

# Control Structure Design for Optimal Operation of 4-Product Thermally Coupled Columns

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# Outline

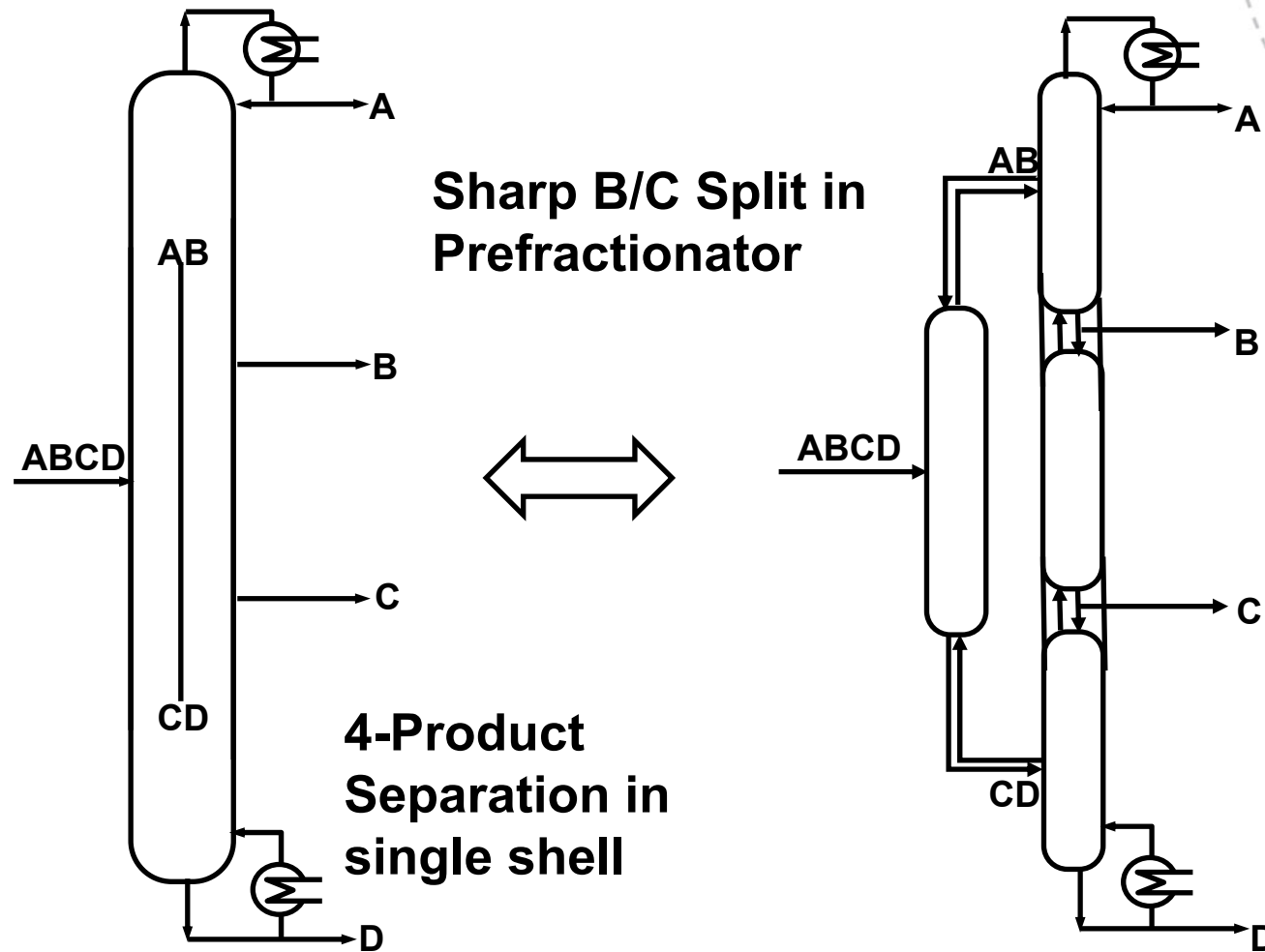
- **Introduction**
- **System 1: 4- Product Kaibel Column**
  - Previous Work
  - Control Structure
  - Experimental Setup
  - Experimental Runs- Steady state profiles
  - Experimental Runs- Vapor Split Experiment
- **System 2: 4- Product Extended Petlyuk Column**
  - Model Details
  - Control Structure
  - Close Loop Results
- **Conclusions**

