

New results for divided-wall columns

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North Sea

Arctic circle

Trondheim

NORWAY

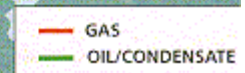
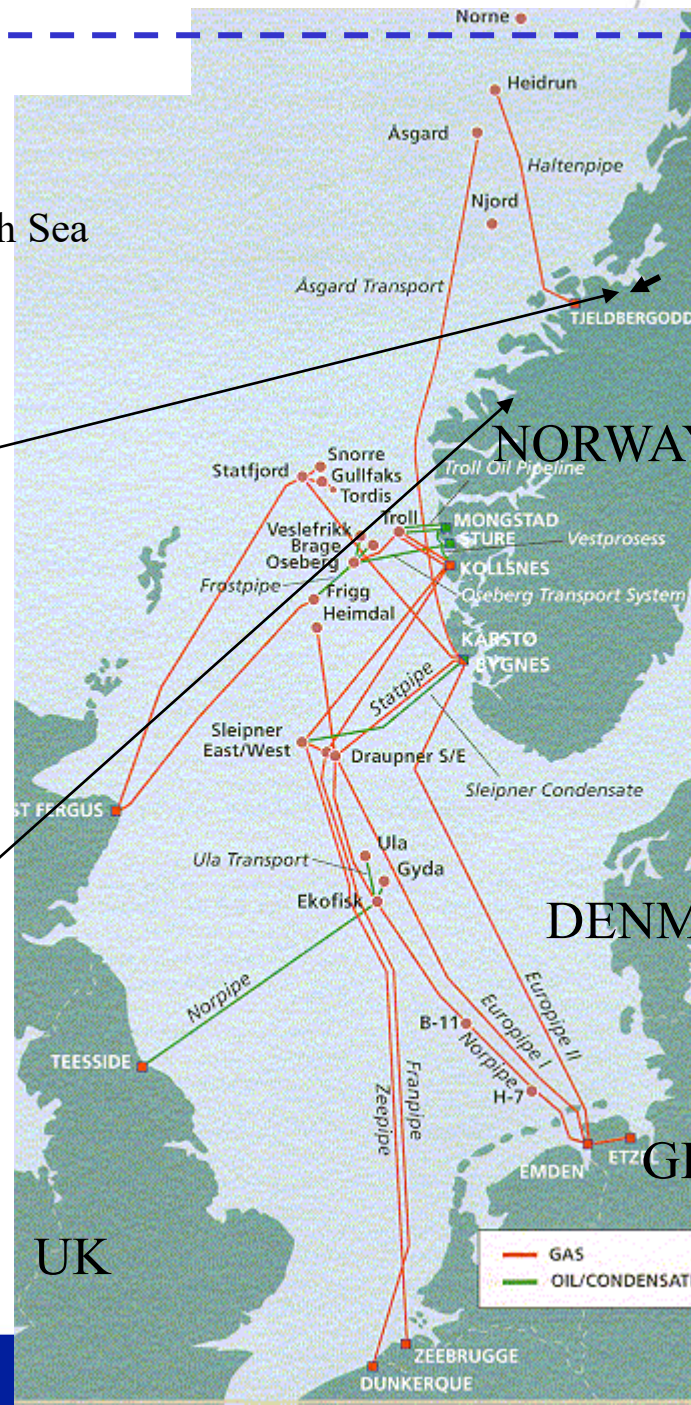
SWEDEN

Oslo

DENMARK

GERMANY

UK

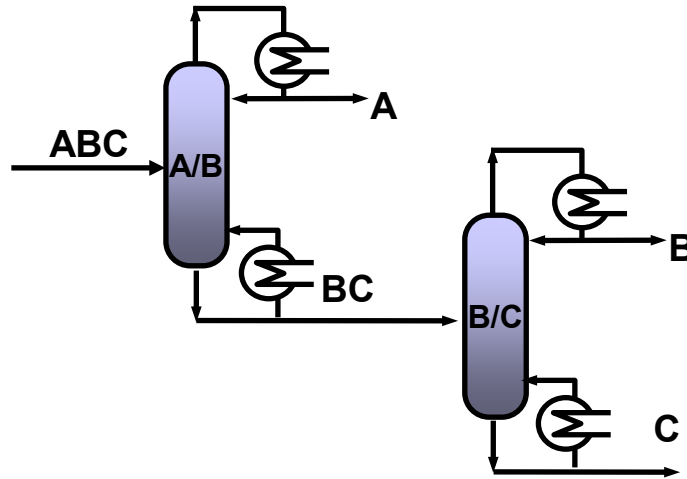


Norwegian University of Science and Technology

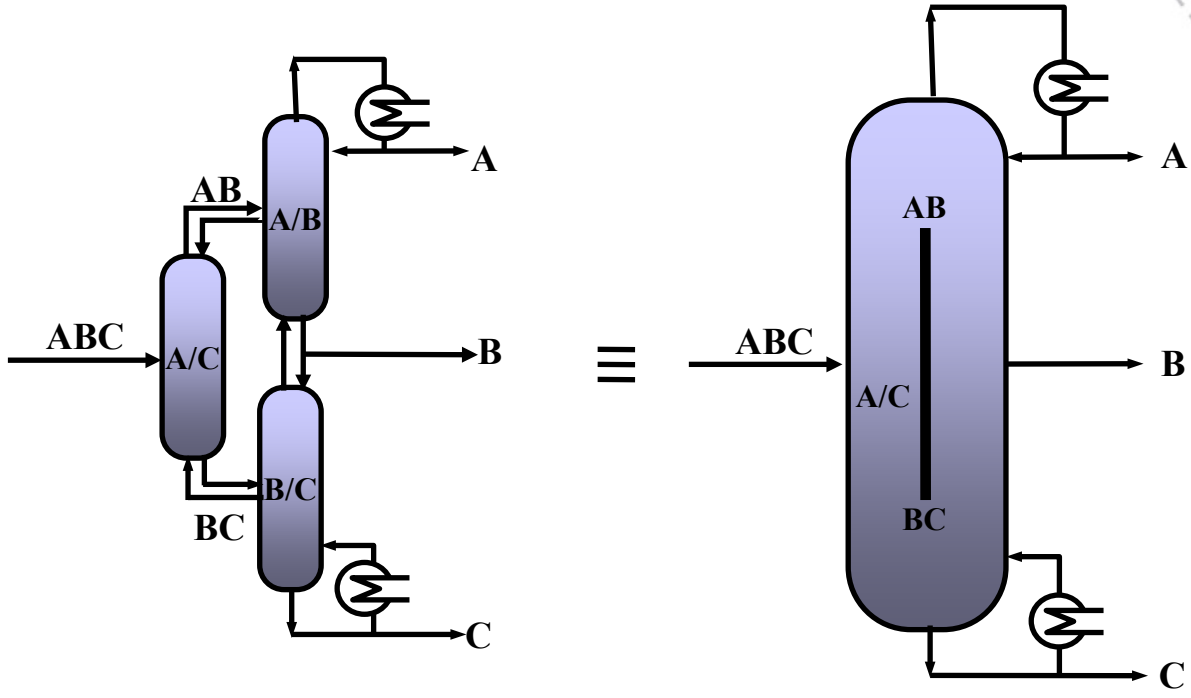
Outline

- **Introduction: Divided wall columns for 3- and 4-product separations**
 - Structures
 - “ V_{\min} diagrams”
- **Experiments: 4- Product Kaibel Column**
 - Experimental Setup
 - Control Structure
 - Experimental Runs- Steady state profiles
 - Experimental data- model fitting
 - Experimental Runs- Vapor Split Experiment
- **Conclusions**

3-product separation: Conventional “direct split”⁵

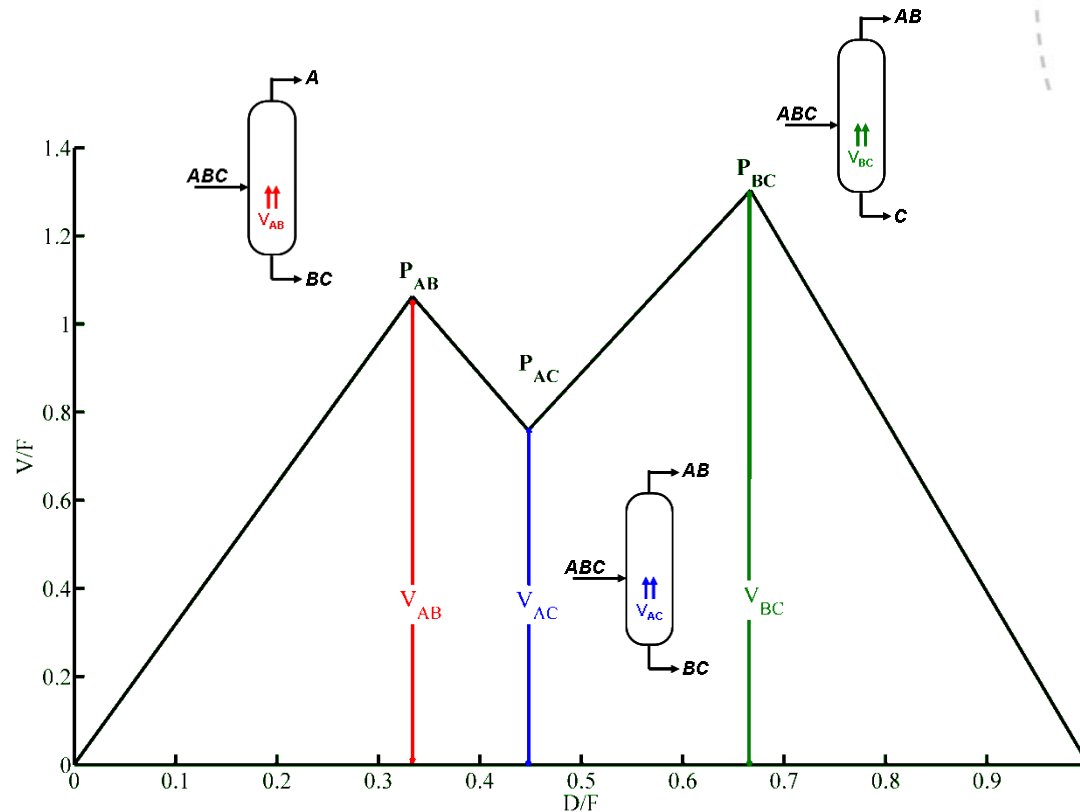


Simplification: Direct coupling (“Petlyuk”) + single shell (divided wall column)



