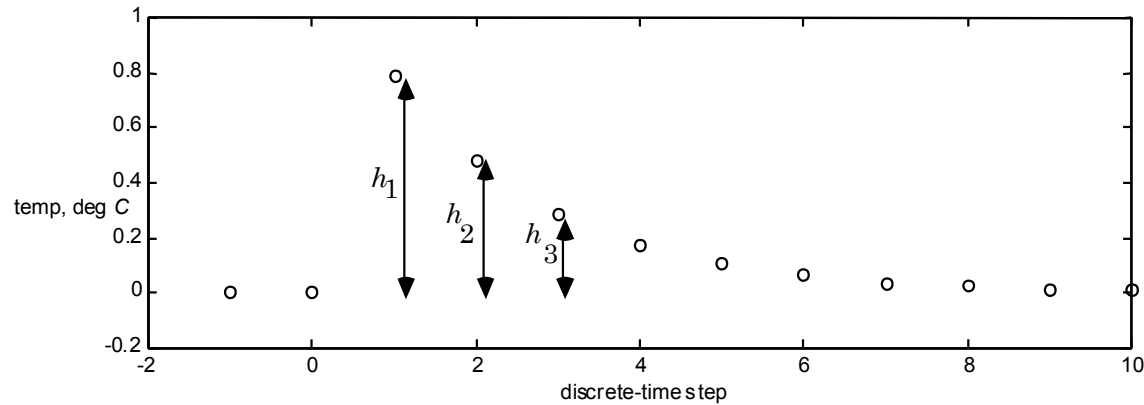
Example Step Response Model



Used in
DMC

$$S = \begin{bmatrix} s_1 & s_2 & s_3 & s_4 & s_5 & \mathbf{L} & s_N \end{bmatrix}^T$$

Example Impulse Response Model



Used in
IDCOM

Impulse and step response
coefficients are related

$$h_i = s_i - s_{i-1}$$

$$s_i = \sum_{j=1}^i h_j$$

Step & Impulse Models from State Space Models

$$x_{k+1} = \Phi x_k + \Gamma u_k$$

$$y_k = Cx_k$$

$$H_i = C\Phi^{i-1}\Gamma$$

$$S_k = \sum_{i=1}^k C\Phi^{i-1}\Gamma = \sum_{i=1}^k H_i$$

MPC based on State Space Models

$$x_{k+1} = \Phi x_k + \Gamma u_k$$

$$y_k = C x_k$$

with known current state, easy to propagate estimates

$$x_{k+1} = \Phi x_k + \Gamma u_k$$

$$y_{k+1} = C x_{k+1} = C \Phi x_k + C \Gamma u_k$$

and, using control changes

$$u_k = u_{k-1} + \Delta u_k$$

$$y_{k+1} = C \Phi x_k + C \Gamma u_{k-1} + C \Gamma \Delta u_k$$

Use ^ notation for model states

Predicted output State estimate Previous input Current Input change

$$\hat{y}_{k+1|k} = C\Phi\hat{x}_{k|k} + C\Gamma u_{k-1} + C\Gamma\Delta u_k$$

Estimate at k+1 Estimate at k Measurements through k

Measurements through k

Now, propagate the prediction for P steps into the future

Output Predictions

$$\underbrace{\begin{bmatrix} \hat{y}_{k+1|k} \\ \hat{y}_{k+2|k} \\ \vdots \\ \hat{y}_{k+P|k} \end{bmatrix}}_{\hat{Y}} = \underbrace{\begin{bmatrix} C\Phi \\ C\Phi^2 \\ \vdots \\ C\Phi^P \end{bmatrix}}_{\text{"free" or "unforced response" (if no more control moves are made)}} \hat{x}_{k|k} + \underbrace{\begin{bmatrix} C\Gamma \\ C\Phi\Gamma + C\Gamma \\ \vdots \\ \sum_{i=1}^P C\Phi^{i-1}\Gamma \end{bmatrix}}_{\text{"forced" response}} u_{k-1}$$

$$f \begin{bmatrix} C\Gamma & 0 & \dots & 0 \\ C\Phi\Gamma + C\Gamma & C\Gamma & 0 & 0 \\ \vdots & \vdots & & \\ \sum_{i=1}^P C\Phi^{i-1}\Gamma & \sum_{i=1}^{P-1} C\Phi^{i-1}\Gamma & \dots & \end{bmatrix} \begin{bmatrix} \Delta u_k \\ \Delta u_{k+1} \\ \vdots \\ \Delta u_{k+M-1} \end{bmatrix} \rightarrow \Delta u_f$$