# Introduction

- **Distillation is energy intensive process.**
- **Exergetic analysis requires minimizing irreversibilities:**
  - mixing effect
  - large  $\Delta T$  across column
- **This leads to Complex distillation arrangement:**
  - **Kaibel Arrangement**
  - **Petlyuk Arrangement**
  - intermediate Reboilers & Coolers etc
  - HIDIC distillation
- **Potential Energy Savings up to ~50 % for 4 product extended Petlyuk & up to ~30 % in Kaibel Arrangement\***

\* Halvorsen et. al. (2003)

# Kaibel Arrangement \*

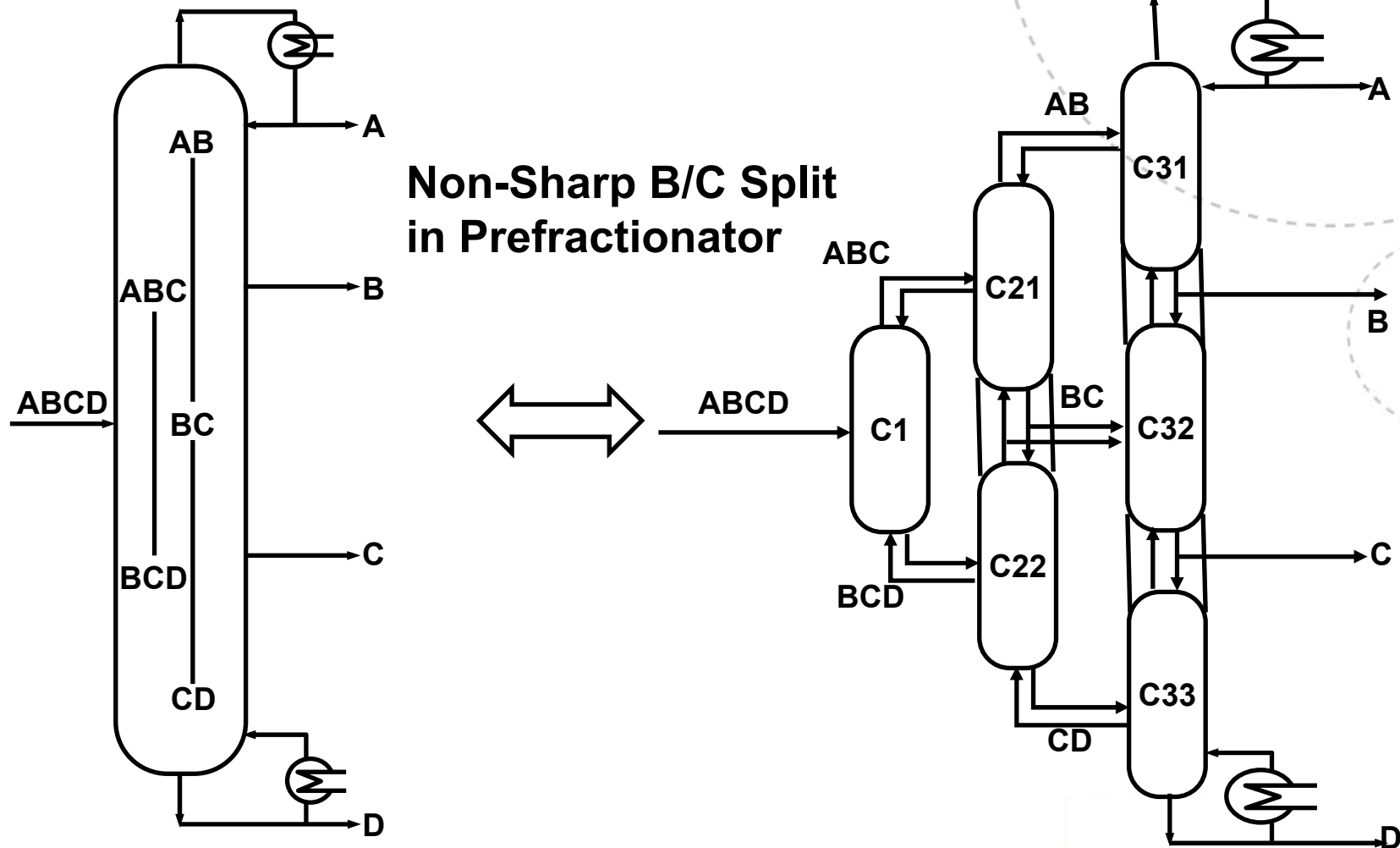


\* Kaibel. G (1987)

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# Extended Petlyuk Arrangement \*



\*Petlyuk, F.B. et al (1965)

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# Previous works

Simulation based studies carried with a plant wide perspective

- *Stabilizing operation of a 4-product Kaibel column* \*
  - **Close 4 temperature loops for stabilization & Inventory Control**
  
- *Optimal steady-state solutions for operating under economic objectives*\*\*
  
- **Model predictive control of the 4-product kaibel column**  
\*\*\*

**Thus there is an incentive to carry out experimental studies on operation of 4-product column**

\* Strandberg, J. et. al (2006)

\*\* Ghadrhan, M. et. al (2010)

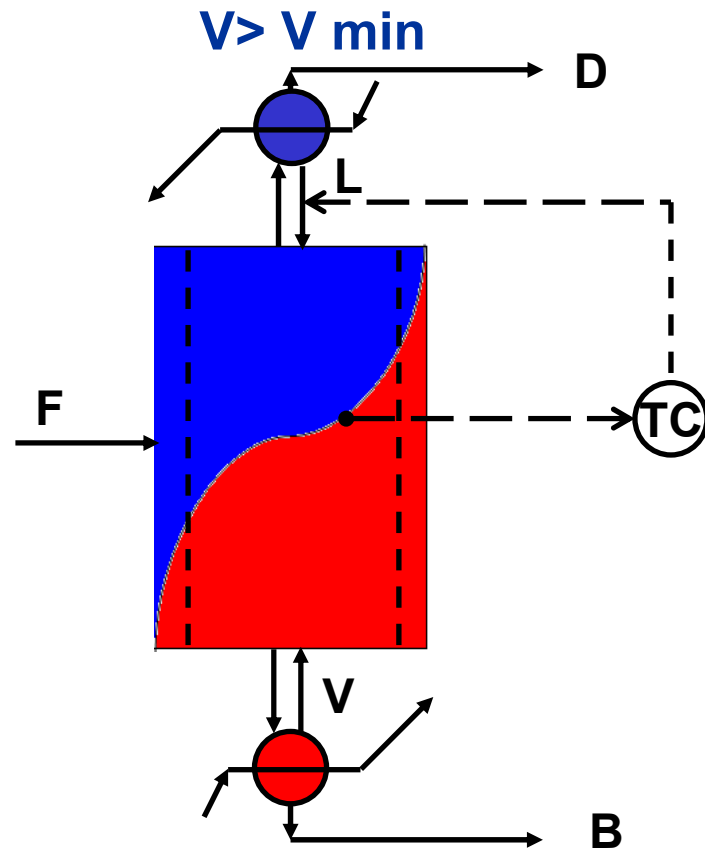
\*\*\* Kverland M. et. Al (2010)