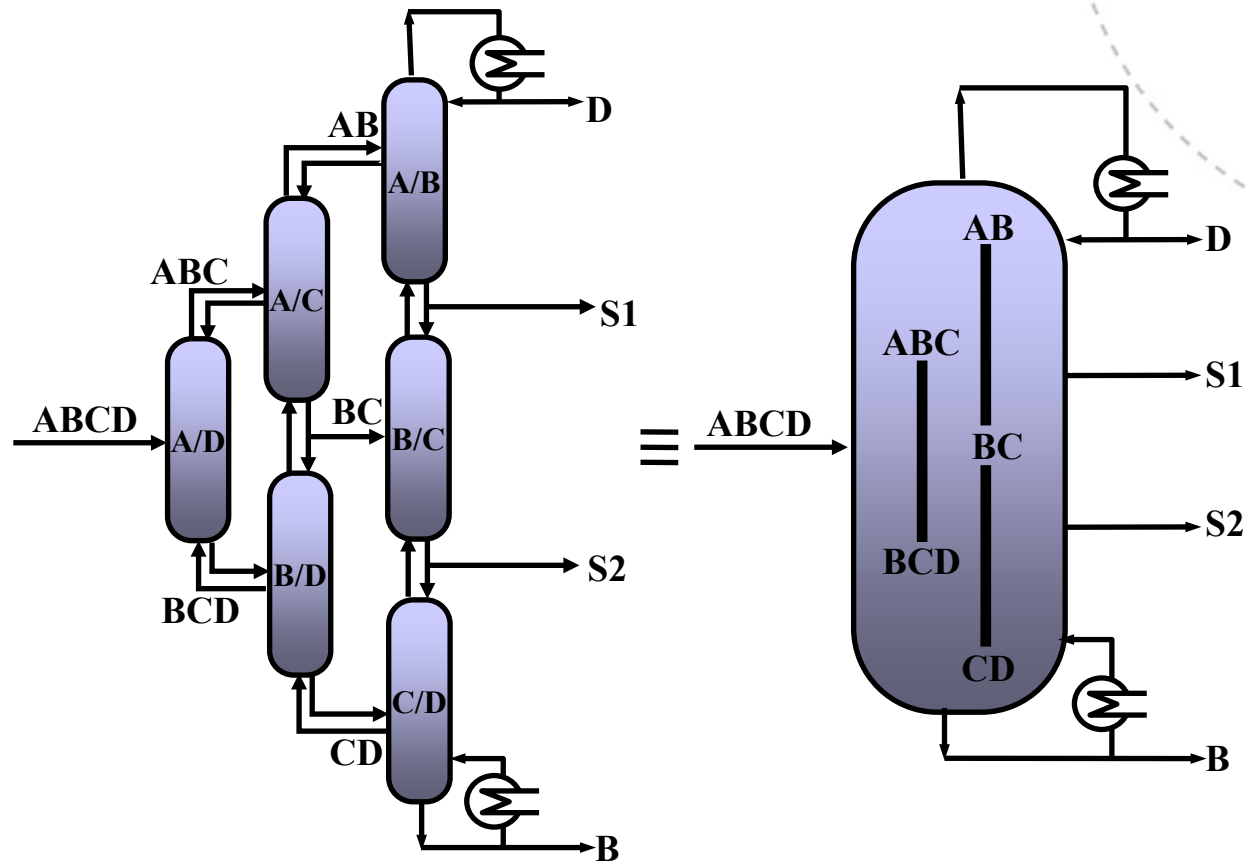
Petlyuk column

V_{\min} diagram for three components



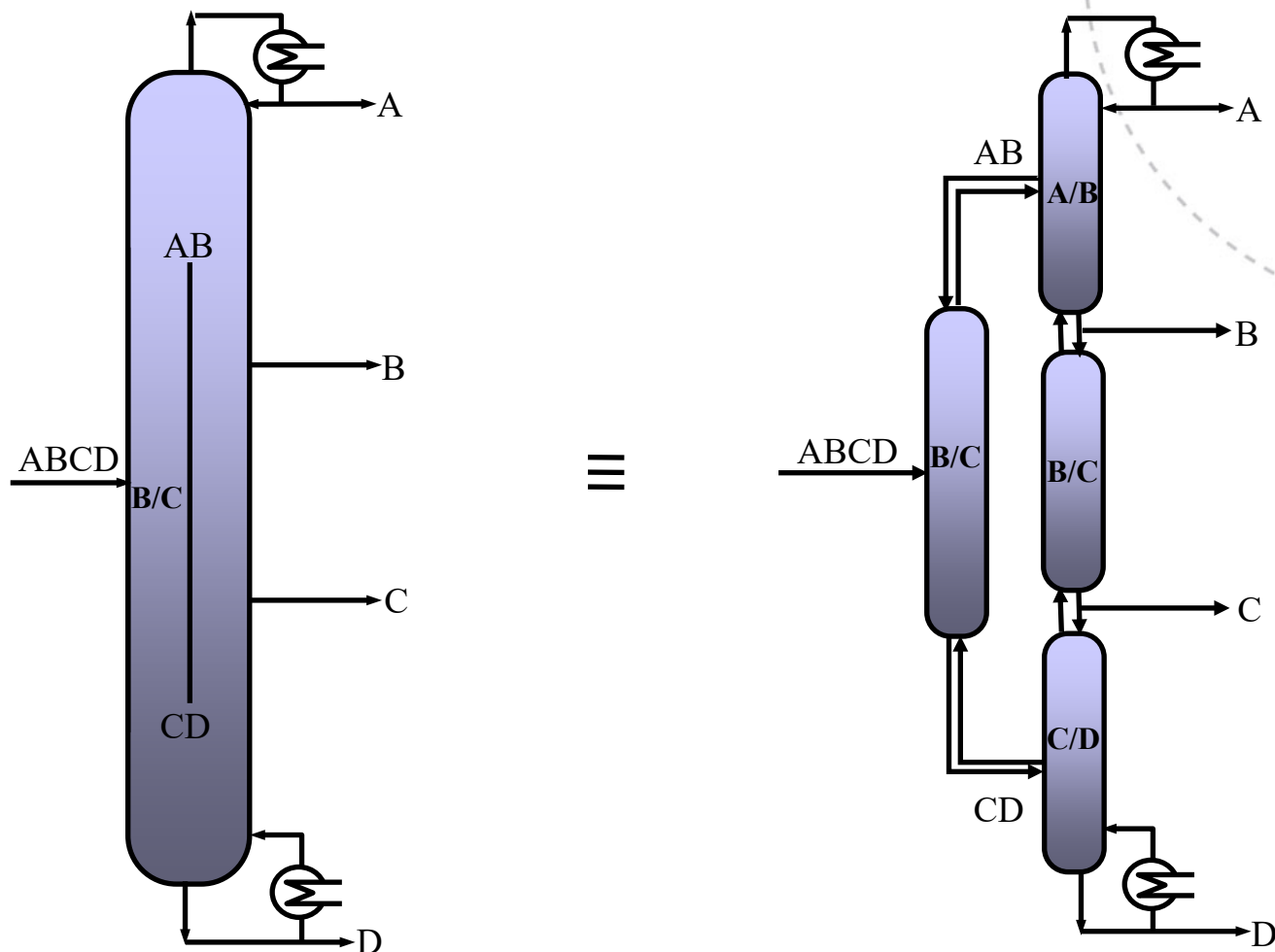
- $V_{\min} | \text{Petlyuk} = \max(V_{AB}, V_{BC}) = V_{BC}$
- $V_{\text{Prefractionator}} = V_{AC}$

4-product separation: Extended Petlyuk



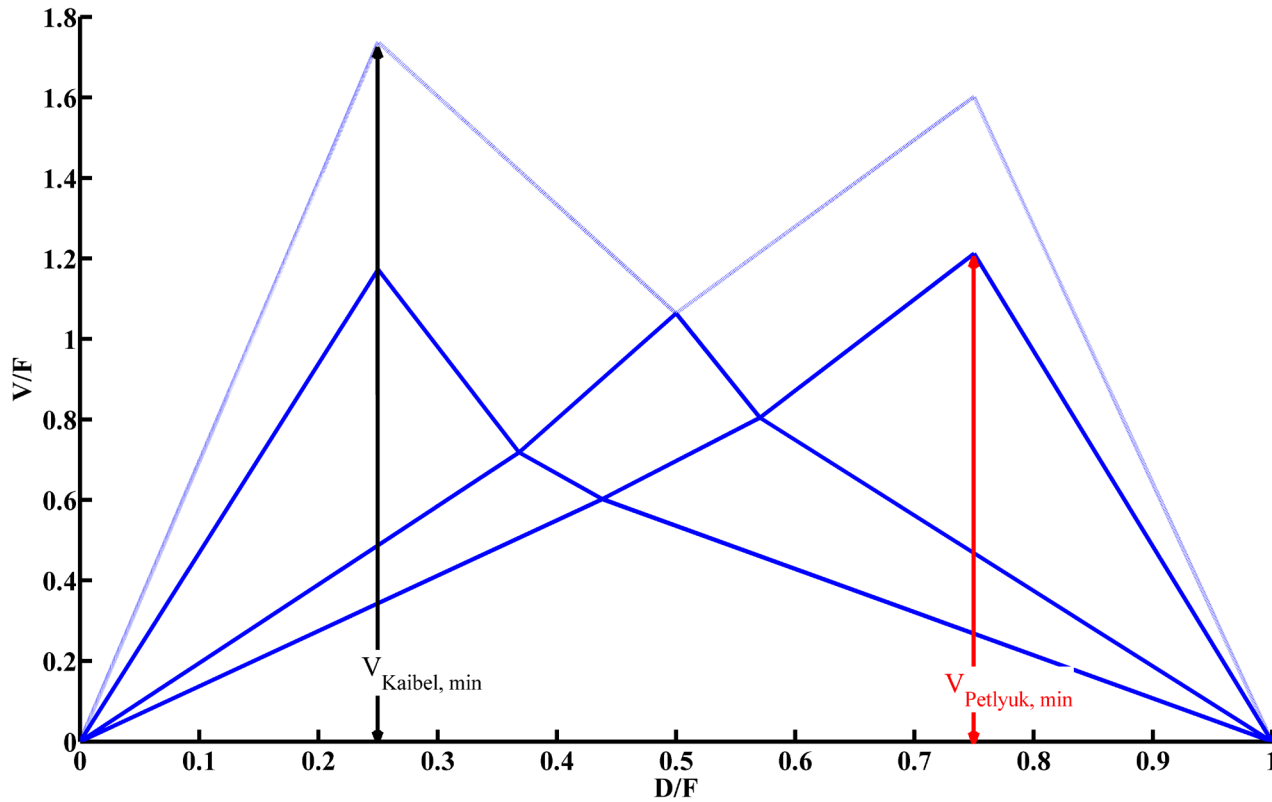
4-product extended Petlyuk column up to ~50 % energy savings

4-product separation: Simplified (“Kaibel column”)



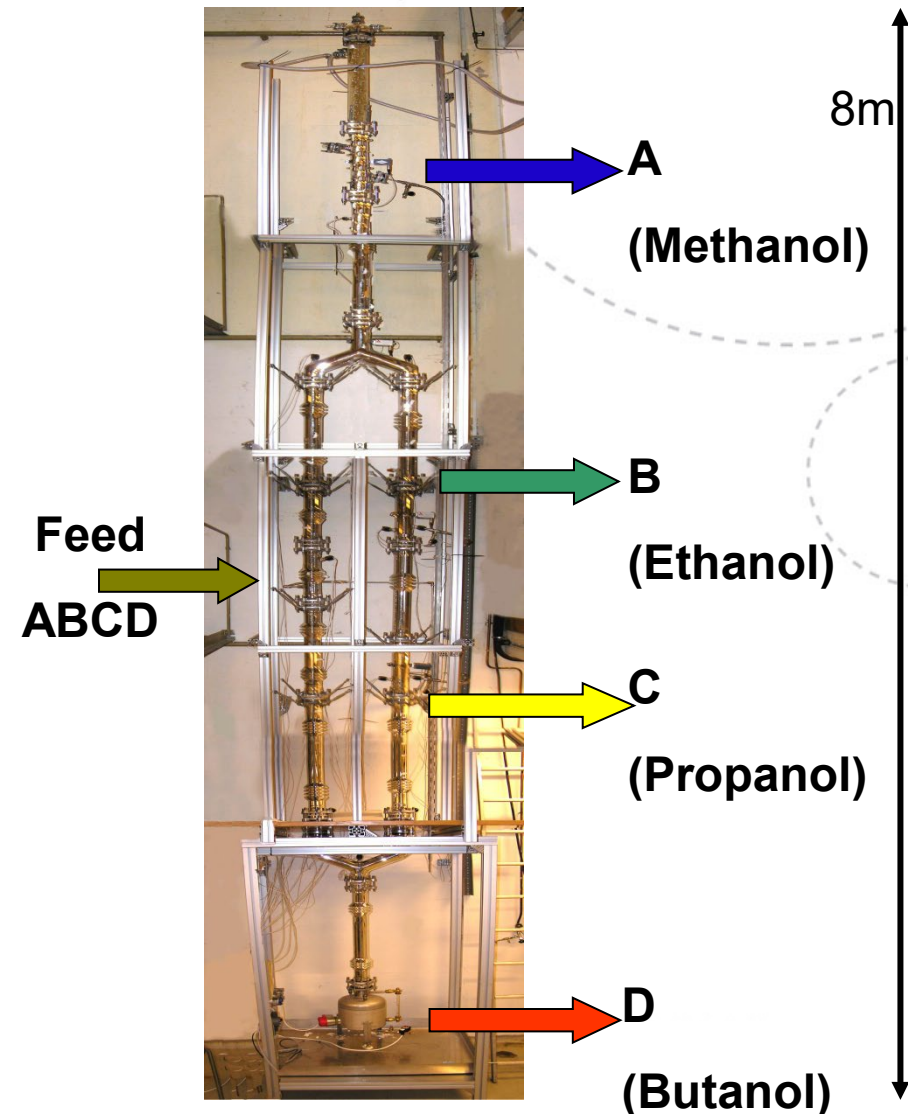
4-product extended Kaibel column up to ~30 % energy savings