"forced" response

S_f

Output Predictions

$$\underbrace{\begin{bmatrix} \hat{y}_{k+1|k} \\ \hat{y}_{k+2|k} \\ \vdots \\ \hat{y}_{k+P|k} \end{bmatrix}}_{\hat{Y}} = \underbrace{\begin{bmatrix} C\Phi \\ C\Phi^2 \\ \vdots \\ C\Phi^P \end{bmatrix} \hat{x}_{k|k} + \begin{bmatrix} S_1 \\ S_2 \\ \vdots \\ S_P \end{bmatrix} u_{k-1}}_{\text{"free" or "unforced response" (if no more control moves are made)}}$$

Step response coefficients

$$f \begin{bmatrix} S_1 & 0 & \cdots & 0 \\ S_2 & S_1 & 0 & 0 \\ \vdots & \vdots & & \\ S_P & S_{P-1} & \cdots & S_{P-M+1} \end{bmatrix} \begin{bmatrix} \Delta u_k \\ \Delta u_{k+1} \\ \vdots \\ \Delta u_{k+M-1} \end{bmatrix}$$

"forced" response

S_f Δu_f

Optimization Problem

$$\min_{\Delta u_f} J = \underbrace{\sum_{i=1}^P (r_{k+i|k} - \hat{y}_{k+i|k})^T W^y (r_{k+i|k} - \hat{y}_{k+i|k})}_{\hat{E}^T W^Y \hat{E}} + \underbrace{\sum_{i=0}^{M-1} \Delta u_{k+i}^T W^u \Delta u_{k+i}}_{\Delta u_f^T W^U \Delta u_f}$$

Where

$$W^Y = \begin{bmatrix} W^y & 0 & 0 \\ 0 & \ddots & 0 \\ 0 & 0 & W^y \end{bmatrix} \quad W^U = \begin{bmatrix} W^u & 0 & 0 \\ 0 & \ddots & 0 \\ 0 & 0 & W^u \end{bmatrix}$$

future setpoints

and

$$\hat{E} = r - \hat{Y} = \underbrace{r - f}_E - S_f \Delta u_f$$

“unforced” (free response) error

so

$$\hat{E} = E - S_f \Delta u_f$$

Optimization Problem

$$\begin{aligned}\hat{E}^T W^Y \hat{E} &= (E - S_f \Delta u_f)^T W^Y (E - S_f \Delta u_f) \\ &= E^T W^Y E - 2\Delta u_f^T S_f^T W^Y E + \Delta u_f^T S_f^T W^Y S_f \Delta u_f\end{aligned}$$

so

$$\min_{\Delta u_f} J = \hat{E}^T W^Y \hat{E} + \Delta u_f^T W^U \Delta u_f$$

can be written

$$\min_{\Delta u_f} J = \Delta u_f^T (S_f^T W^Y S_f + W^U) \Delta u_f - 2\Delta u_f^T S_f^T W^Y E$$

and the unconstrained solution is found from

$$\partial J / \partial \Delta u_f = 0$$

Unconstrained Solution

Analytical Solution for Unconstrained System

$$\Delta u_f = \left(S_f^T W^Y S_f + W^U \right)^{-1} S_f^T W^Y E$$

“unforced” error



In practice, do not actually invert a matrix. Solve as set of simultaneous equations (or use \ in MATLAB)

$$\Delta u_f = \left(S_f^T W^Y S_f + W^U \right) \backslash S_f^T W^Y E$$

Vector of Control Moves

$$\Delta u_f = \begin{bmatrix} \Delta u_k \\ \Delta u_{k+1} \\ \vdots \\ \Delta u_{k+M-1} \end{bmatrix}$$

current and future moves

Although a set of control moves is computed, only the first move Δu_k is implemented

The next output at $k+1$ is obtained, then a new optimization problem is solved

MPC Tuning Parameters

- Prediction Horizon, P
- Control Horizon, M
- Manipulated Input Weighting, W^u

Usually, **$P \gg M$** for robustness (less aggressive action). Sometimes $M = 1$, with P varied for desired performance.