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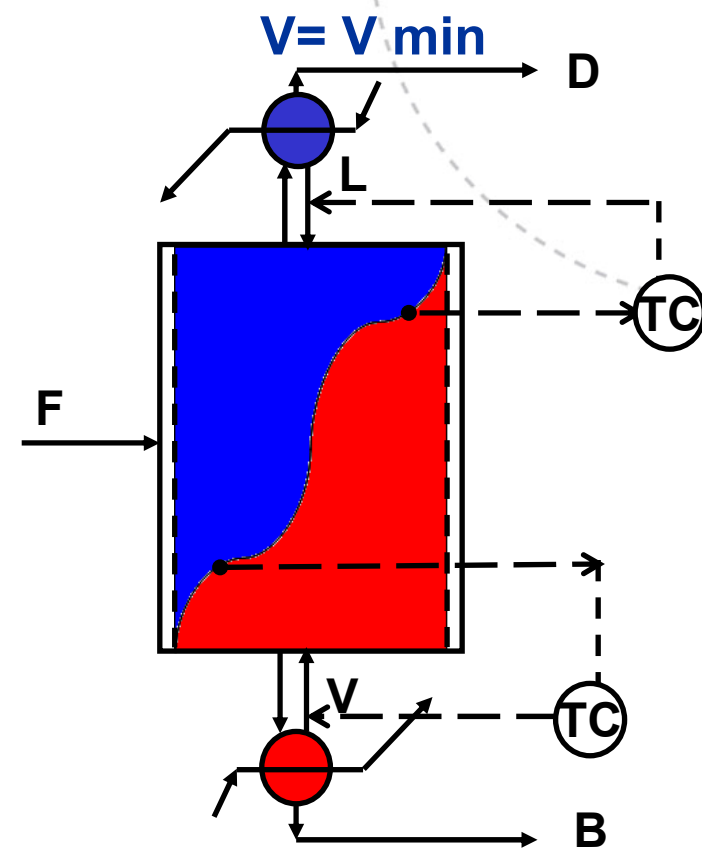
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# Control Structure (Ordinary Distillation)