V_{\min} diagram for four components

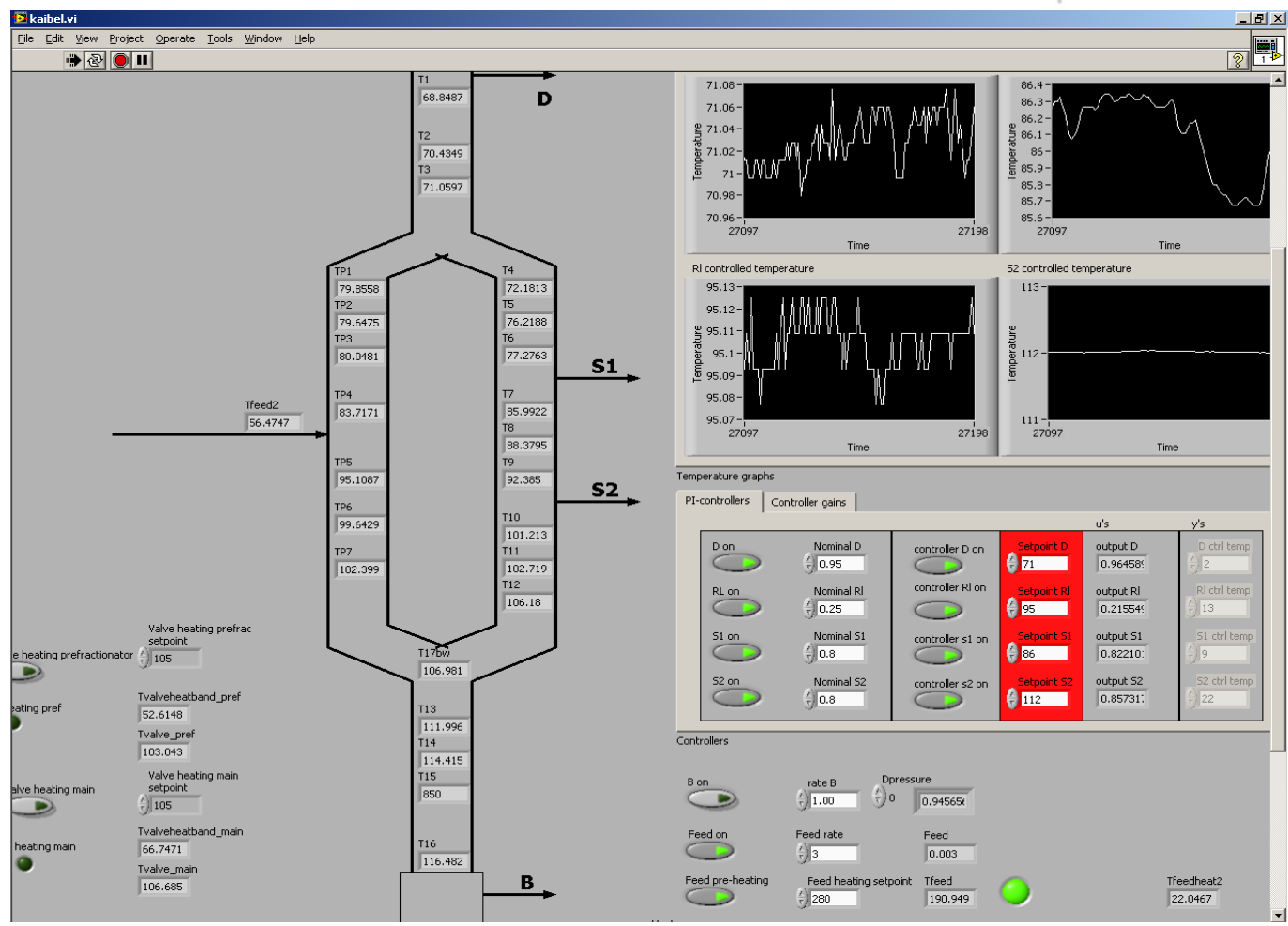


Experimental Set up

- 4 products
- Packed Column
- Magnetic funnel-liquid split & Product valves
- Number of theoretical stages (experimentally determined):
 - Prefractionator: 13
 - Main column : 21

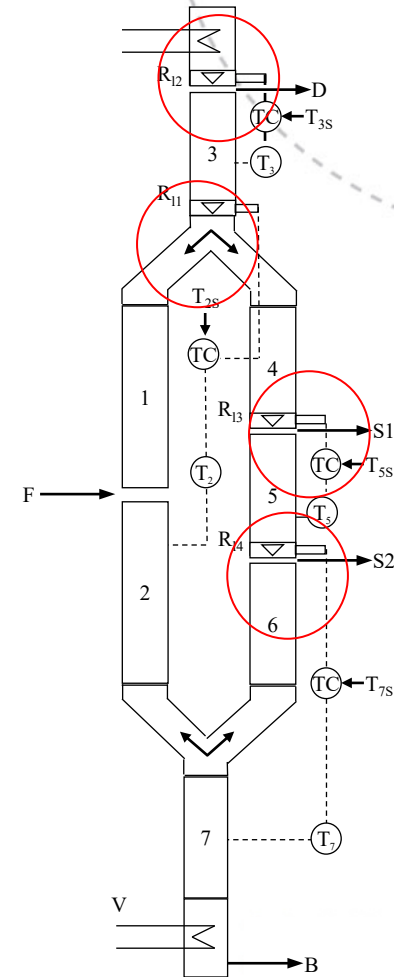


Experimental Set up (Labview Interface)...



Control Structure (As used in experiments)

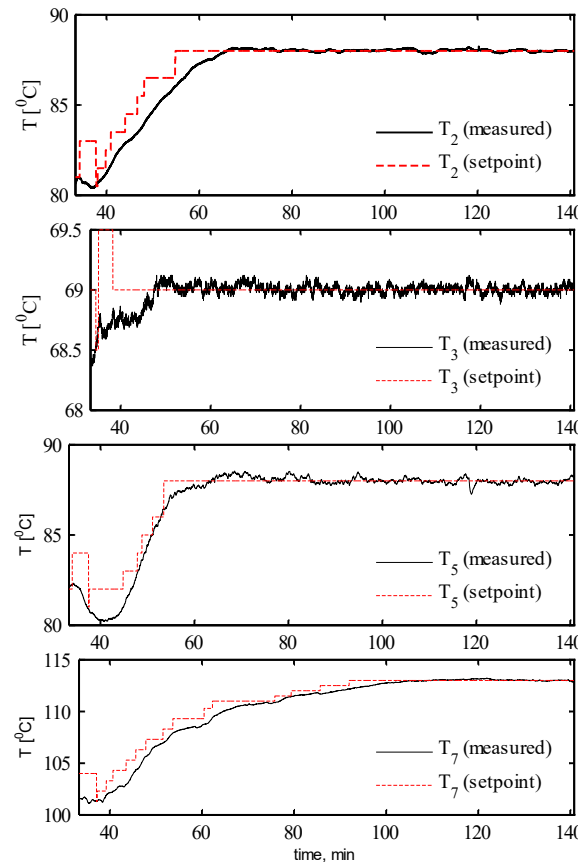
- Boilup $V = \text{constant}$
- 4 control degrees of freedom:
 - Liquid split ratio R_{L1} ,
 - Reflux ratio R_{L2} (top)
 - Reflux ratio R_{L3} (middle)
 - Reflux ratio R_{L4} (bottom)
- Decentralized Control with 4 PI Temperature Controllers:
 - T_{2s} is adjusted to get large temperature change in the prefractionator
 - T_{3s} , T_{5s} , T_{7s} is adjusted to get the temperature of product stages close to the boiling points of their main components



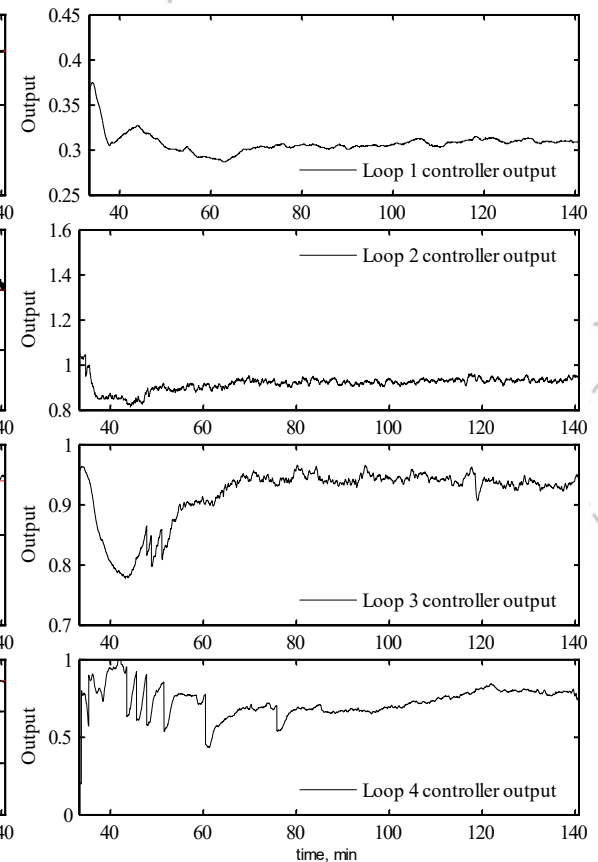
Start-up

- T_{2s} is adjusted to get large temperature change in the prefractionator
- T_{3s} , T_{5s} , T_{7s} is adjusted to get the temperature of product stages close to the boiling points of their main components

