

1 Problem 1

This is a follow-up of Exercise 1. The idea is to go back to Exercise 1 and reinterpret in terms of what you have learned later.

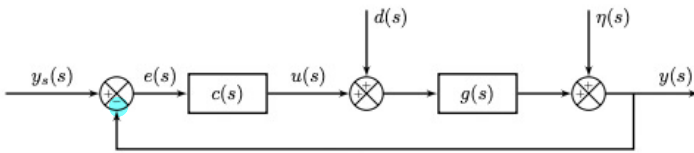


Figure 1: Controlled System

In the block diagram we have $d = \Delta T_F$, $y = \Delta T$ and $u = \Delta Q / (F C_P)$. The transfer function is given by

$$g(s) = \frac{e^{-100s}}{20s + 1} \quad (1)$$

1.1 P-control with $c(s) = K_c$

Derive the closed-loop transfer functions from d to u and y :

$$\begin{aligned} y &= h_1(s)d \\ u &= h_2(s)d \end{aligned}$$

What are the steady-state values of y and u when $d = 1$ (unit step) as a function of K_c , that is, what is $h_1(0)$ and $h_2(0)$? What are the values for $K_c = 0.5$? Does this agree with the simulations in Exercise 1? Why is there a steady-state offset, that is, why does not $y(t)$ return back to 0?

$$\begin{aligned} \text{CL: } T_{\text{CL}} &= \frac{\text{dir loop}}{1 + \text{loop}} \\ \Rightarrow h_1 &= \frac{g}{1 + g \cdot c} = \frac{g}{1 + K_c g} = \frac{e^{-100s} / (20s + 1)}{1 + K_c e^{-100s} / (20s + 1)} = \frac{e^{-100s}}{20s + 1 + K_c e^{-100s}} \\ h_1 &= \frac{e^{-100s}}{20s + 1 + K_c e^{-100s}} \\ h_2 &= \frac{-g \cdot c}{1 + g \cdot c} = \frac{-e^{-100s} / (20s + 1)}{1 + K_c e^{-100s} / (20s + 1)} = \frac{-K_c e^{-100s}}{20s + 1 + K_c e^{-100s}} \\ h_2 &= \frac{-K_c e^{-100s}}{20s + 1 + K_c e^{-100s}} \end{aligned}$$

SS-values:

When d is a unit step, $\mathcal{L}(d) = \frac{1}{s}$, then, using the final value theorem:

$$\lim_{t \rightarrow \infty} y(t) = \lim_{s \rightarrow 0} s \cdot T(s) = \lim_{s \rightarrow 0} s \cdot h_1(s) \cdot \frac{1}{s} = \lim_{s \rightarrow 0} h_1(s) = \frac{1}{1 + K_c} = \frac{1}{1 + 0.5}$$

$$\Rightarrow \underline{\underline{y(\infty) = 0.667}}$$

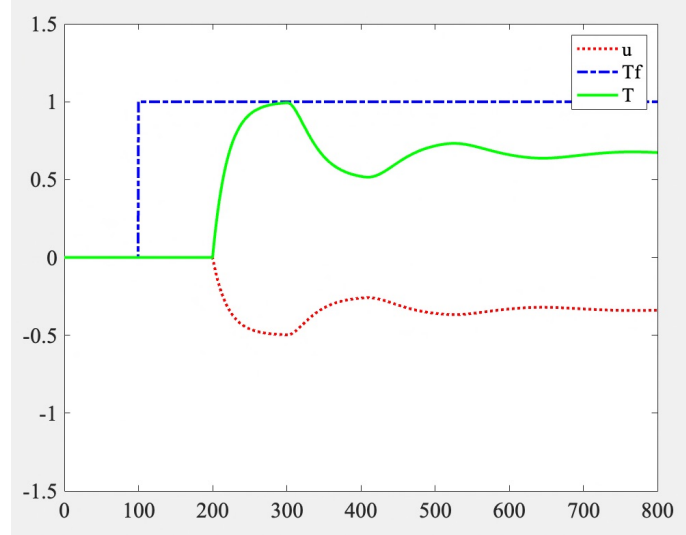
Similarly:

$$\lim_{t \rightarrow \infty} u(t) = \lim_{s \rightarrow 0} h_2(s) = \frac{-K_c}{1 + K_c} = \frac{-0.5}{1 + 0.5}$$

$$\underline{\underline{u(\infty) = -0.333}}$$

This looks accurate compared to 2,3-2 in exercise 1.

We have a steady-state offset due to a lack of integral action.
We need $C(s) \rightarrow \infty$ when $s=0$



1.2 SIMC PI-control

Derive the SIMC PI-controller (K_c, τ_I) for the choices $\tau_c = 100$, $\tau_c = 50$ and $\tau_c = 0$. What is the steady-state value of y and u when $d = 1$ (unit step)? Plot the responses for $y(t)$ and $u(t)$ to a step in d (see solution to Exercise 1).