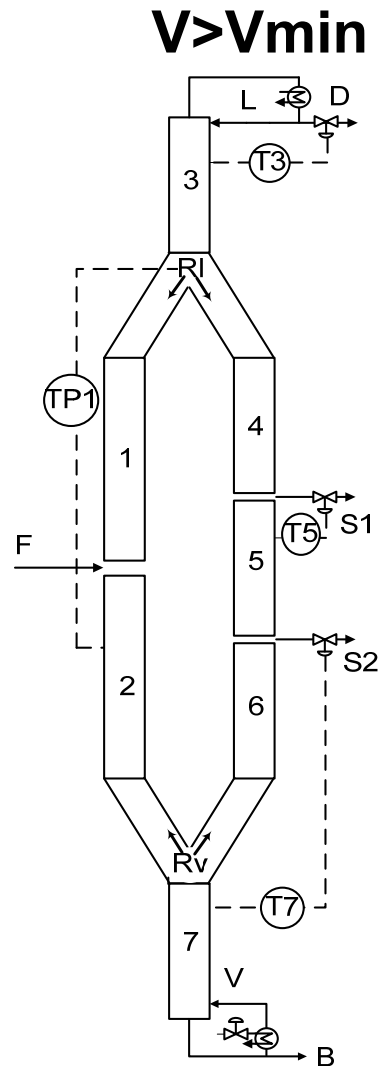


Single point control  
can stabilize the  
profiles

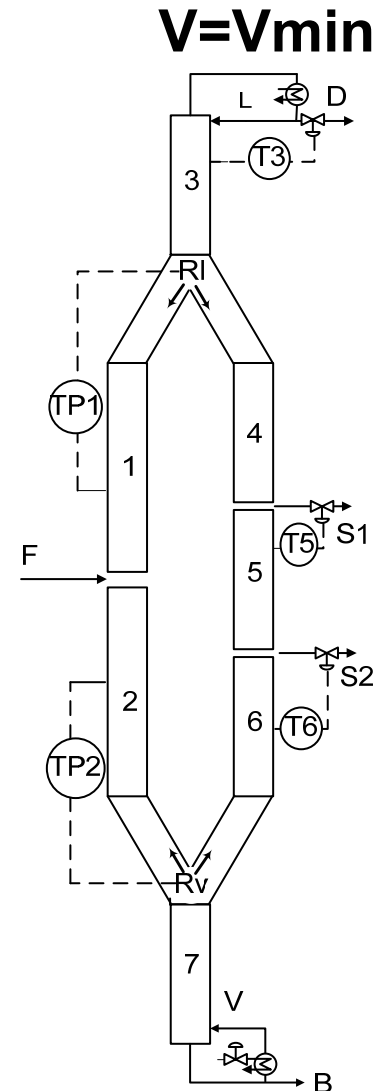


Two point control  
can stabilize  
column profiles

# Control Structure (Kaibel Column)



**4-point  
temperature  
control with one  
temperature in  
prefractionator**



**Rv Loop can be added**

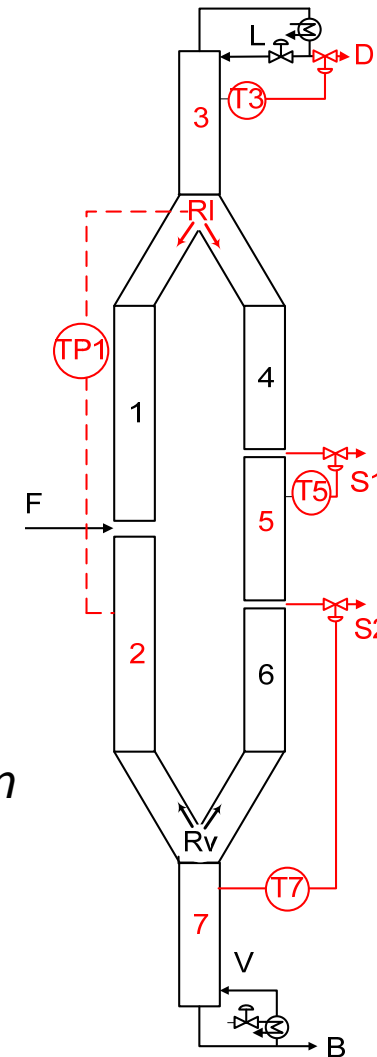
•when  $V = V_{min}$ , 2  
temperatures may  
be needed in  
prefractionator

•or, as DOF for any  
other economic  
objective

# Control Structure (As used in experiments)

- Decentralized Control with 4 PI Controllers
- 4 temperature sections 2, 3, 5, 7 in regulatory layer with R/I, D, S1 & S2
- $V=V_{max}$ , Vapor Split (Rv) not part of regulatory layer