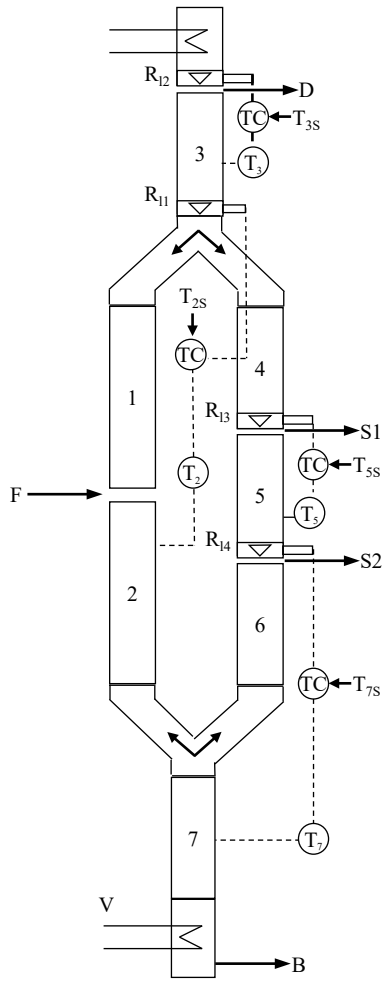
Temperatures



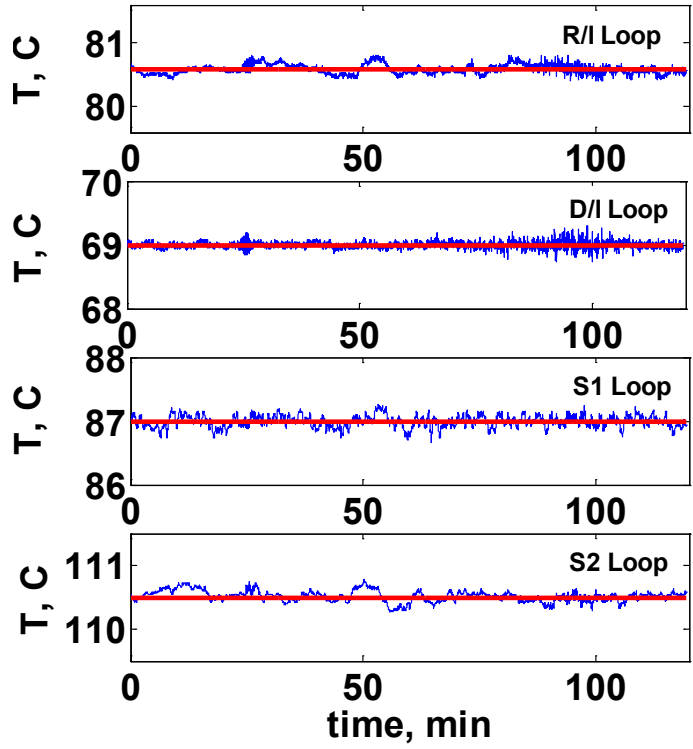
Reflux ratios



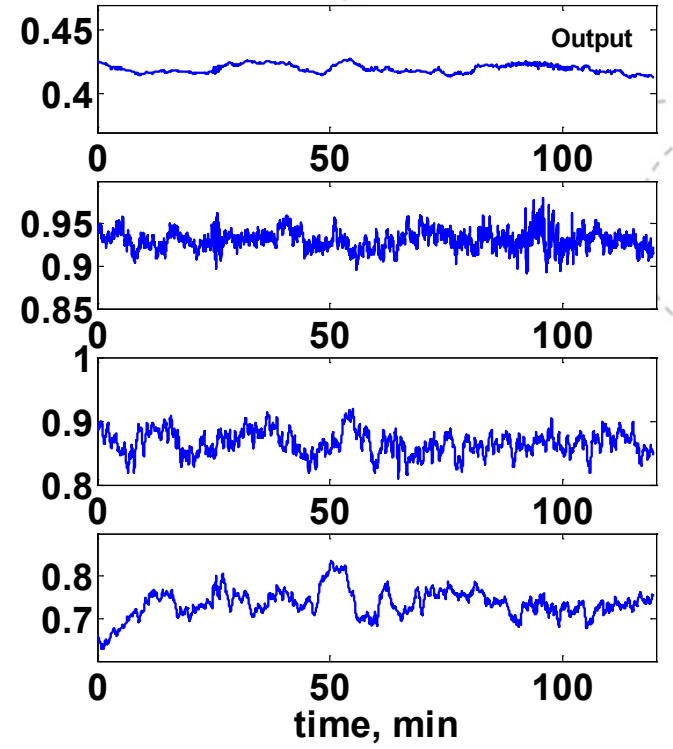
Steady Profiles with 4 temperature loops



TEMPERATURES

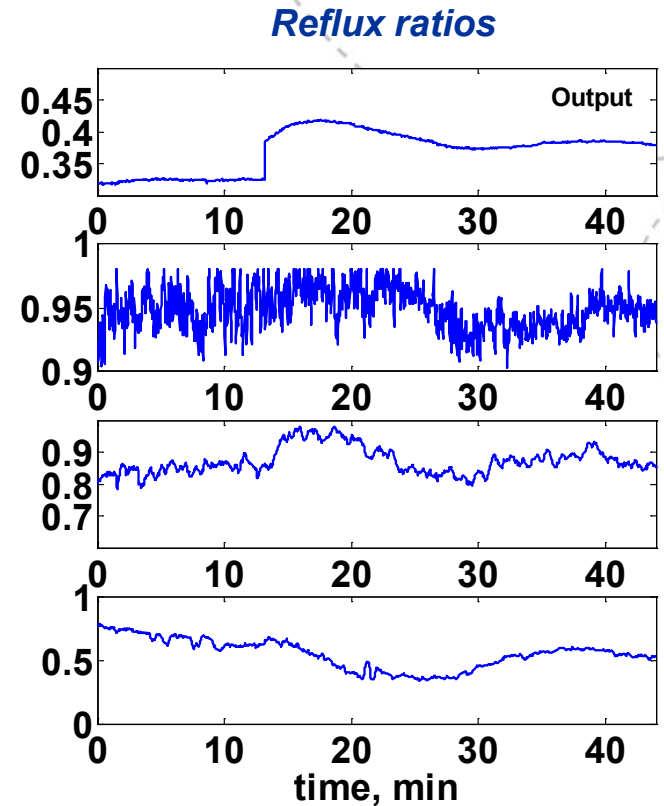
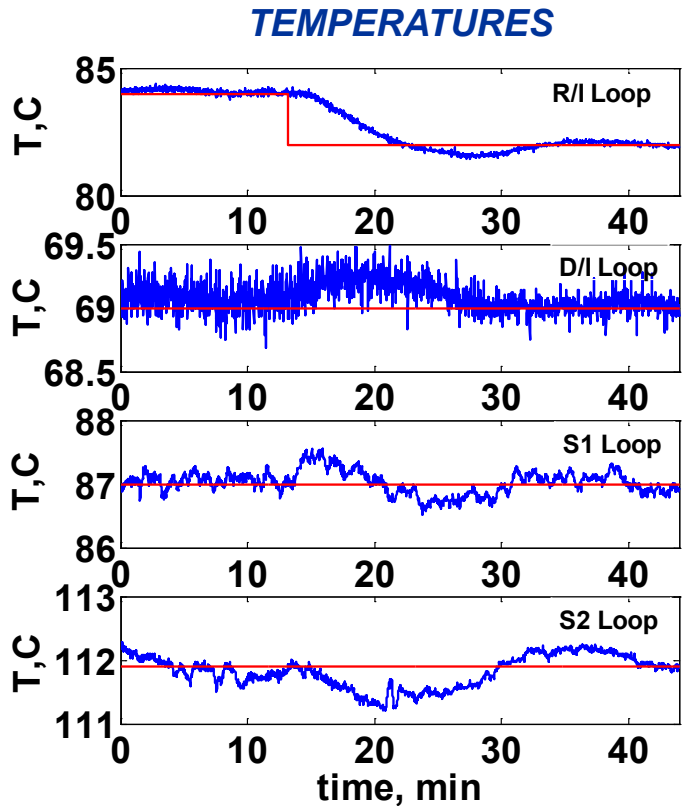
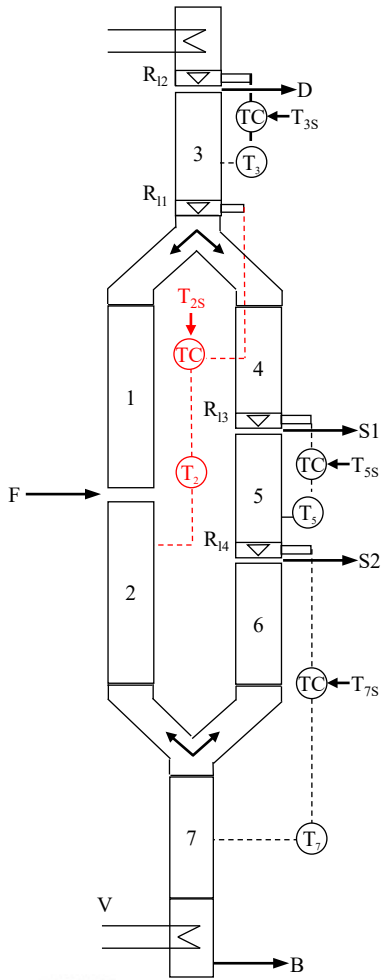


Reflux ratios



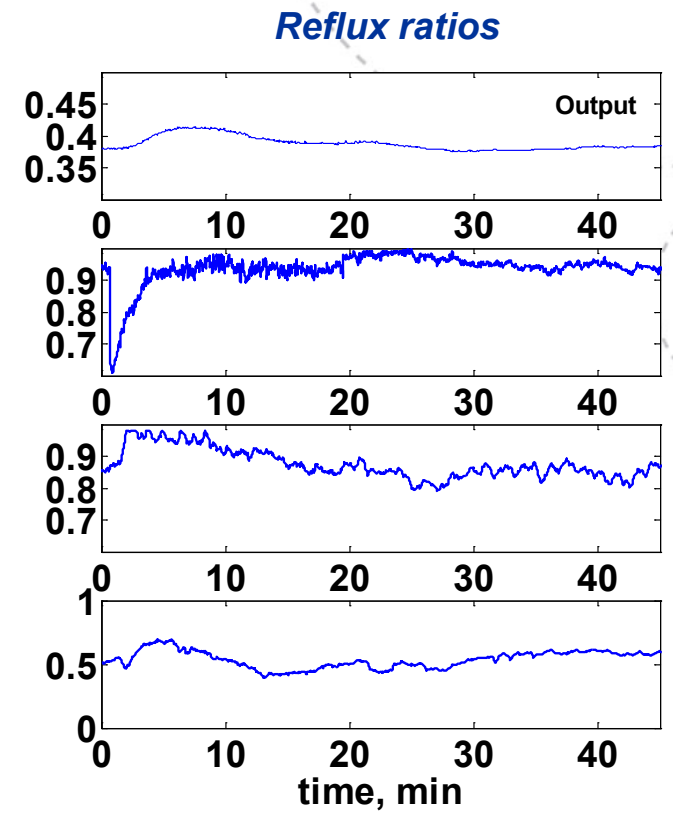
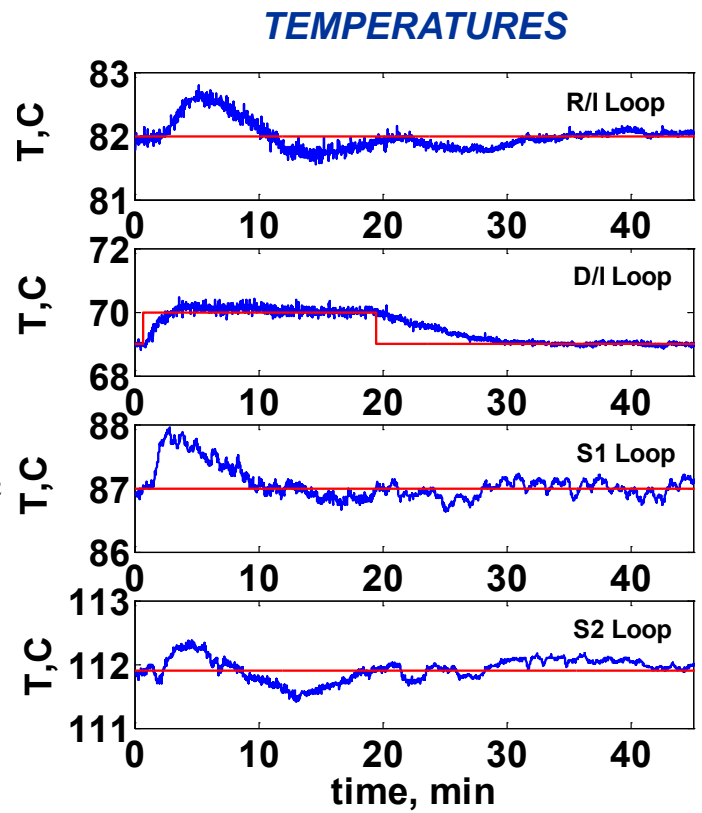
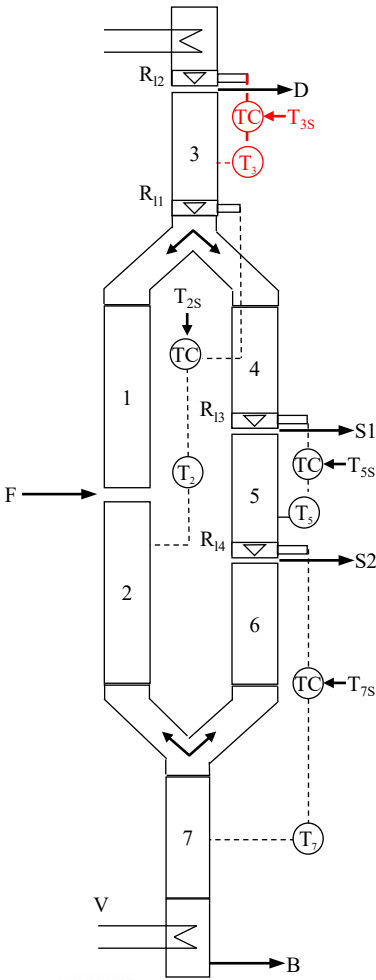
Steady Profiles with 4 temperature loops..