Sometimes larger input weights for robustness

Pre-Summary

- Concise overview of MPC
- State space model, unconstrained solution
- Have not discussed
 - State estimation and “**corrected outputs**”
 - **The additive disturbance assumption of DMC is covered in the slides that follow (this is identical to the plant-model mismatch term in IMC)**
 - Disturbances
 - Constraints
 - Other model forms

Original DMC Approach to Plant-Model Mismatch

$$\hat{x}_{k|k-1} = \Phi \hat{x}_{k-1|k-1} + \Gamma u_{k-1}$$

$$\hat{y}_{k|k-1} = C \hat{x}_{k|k-1}$$

Prediction at step k, based on information at k-1

Measured output

$$\hat{p}_{k|k} = y_k - \hat{y}_{k|k-1}$$

Model output predicted from k-1

“additive output” disturbance assumption (previously d_k)

$$\hat{y}_{k|k} = \hat{y}_{k|k-1} + \hat{p}_{k|k}$$

Forces the model “corrected output” equal to measured output

Notice that Model States are Not “Corrected”

$$\hat{x}_{k|k} = \hat{x}_{k|k-1}$$

Model Prediction to k+1

$$\hat{x}_{k+1|k} = \Phi \hat{x}_{k|k} + \Gamma u_k$$

$$\hat{p}_{k+1|k} = \hat{p}_{k|k}$$

Assumes future corrections
equal to current correction

$$\hat{y}_{k+1|k} = C \hat{x}_{k+1|k} + \hat{p}_{k+1|k} =$$

$$= C \Phi \hat{x}_{k|k} + C \Gamma u_k + \hat{p}_{k+1|k}$$

$$= C \Phi \hat{x}_{k|k} + C \Gamma u_{k-1} + C \Gamma \Delta u_k + \hat{p}_{k+1|k}$$

Continue Output Predictions

$$\underbrace{\begin{bmatrix} \hat{y}_{k+1|k} \\ \hat{y}_{k+2|k} \\ \vdots \\ \hat{y}_{k+P|k} \end{bmatrix}}_{\hat{Y}} = \underbrace{\begin{bmatrix} C\Phi \\ C\Phi^2 \\ \vdots \\ C\Phi^P \end{bmatrix} \hat{x}_{k|k} + \begin{bmatrix} I \\ I \\ \vdots \\ I \end{bmatrix} \hat{p}_{k|k} + \begin{bmatrix} C\Gamma \\ C\Phi\Gamma + C\Gamma \\ \vdots \\ \sum_{i=1}^P C\Phi^{i-1}\Gamma \end{bmatrix} u_{k-1}}_{\text{"free" or "unforced response" (if no more control moves are made)}}$$

$$\begin{matrix} f \\ \\ S_f \end{matrix} \begin{bmatrix} C\Gamma & 0 & \dots & 0 \\ C\Phi\Gamma + C\Gamma & C\Gamma & 0 & 0 \\ \vdots & \vdots & & \\ \sum_{i=1}^P C\Phi^{i-1}\Gamma & \sum_{i=1}^{P-1} C\Phi^{i-1}\Gamma & \dots & \end{bmatrix} \begin{bmatrix} \Delta u_k \\ \Delta u_{k+1} \\ \vdots \\ \Delta u_{k+M-1} \end{bmatrix} \rightarrow \Delta u_f$$