*Next couple of slides summarize experimental validation*

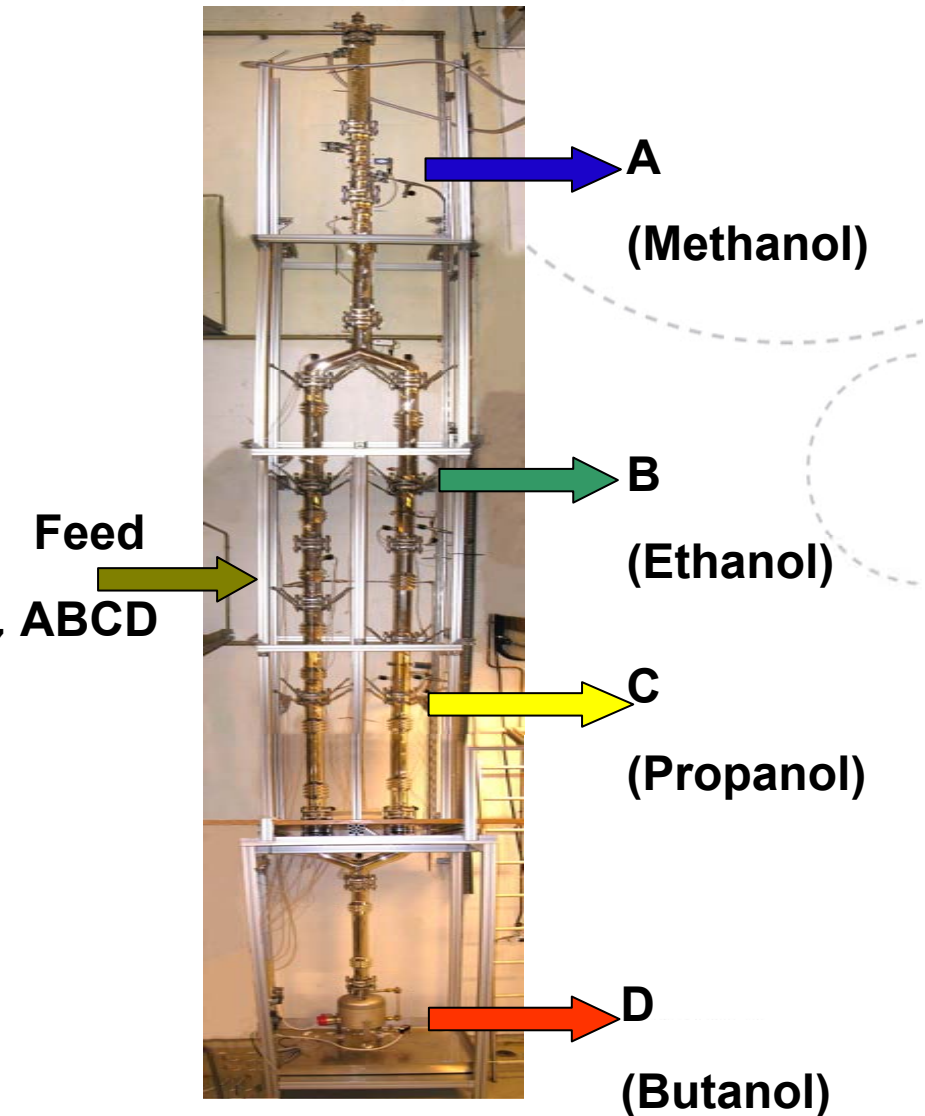