From ex 1: $k=1, \tau_1=20$

$$K_c = \frac{1}{k} \cdot \frac{\tau_1}{\tau_c + \theta}, \quad \tau_I = \min(\tau_1, 4(\tau_c + \theta))$$

$\tau_c = 100$:

$$K_c = \frac{1}{1} \cdot \frac{20}{100+100} = 0,1$$

$$\tau_I = \min(20, 400) = 20$$

$\tau_c = 50$:

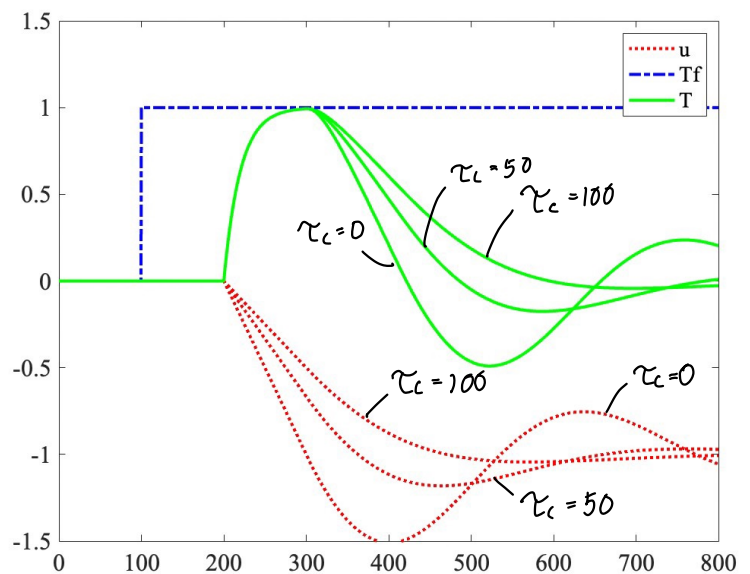
$$K_c = \frac{1}{1} \cdot \frac{20}{50+100} = 0,133$$

$$\tau_I = \min(20, 600) = 20$$

$\tau_c = 0$:

$$K_c = \frac{1}{1} \cdot \frac{20}{100} = 0,2$$

$$\tau_I = \min(20, 400) = 20$$



Now, having PI, the transfer function is $C(s) = K_c \frac{\tau_I s + 1}{\tau_I s}$

$$\Rightarrow h_1 = \frac{g}{1 + g \cdot c} = \frac{e^{-100s} / (20s + 1)}{1 + \frac{e^{-100s}}{20s + 1} \cdot K_c \cdot \frac{\tau_I s + 1}{\tau_I s}} = \frac{e^{-100s}}{(20s + 1) + K_c e^{-100s} \cdot \frac{\tau_I s + 1}{\tau_I s}}$$

$$h_1 = \frac{\tau_I s e^{-100s}}{\tau_I s (20s + 1) + K_c e^{-100s} (\tau_I s + 1)}$$

We can see that $y(\infty) = h_1(0) = 0 \forall \tau_c$ from the expression

$$h_2 = \frac{-g \cdot c}{1 + g \cdot c} = \frac{-K_c \cdot \frac{e^{-100s}}{20s + 1} \cdot \left(\frac{\tau_I s + 1}{\tau_I s}\right)}{1 + K_c \cdot \frac{e^{-100s}}{20s + 1} \cdot \left(\frac{\tau_I s + 1}{\tau_I s}\right)} = \frac{-K_c \cdot e^{-100s} (\tau_I s + 1)}{\tau_I s (20s + 1) + K_c e^{-100s} (\tau_I s + 1)}$$

$$u(\infty) = h_2(0) = \frac{-K_c}{K_c} = -1$$

$$\Rightarrow \underline{u(\infty) = -1 \forall \tau_c}$$

1.3 Ziegler-Nichols PI

In Exercise 1 we found that the "critical" or "ultimate" gain with P-control is $K_u = 1.13$.

Use the simulations from Exercise 1 to derive Ziegler-Nichols PI-settings.