"forced" response

Output Predictions

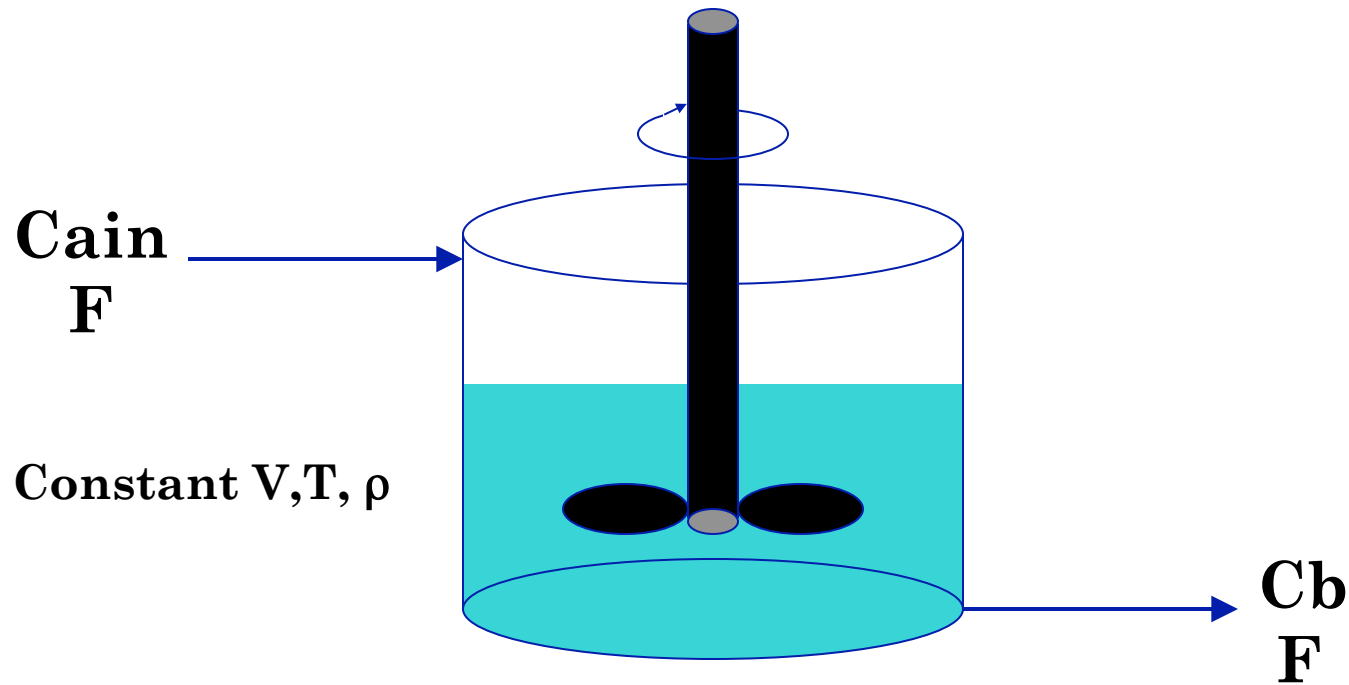
$$\underbrace{\begin{bmatrix} \hat{y}_{k+1|k} \\ \hat{y}_{k+2|k} \\ \vdots \\ \hat{y}_{k+P|k} \end{bmatrix}}_{\hat{Y}} = \underbrace{\begin{bmatrix} C\Phi \\ C\Phi^2 \\ \vdots \\ C\Phi^P \end{bmatrix} \hat{x}_{k|k} + \begin{bmatrix} I \\ I \\ \vdots \\ I \end{bmatrix} \hat{p}_{k|k} + \begin{bmatrix} S_1 \\ S_2 \\ \vdots \\ S_P \end{bmatrix} u_{k-1}}_{\text{"free" or "unforced response" (if no more control moves are made)}}$$

$$f \begin{bmatrix} S_1 & 0 & \cdots & 0 \\ S_2 & S_1 & 0 & 0 \\ \vdots & \vdots & & \\ S_P & S_{P-1} & \cdots & S_{P-M+1} \end{bmatrix} \begin{bmatrix} \Delta u_k \\ \Delta u_{k+1} \\ \vdots \\ \Delta u_{k+M-1} \end{bmatrix}$$