Liquid Split Loop -2 C



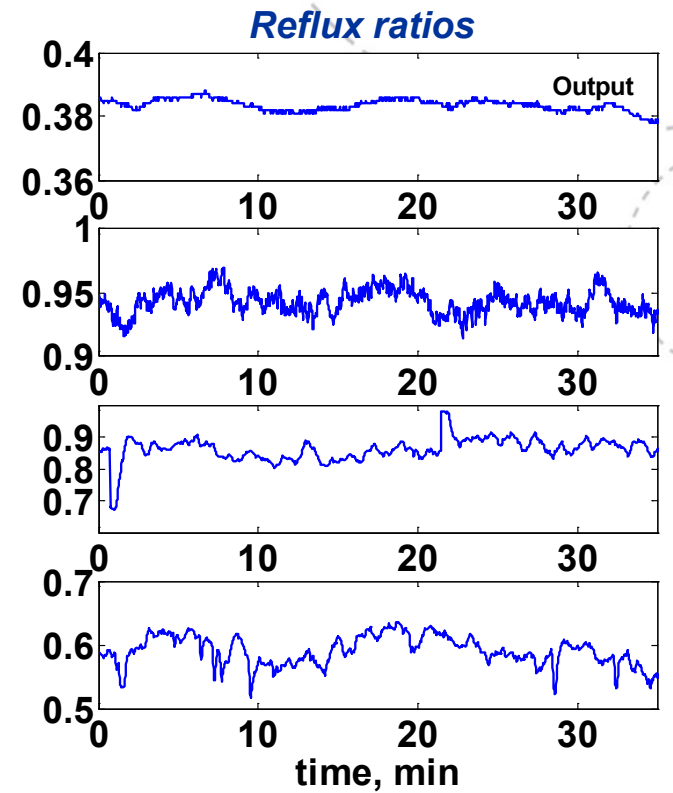
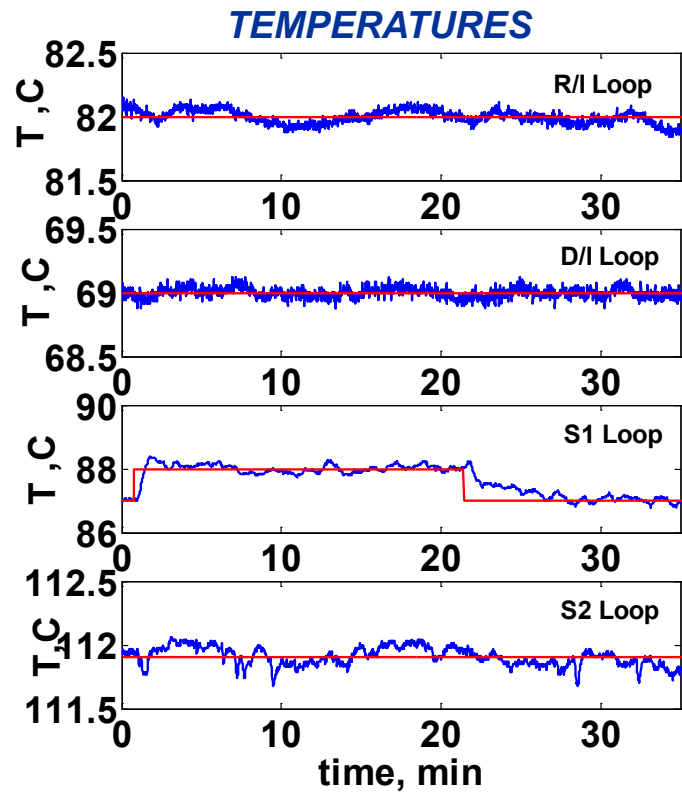
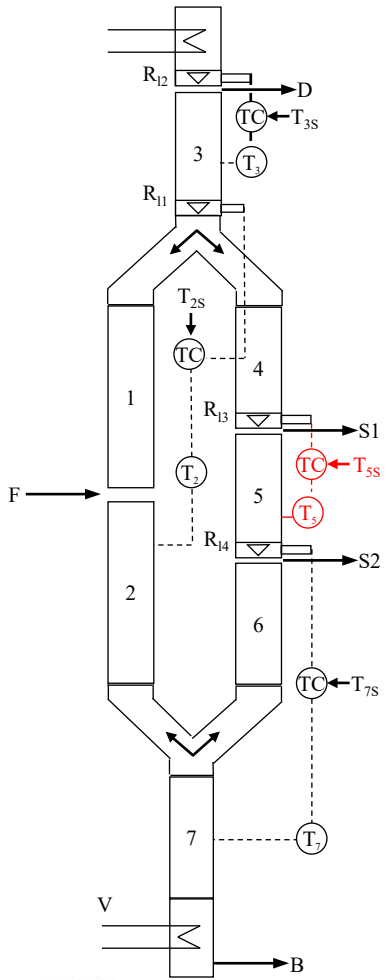
Steady Profiles with 4 temperature loops..

Distillate Loop ± 1 C



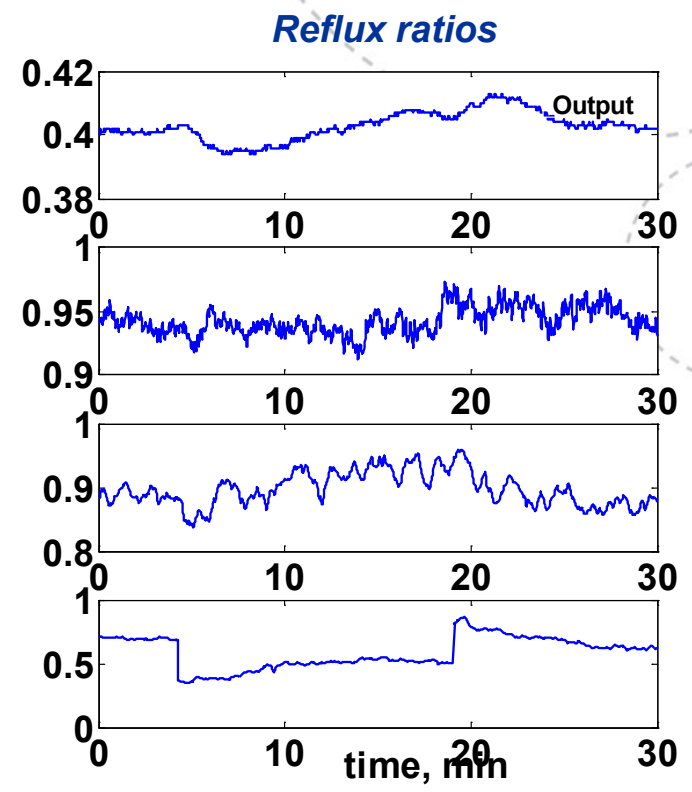
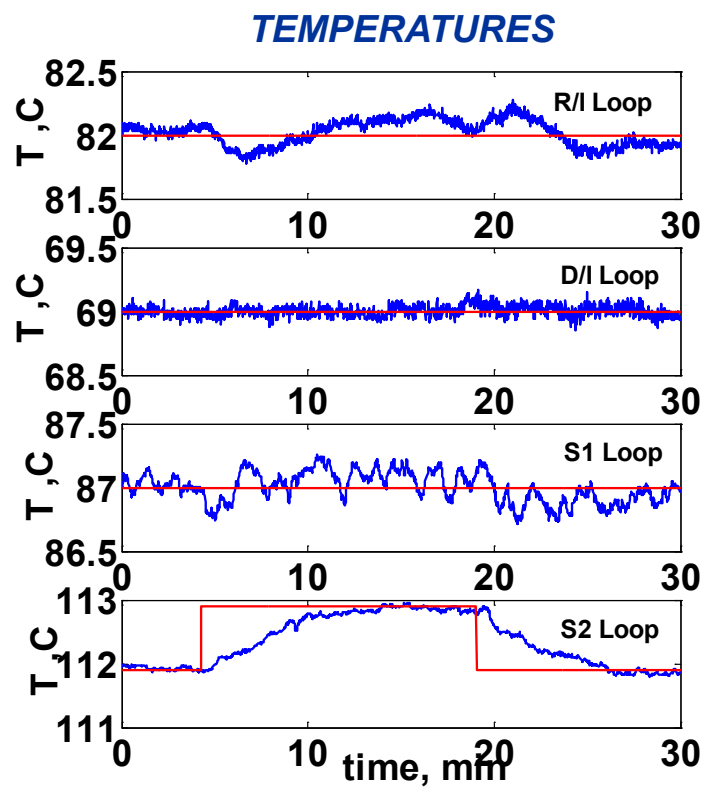
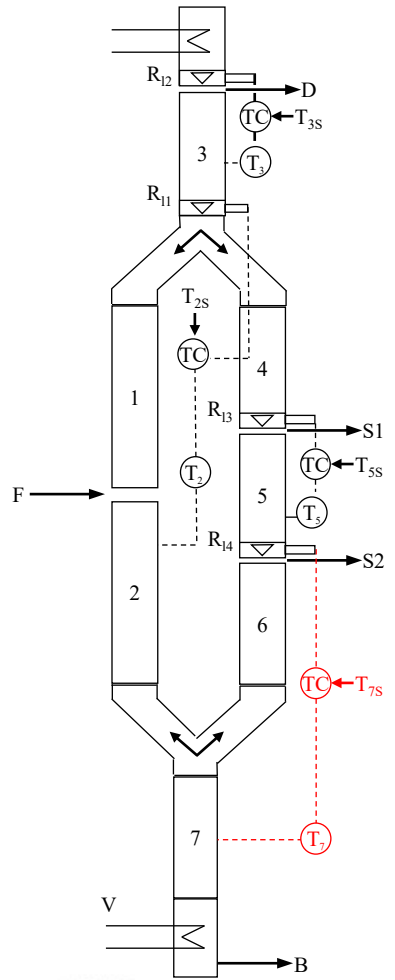
Steady Profiles with 4 temperature loops..