# Outline

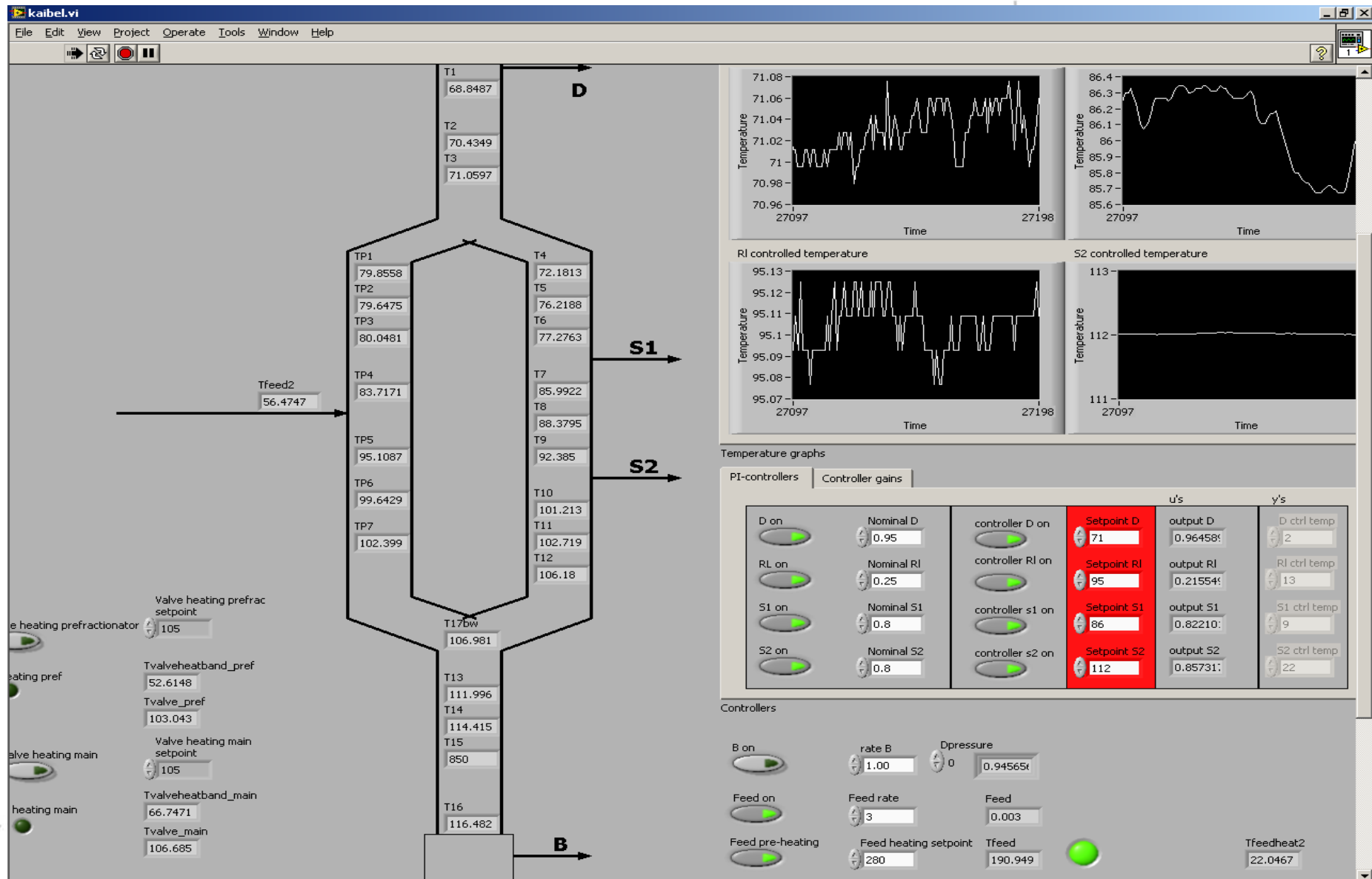
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# Experimental Set up