"forced" response

S_f Δu_f

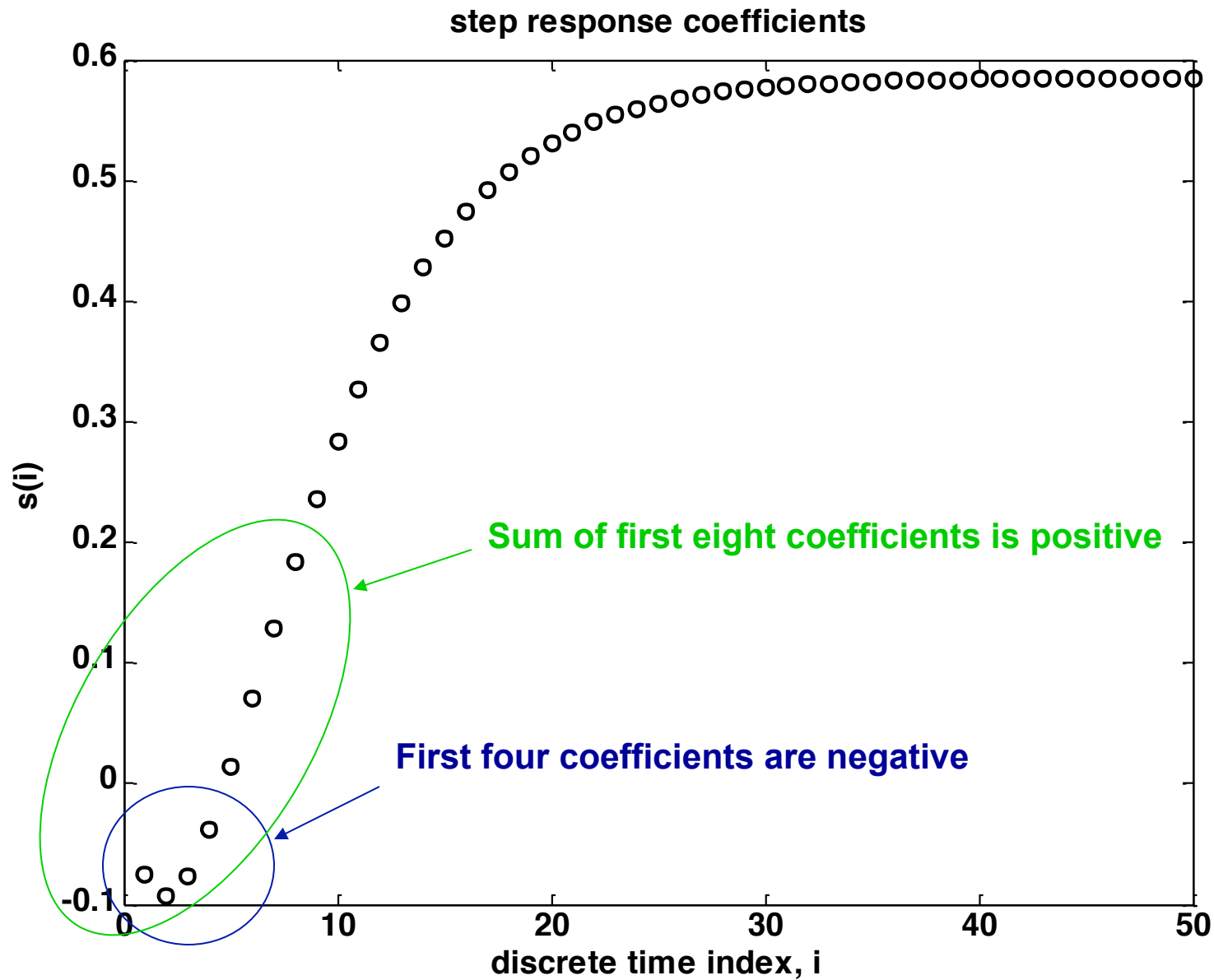
Example **Inverse Response** Process: Van de Vusse