S1 Loop ± 1 C

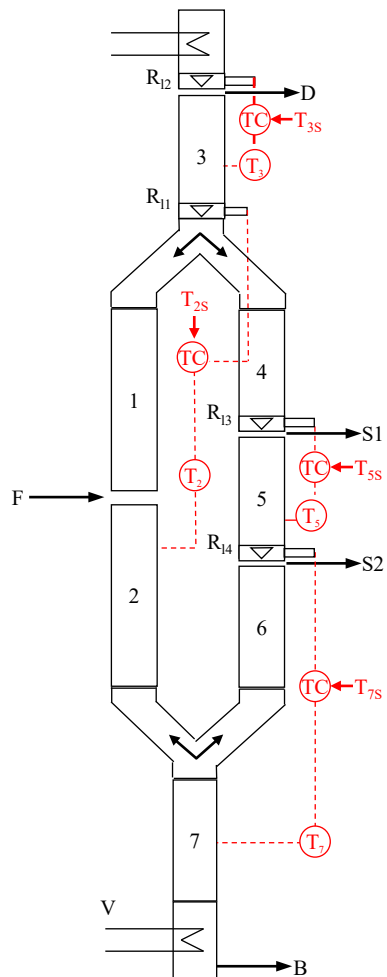


Steady Profiles with 4 temperature loops..

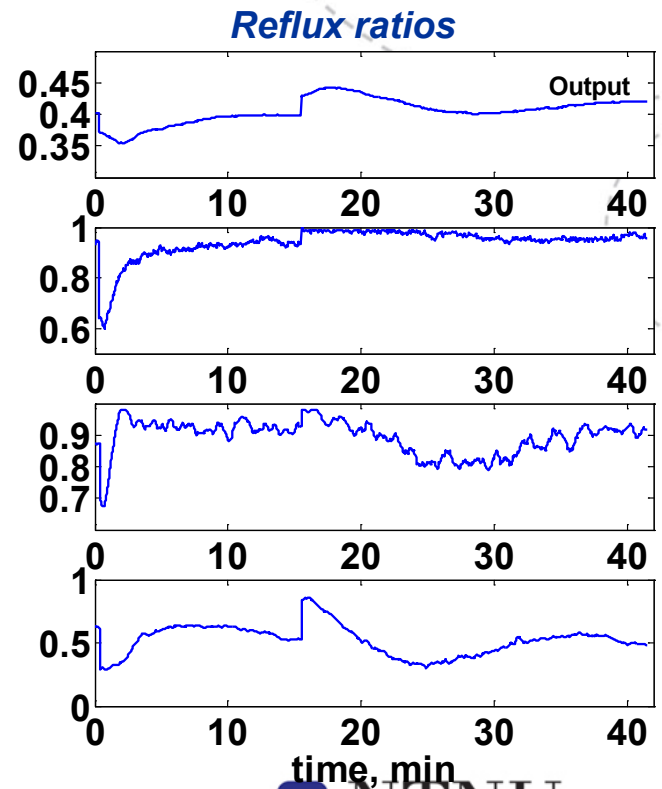
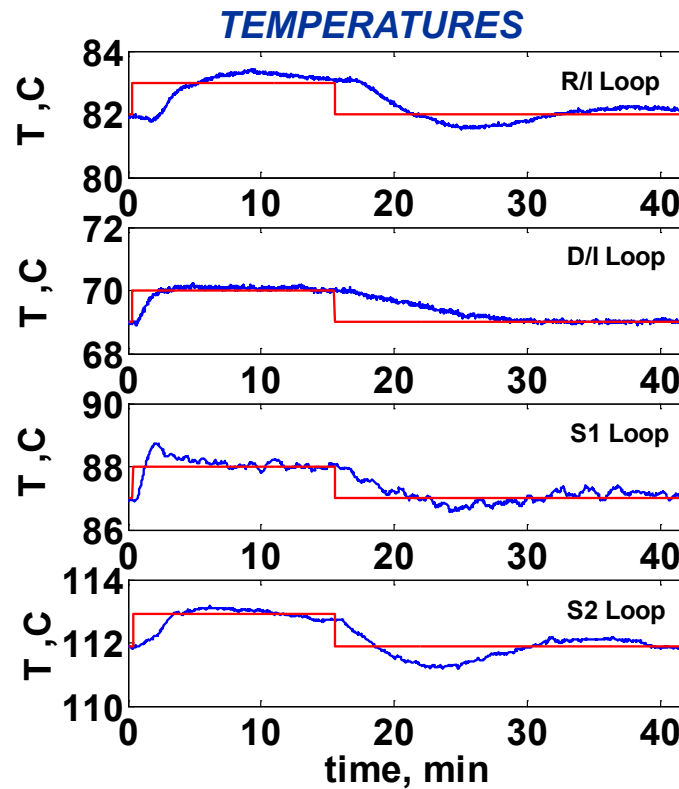
S2 Loop ± 1 C



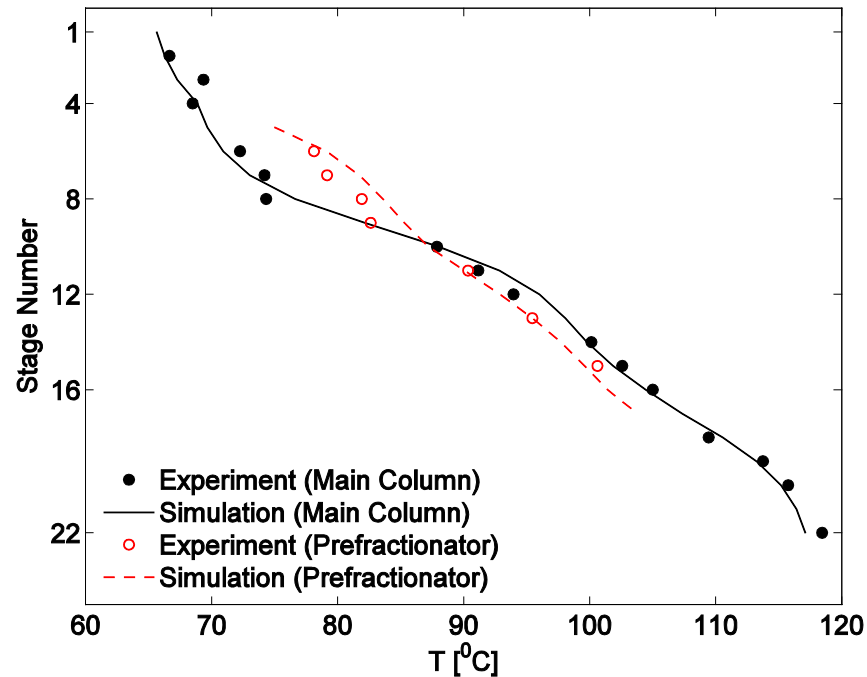
Steady Profiles with 4 temperature loops..



All Loops ± 1 C



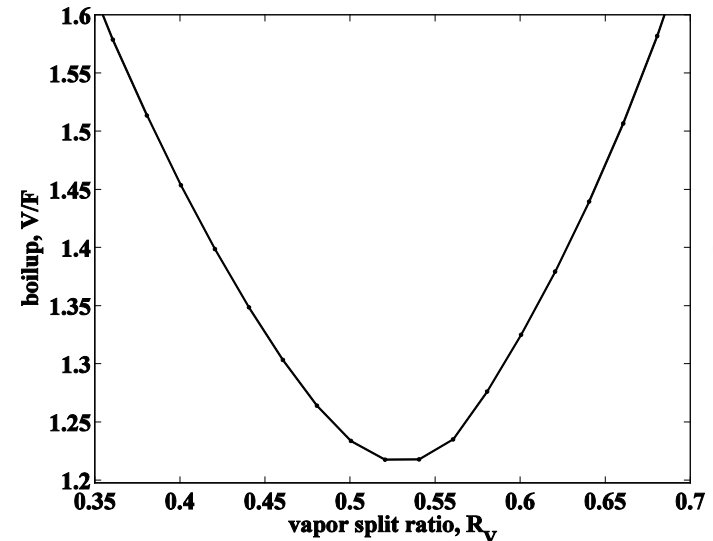
Model (lines) and experiments (points) fit well



	D		S1		S2		B	
	Simulation	Experiment	Simulation	Experiment	Simulation	Experiment	Simulation	Experiment
Methanol	92.6%	92.6%	15.4%	17.2%	0.21%	0	0	0
Ethanol	7.3%	7.3%	51.5%	51.5%	4.52%	5.38%	0	0
Propanol	0	0	32.9%	31.2%	89.6%	89.6%	3.14%	6.68%
Butanol	0	0	0	0	5.67%	5.02%	96.86%	93.32%

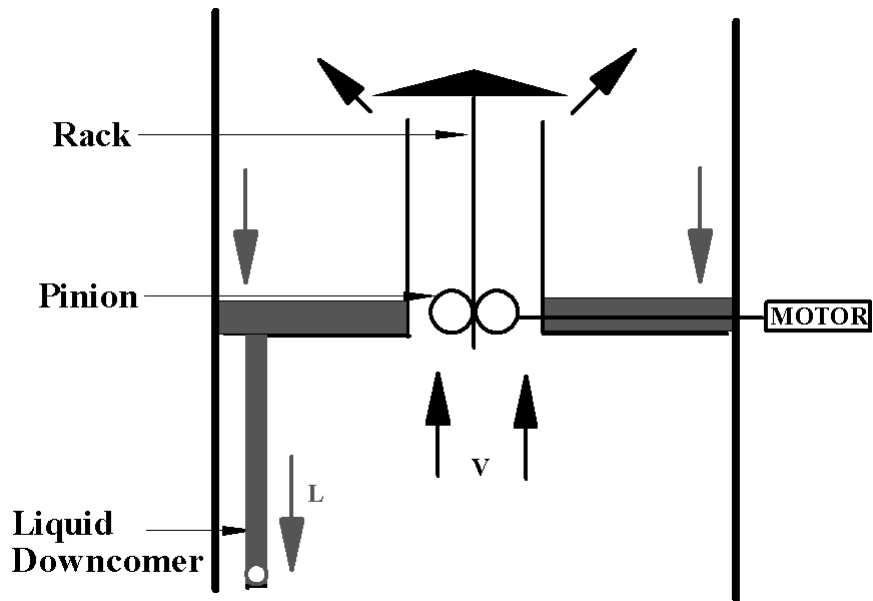
Vapor Split

- So far: Vapor split (R_v) kept constant
- But: Energy usage depends on R_v .
- Implement adjustable R_v
- But: Difficult to set R_v at desired value
 - Solution: Use R_v for temperature control (**feedback**)
 - The more precise liquid split (R_l) can be preset



V/F vs R_v for Kaibel column

Vapor Split Experiment..