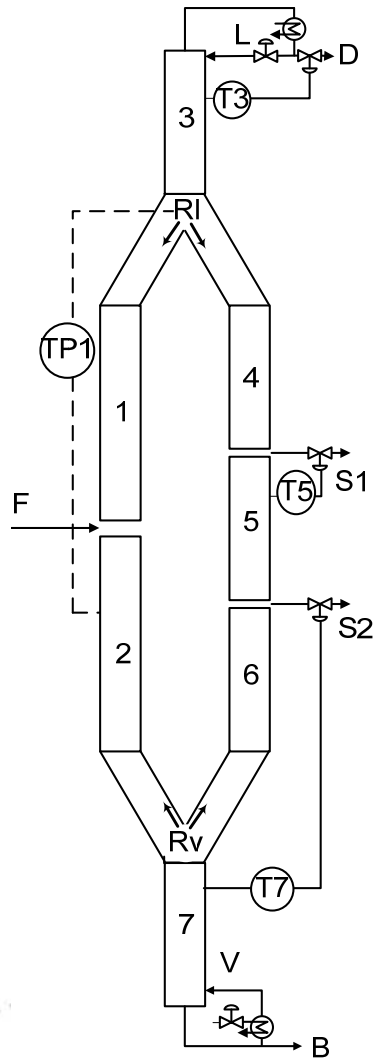
- 4 products
- Atmospheric pressure
- Packed Column
- Magnetic funnel-liquid split & Product valves
- Vapor split: Rack and Pinion
- Number of theoretical stages (experimentally determined):
  - Total stages in Prefractionator = 17
  - Total Stages in main column = 21
  - High Purity is impossible with given number of stages and flooding limitation
- Labview interface