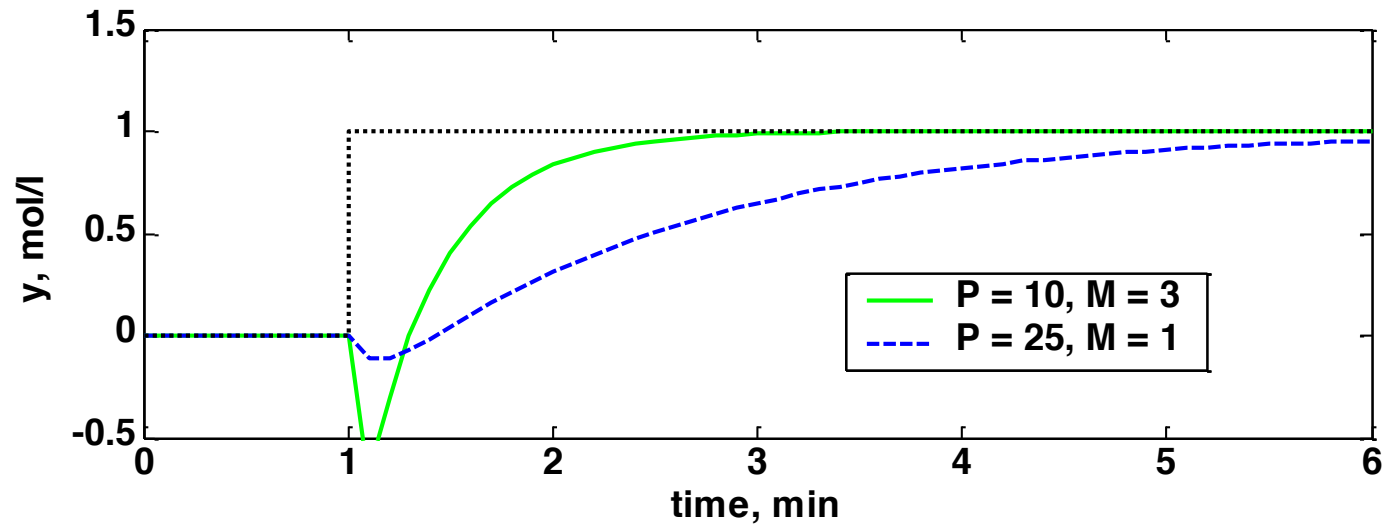
$$\frac{dC_a}{dt} = -k_1 C_a - k_3 C_a^2 + (C_{a_{in}} - C_a)u$$