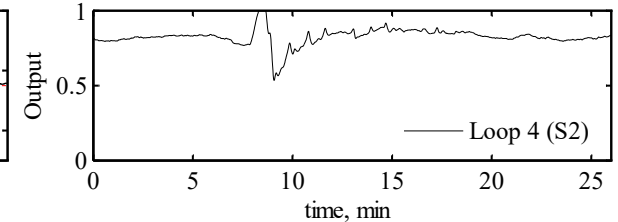
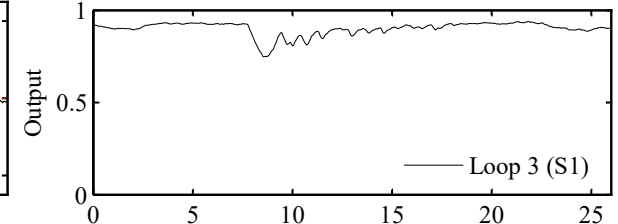
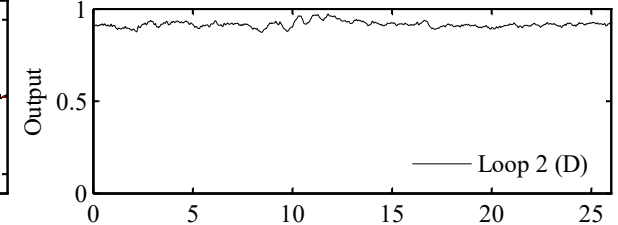
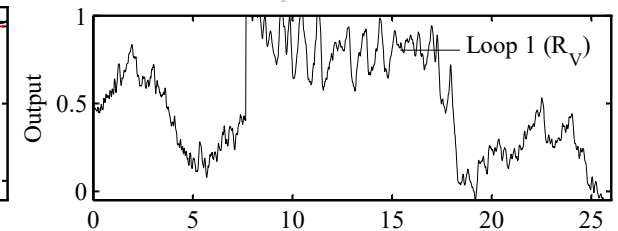
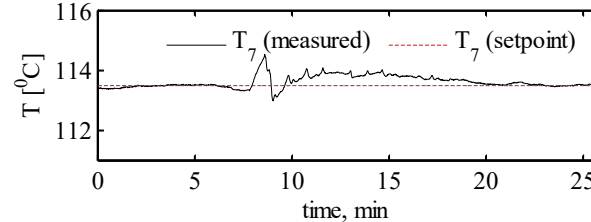
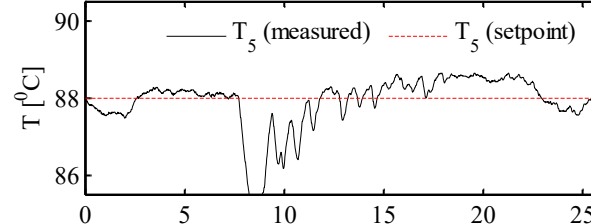
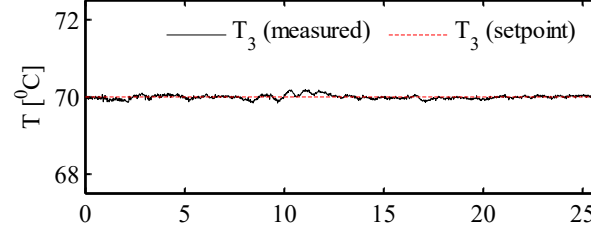
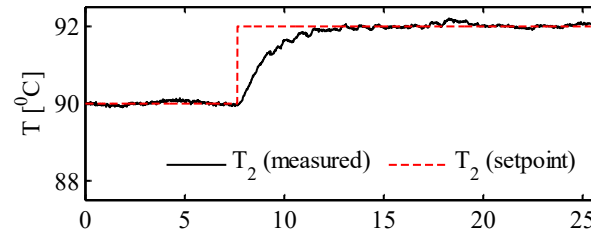
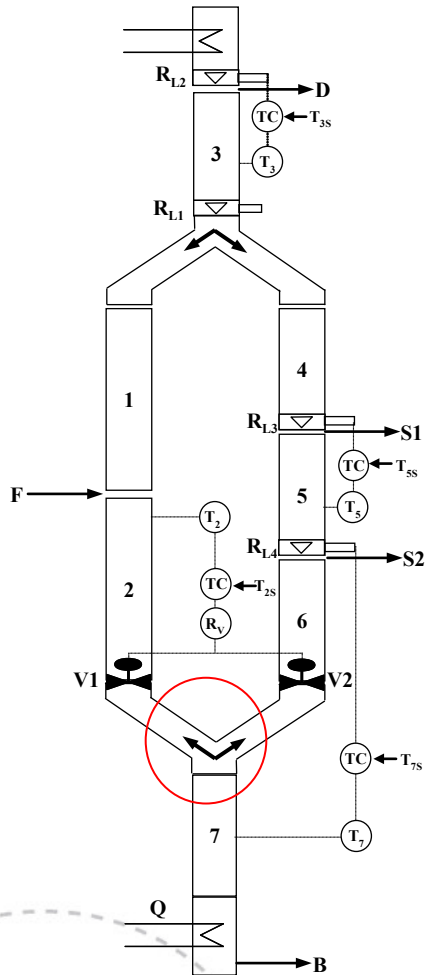


Schematic of the vapor split valve



**From top left: Valve in fully open position
Top right: Rack and pinion arrangement**

Vapor Split Experimental run (Kaibel Column)



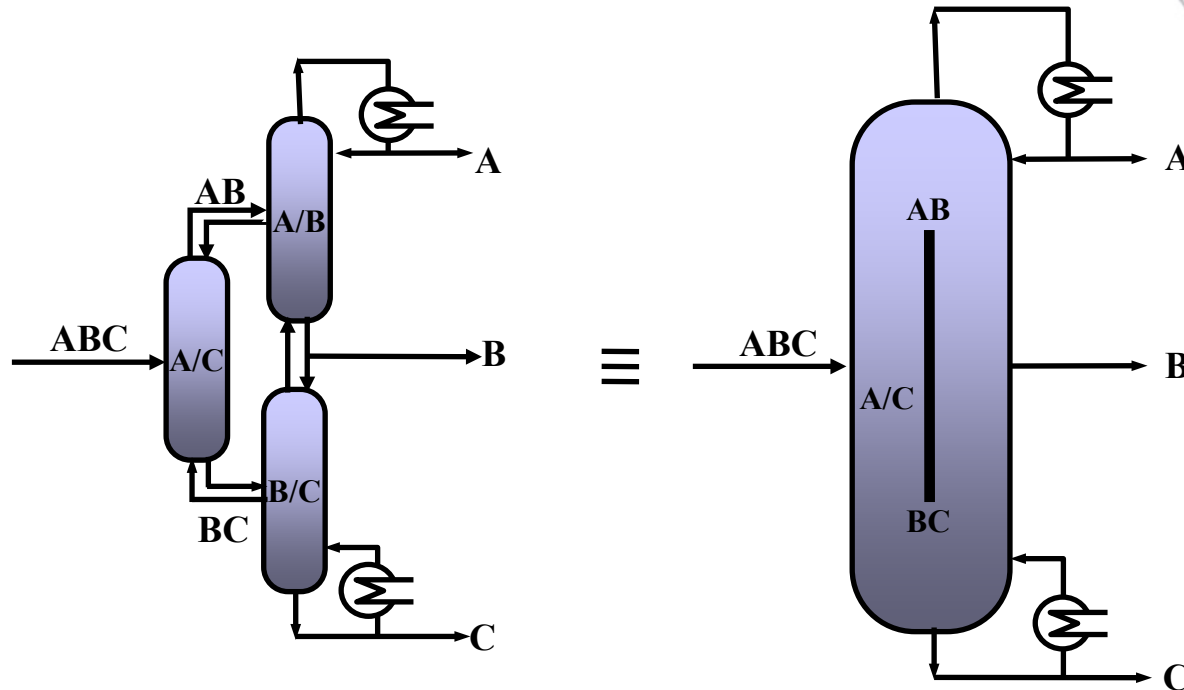
Conclusions

- **Four-Product Kaibel column**
 - Experimentally demonstrated 4-point temperature control for stabilizing and startup operation
 - Experimentally demonstrated active vapor split control
 - Experimental data fits well with the model

Outline

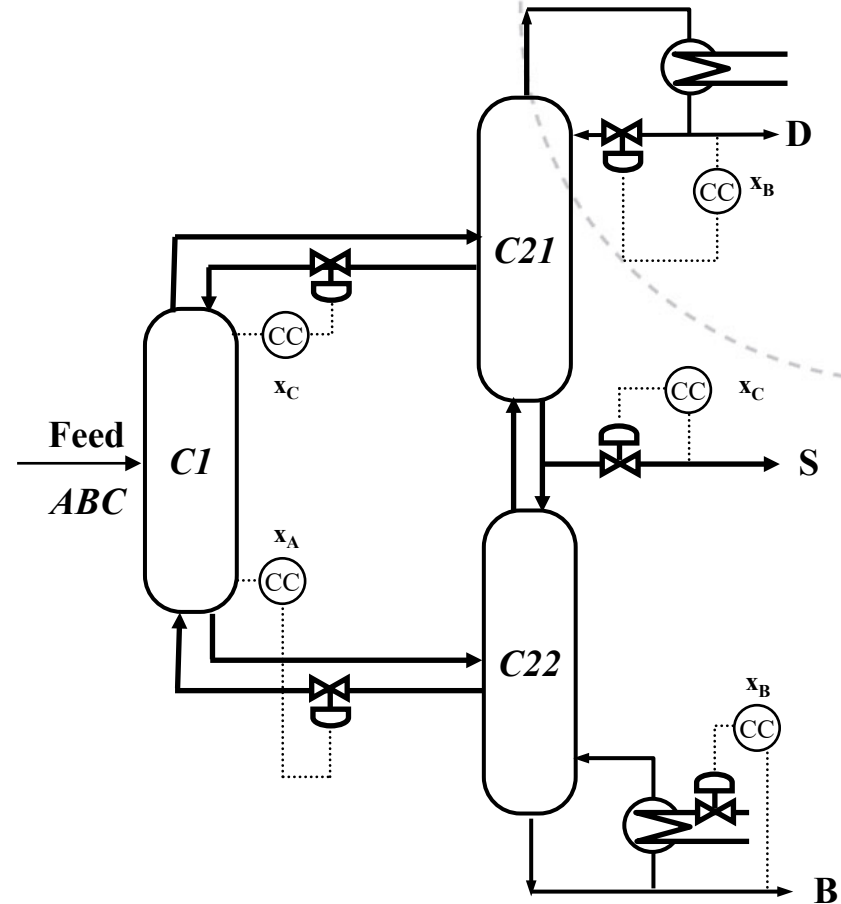
- Introduction
- **4- Product Kaibel Column**
 - Four-product Kaibel column
 - Control Structure
 - Experimental Setup
 - Experimental Runs- Steady state profiles
 - Experimental Runs- Vapor Split Experiment
- **3- Product Petlyuk Column**
 - Three-product Petlyuk column
 - The “ V_{\min} diagrams”
 - Control Structures
 - Close Loop Results
- Conclusions

