# Modeling a Multiphase Subsea Separation System TKP 4550 Specialization Project

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# 1 Project Scope

# Motivation

#### 3 Model Description

- Deliquidizer
- Governing equations

#### Results

- Comparison to Experimental Data
- Flow rate effect
- Flow split effect

# 1 Project Scope

#### 2 Motivation

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- Based on the work from two Master thesis'.
  - Preben F. Tyvold(2015)
  - Fahad Matovu(2015)
- Model for Gas-Liquid separation
  - Model from Tyvold
  - Parameters from Matovu

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# Motivation

- Increased research focus
- Large focus in industry
- Improves economics



Figure: Picture from Statoil [2].

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Figure: From Tyvold [1]

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Model Description

Radial velocity
$$v_r(r,z) = rac{2r_d^2(
ho_d-
ho_c)}{9\mu} \, rac{v_ heta^2(r,z)}{r}$$

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Image: A matrix

Model Description

Radial velocity  
$$v_r(r,z) = rac{2r_d^2(
ho_d - 
ho_c)}{9\mu} \, rac{v_ heta^2(r,z)}{r}$$

# Soave-Redlich-Kwong Equation of State

$$p = \frac{RT}{V_m - b} - \frac{a\,\alpha}{V_m(V_m + b)}$$

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# Radial velocityDroplet size $v_r(r, z) = \frac{2r_d^2(\rho_d - \rho_c)}{9\mu} \frac{v_\theta^2(r, z)}{r}$ $r_d = m q_{in} + c$ Soave-Redlich-Kwong Equation<br/>of StateSoave-Redlich-Kwong Equation<br/>of State

$$p = \frac{RT}{V_m - b} - \frac{a\,\alpha}{V_m(V_m + b)}$$

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Radial velocity	Droplet size		
$v_r(r,z) = \frac{2r_d^2(\rho_d - \rho_c)}{9\mu} \frac{v_\theta^2(r,z)}{r}$	$r_d = m q_{in} + c$ Tangential velocity		
Soave-Redlich-Kwong Equation of State	$v_{ heta}(r,z) = v_{ heta}^0(r) \exp(rac{-C_{decay} z}{2R})$		
$p=rac{RT}{V_m-b}-rac{alpha}{V_m(V_m+b)}$	211		

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#### Conclusion

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Table: Comparison between experimental data and model results. Flow split(FS) = 0.97 and inlet gas fraction  $\alpha_{in} = 0.83$ .

Inlet flow	GVF <sub>LPO</sub> [-]	GVF <sub>LPO</sub> [-]	LVF <sub>HPO</sub> [-]	LVF <sub>HPO</sub> [-]
q <sub>in</sub> [m <sup>3</sup> /h]	Exp.data	Model Results	Exp.data	Model Results
204.9	0.85	0.86	0.71	1
208.1	0.85	0.86	0.83	1
217.8	0.85	0.86	0.77	1

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# Flow rate effect Results

• Flow split = 0.8

• 
$$\alpha_{in} = 0.8$$



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# Flow split effect Results

• 
$$q_{in} = 140 \ m^3/h$$

• 
$$\alpha_{in} = 0.8$$

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# Project Scope

# 2 Motivation

#### B Model Description

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#### Results

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- Satisfying accuracy in GVF<sub>LPO</sub>
- Expected performance towards flow rate
- Performance towards flow split:
  - ${\bullet}~$  As expected at FS > 0.5
  - ${\bullet}~$  Not as expected at FS < 0.5
- Looking forward
  - More accurate model parameters
  - Better droplet size correlations
  - Optimization of separator.

- Johannes Jäschke
- Tamal Das

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# Tyvold, P.

Modeling and Optimization of a Subsea Oil-Water Separation System. Master thesis, Norwegian University of Science and Technology, Trondheim, 2015.

# Statoil

The Subsea Factory

http://www.statoil.com/en/technologyinnovation/ fielddevelopment/aboutsubsea/Pages/Lengre

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