$$\frac{dC_b}{dt} = k_1 C_a - k_2 C_b - C_b u \quad \text{where } u = F/V$$

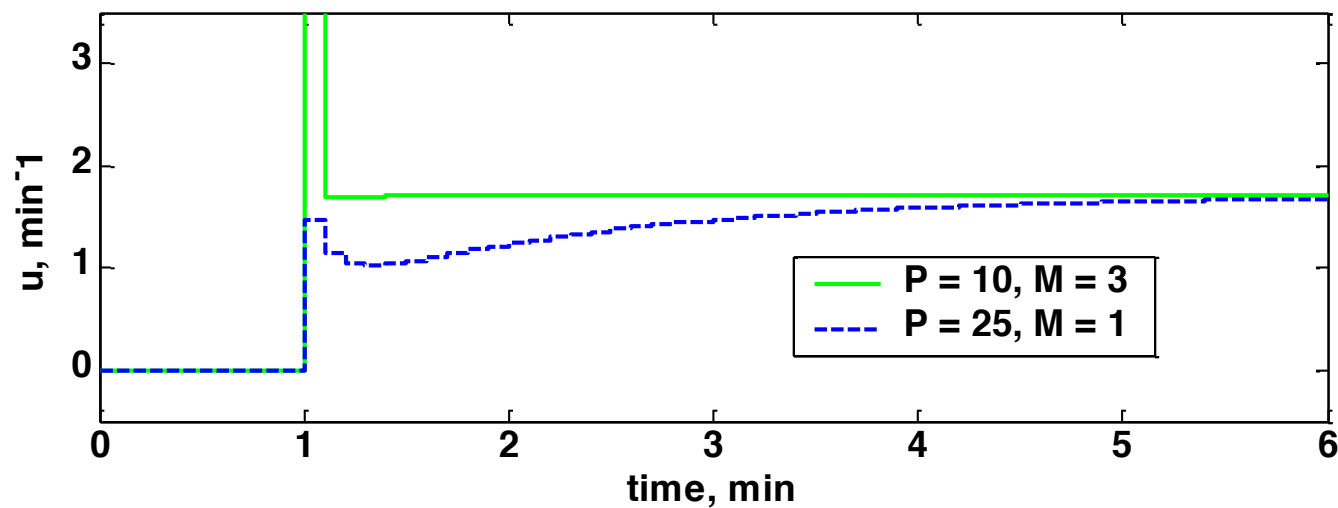
Example: Inverse Response Process



Closed-Loop: Compare $P=10, M=1$ with $P=25, M=1$

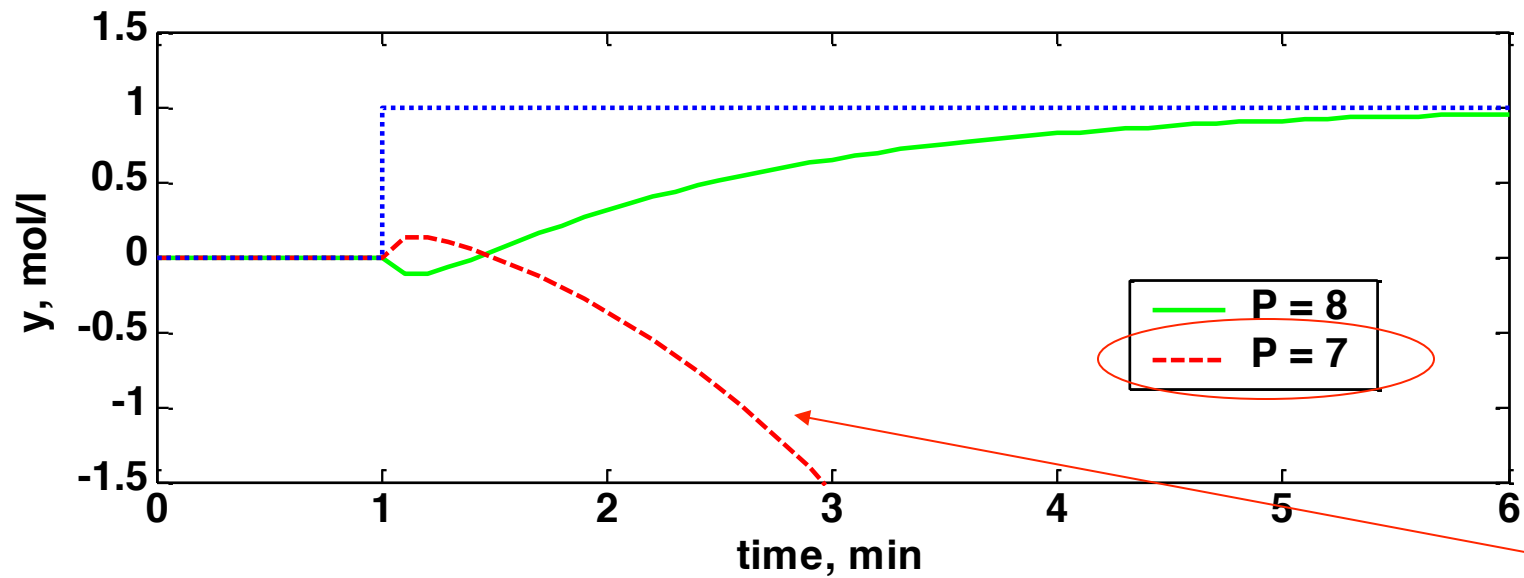


Short prediction horizons & long control horizons lead to more aggressive action

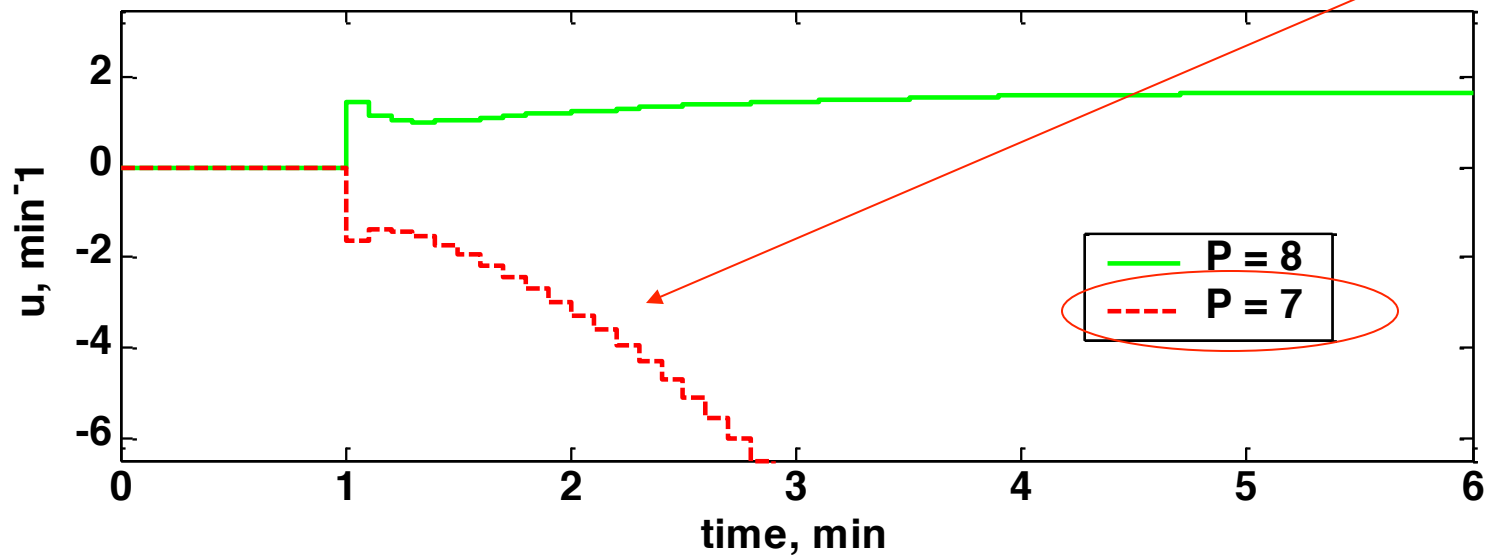


Results

Control Horizon: $M = 1$, Weighting: $W = 0$



**P=7:
Unstable**



Stability of Inverse Response Systems with DMC

- For a control horizon, $M = 1$, closed-loop MPC will be stable for a prediction horizon where the sum of the impulse response coefficients has the same sign as the process gain