Three-product Petlyuk column

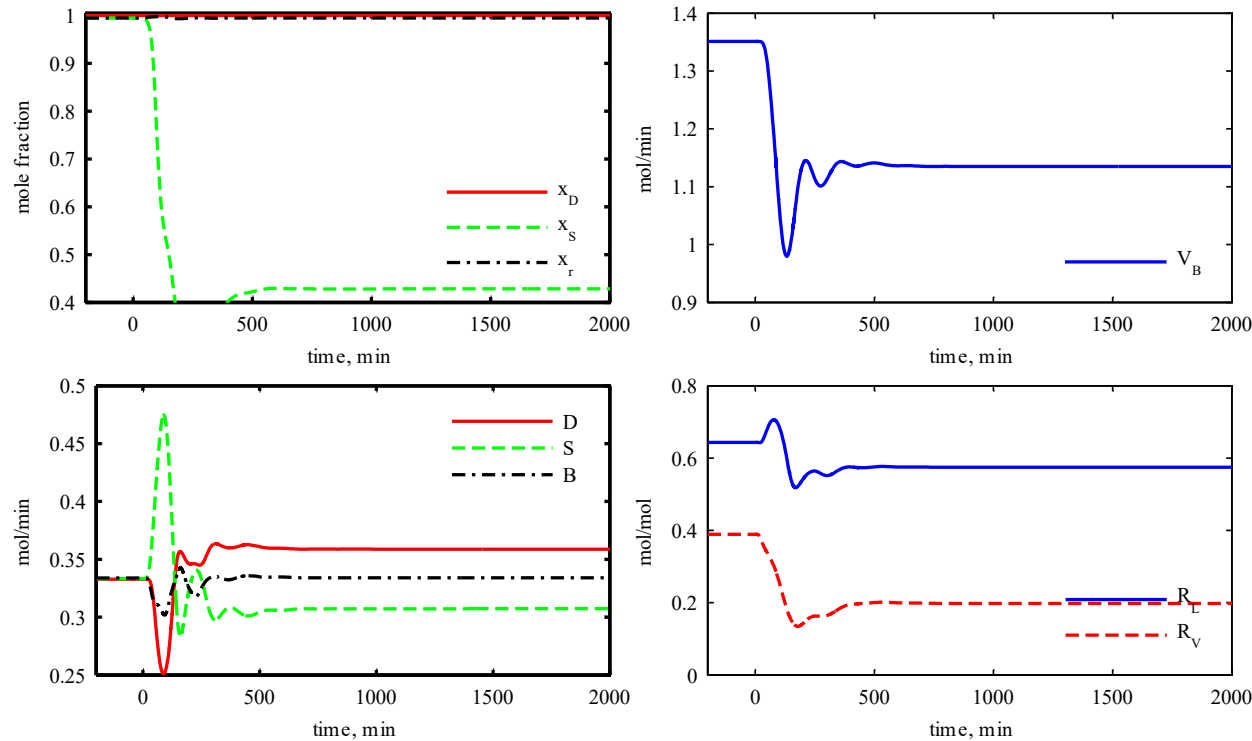


Control Structure 1

- Five degrees of freedom including vapor split
- Control key impurities using “close-by” pairings
- Side product has two side impurities
 - In CS1, S is paired with heavy key (x_C)



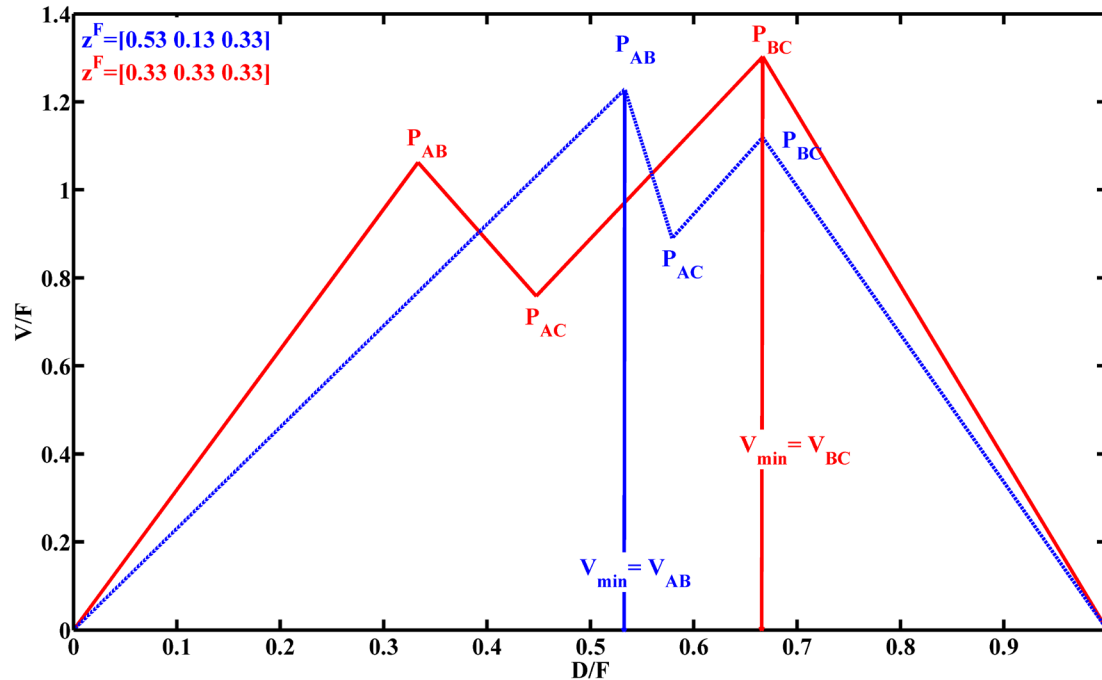
Closed-loop result from CS1



Fails for feed composition disturbance $z_f = [53 \ 13 \ 33]$

from nominal equimolar feed

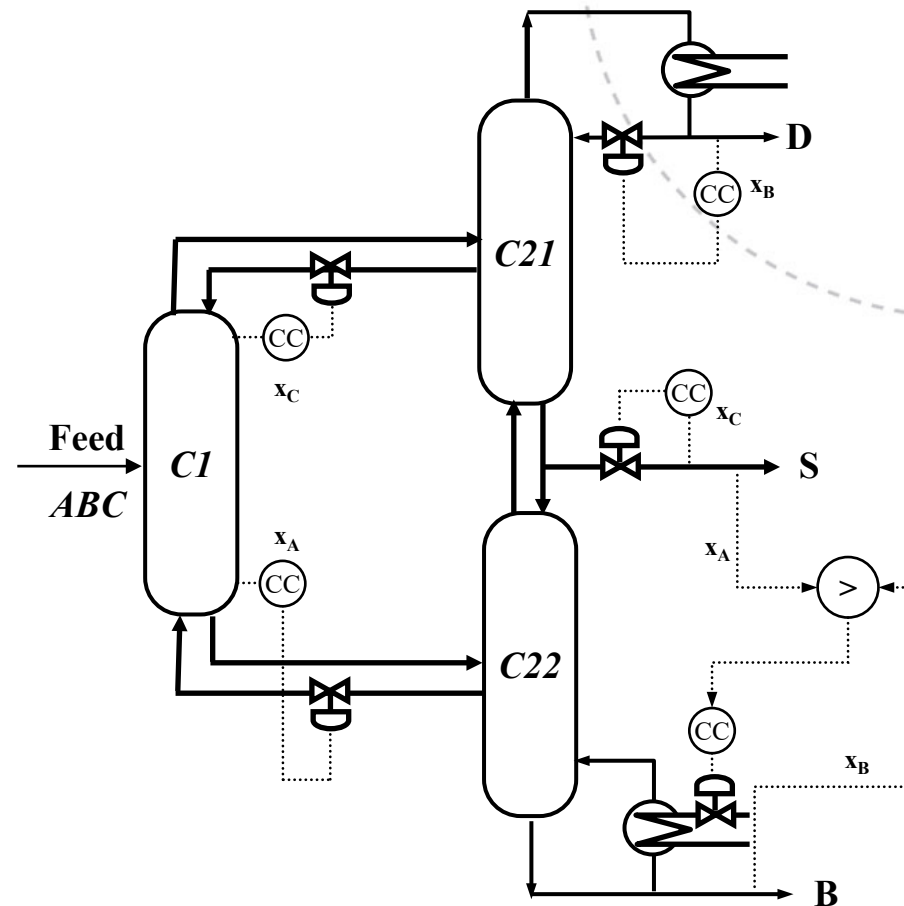
Why CS1 failed ??



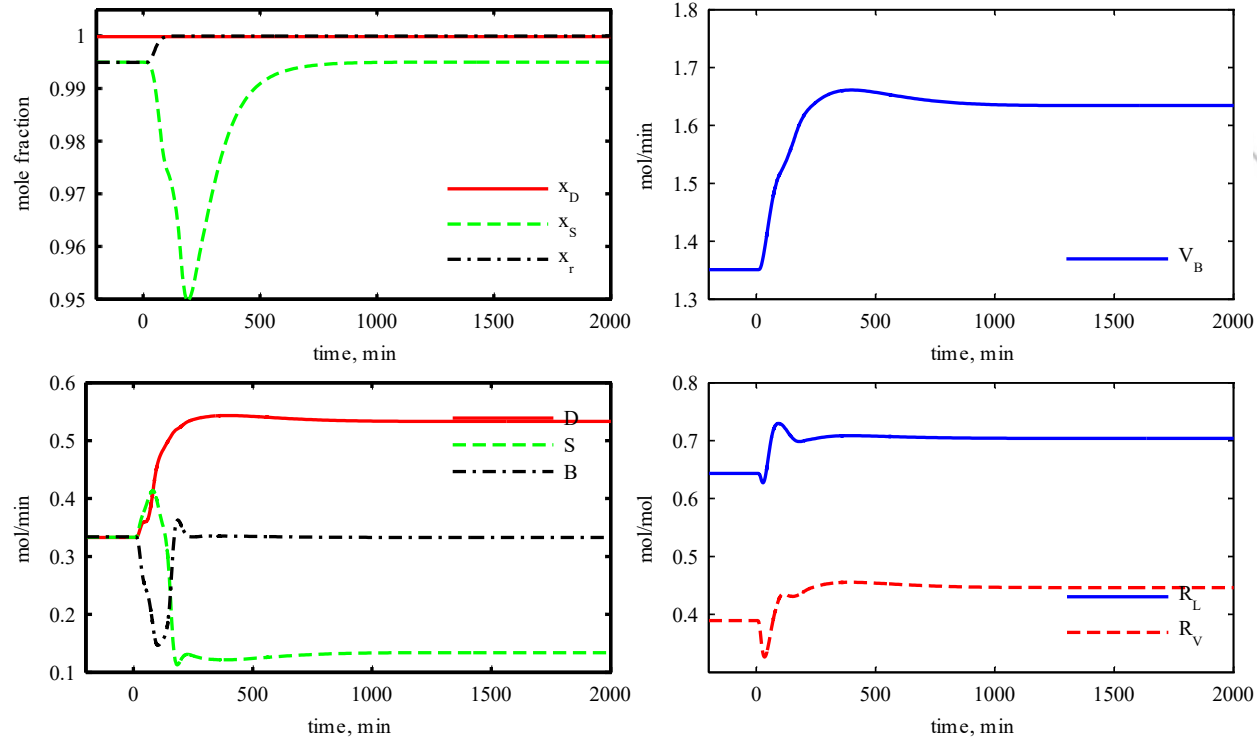
- For nominal equimolar feed, B/C is the most difficult split
- For the new feed A/B is more difficult feed and CS1 can not provide sufficient vapor in top section of main column

Control Structure 2

- Same as CS1, but boilup now has a maximum select controller with:
 - light key, x_A at S or,
 - light key, x_B at reboiler



Closed loop results from CS2



- Works for all feed composition disturbance from nominal equimolar feed
- The purity of bottom product may be over purified for some disturbances