Adding a piece of code to the script from exercise 1:

```
% Finner toppene og perioden til exercise 7 oppgave 1.3
```

```
bigboi1 = 0;
peakttime1 = 0;
bigboi2 = 0;
peakttime2 = 0;
for i = 1:size(T)
    if time(i) > 500 & time(i) < 600
        if T(i) > bigboi1
            bigboi1 = T(i);
            peakttime1 = time(i);
        end
    elseif time(i) > 700
        if T(i) > bigboi2
            bigboi2 = T(i);
            peakttime2 = time(i);
        end
    end
end
disp('Perioden er')
disp(peakttime2 - peakttime1)
```

Looking at graph from exercise 1

$$\Rightarrow \underline{P = 234,35 \text{ s}}$$

Using the rules for PI

ess information obtain PID settings:

Table 11.4 Controller Settings based on the Continuous Cycling Method

Ziegler-Nichols	K_c	τ_I	τ_D
P	$0.5K_{cu}$	—	—
PI	$0.45K_{cu}$	$P_u/1.2$	—
PID	$0.6K_{cu}$	$P_u/2$	$P_u/8$

← PID is for ideal form

We get

$$\underline{K_c = 0,45 \cdot 1,13 = 0,5085}$$

$$\underline{\tau_I = \frac{234,35}{1,2} = 195,29}$$

1.4 Smith predictor: time-delay compensation

What is the Smith Predictor controller for this process (with τ_c as a parameter)? Show how it can be realized in a block diagram.

Note that setting $\tau_c = 0$ would give "ideal control", but in practise this controller would not be robust.

The closed loop transfer function:

$$T_{CL} = \frac{C \cdot g}{1 + C \cdot g}, \text{ we must find } C, \text{ know } g = \frac{e^{-\theta s}}{20s + 1}, \theta = 100$$

* We are looking to find a C_{SP} , so we get a desired set-point response

Then, setting the CL-transfer functions equal to the wanted first order response

$$T_{CL} = \frac{y}{y_s} \Rightarrow \frac{g \cdot C_{SP}}{1 + g \cdot C_{SP}} = \frac{e^{-\theta s}}{\tau_c s + 1} \quad / \cdot \frac{1}{g}$$

$$\frac{1}{g \cdot C_{SP}} + 1 = \frac{\tau_c s + 1}{e^{-\theta s}}$$

$$\frac{1}{g \cdot C_{SP}} = \frac{\tau_c s + 1 - e^{-\theta s}}{e^{-\theta s}}$$

$$\Rightarrow C_{SP} = \frac{1}{g} \cdot \frac{e^{-\theta s}}{\tau_c s + 1 - e^{-\theta s}} \quad / \text{insert } g$$

$$C_{SP} = \frac{20s + 1}{\cancel{e^{-\theta s}}} \cdot \frac{e^{-\theta s}}{\tau_c s + 1 - e^{-\theta s}}$$

$$\underline{\underline{C_{SP} = \frac{20s + 1}{\tau_c s + 1 - e^{-\theta s}}}}$$

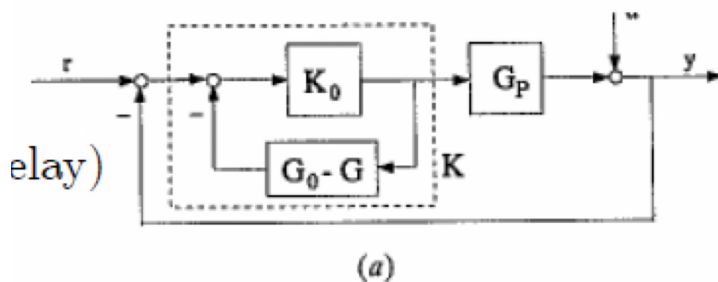
We want a structure like this, where K is the inner transfer loop

K_0 is the primary controller

G_0 is the model without delay

G is the model with delay

G_p is the actual plant



\Rightarrow Assuming a perfect model, $G_p = \frac{e^{-\theta s}}{20s+1} = G$

$$G = \frac{e^{-\theta s}}{20s+1}, \quad G_0 = \frac{1}{20s+1}$$

$$G_0 - G = \frac{1}{20s+1} (1 - e^{-\theta s})$$

We want: K to be Csp. For the closed loop:

$$K = \frac{K_0}{1 + K_0(G_0 - G)} = C_{SP} = \frac{20s+1}{\tau_c s + 1 - e^{-\theta s}}$$

$$\frac{K_0}{1 + \frac{K_0}{20s+1} (1 - e^{-\theta s})} = \frac{20s+1}{\tau_c s + 1 - e^{-\theta s}}$$

$$\frac{K_0 \cancel{(20s+1)}}{20s+1 + K_0(1 - e^{-\theta s})} = \frac{\cancel{20s+1}}{\tau_c s + 1 - e^{-\theta s}}$$

$$\frac{K_0}{20s+1 + K_0(1 - e^{-\theta s})} = \frac{1}{\tau_c s + 1 - e^{-\theta s}}$$

$$K_0 (\tau_c s + 1 - e^{-\theta s}) = 20s + 1 + K_0(1 - e^{-\theta s})$$

$$K_0 \cdot \tau_c s = 20s + 1$$

$$\underline{K_0 = \frac{20s+1}{\tau_c s}}$$

We then get the following block diagram