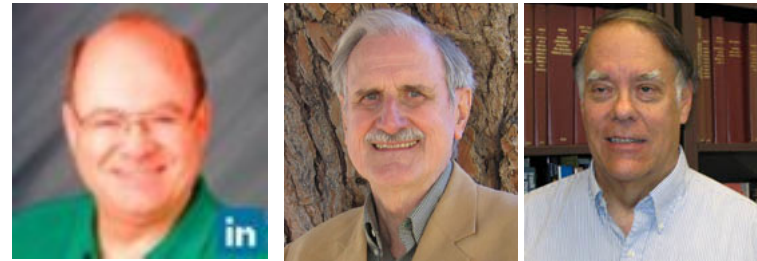
$$\sum_{i=1}^{P_{\min}} s_i > 0$$

Predictive Controller Design for Single-Input/Single-Output (SISO) Systems

Paul R. Maurath,[†] Duncan A. Mellichamp, and Dale E. Seborg*

Department of Chemical and Nuclear Engineering, University of California, Santa Barbara, Santa Barbara, California 93106

Ind. Eng. Chem. Res. 1988, 27, 956–963



For the example, $P_{\min} = 8$, so $P = 7 = \text{unstable}$

Summary

- Concise overview of MPC
- State space model, unconstrained solution
- The additive disturbance assumption of DMC is used for plant-model mismatch
- Upcoming topics
 - Disturbances and state estimation (Kalman filtering framework)
 - Constraints
 - Other model forms