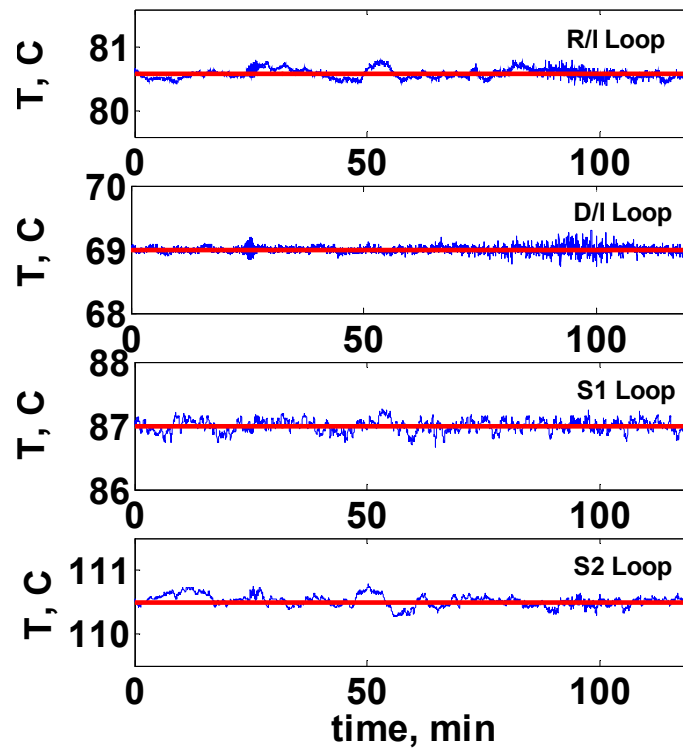
# Experimental Set up (Labview Interface)...



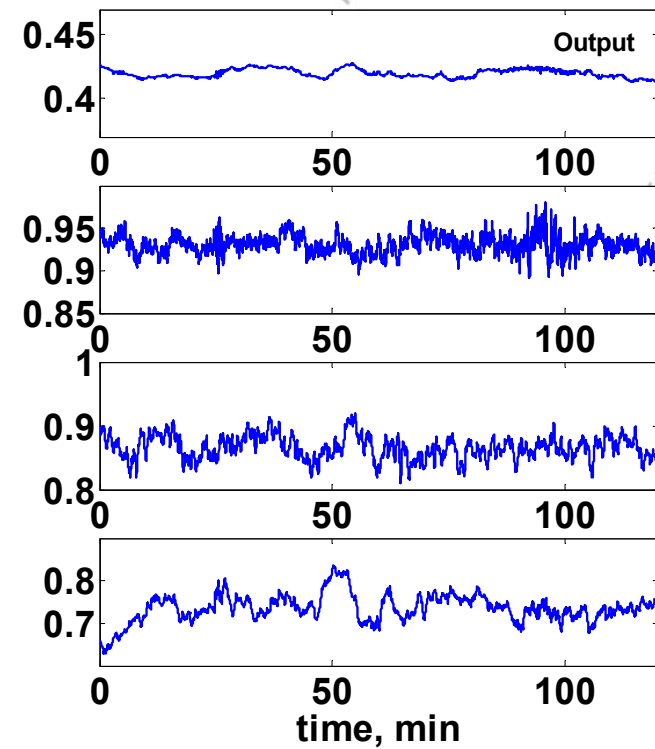
# Steady Profiles with 4 temperature loops



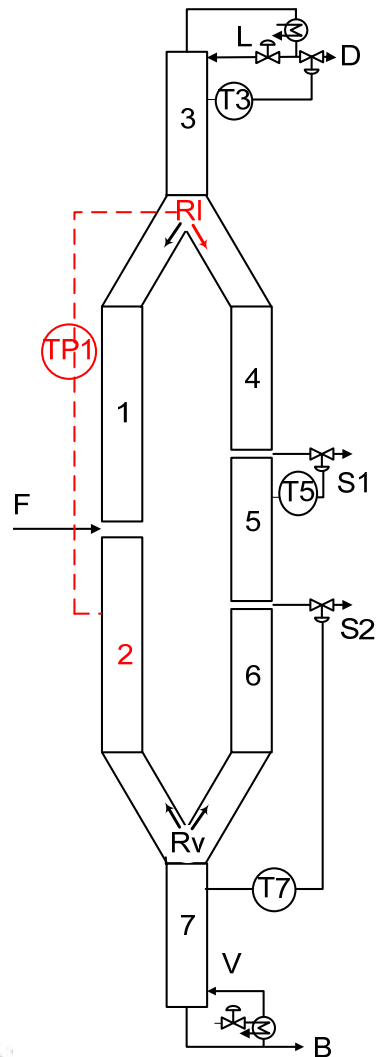
## TEMPERATURES



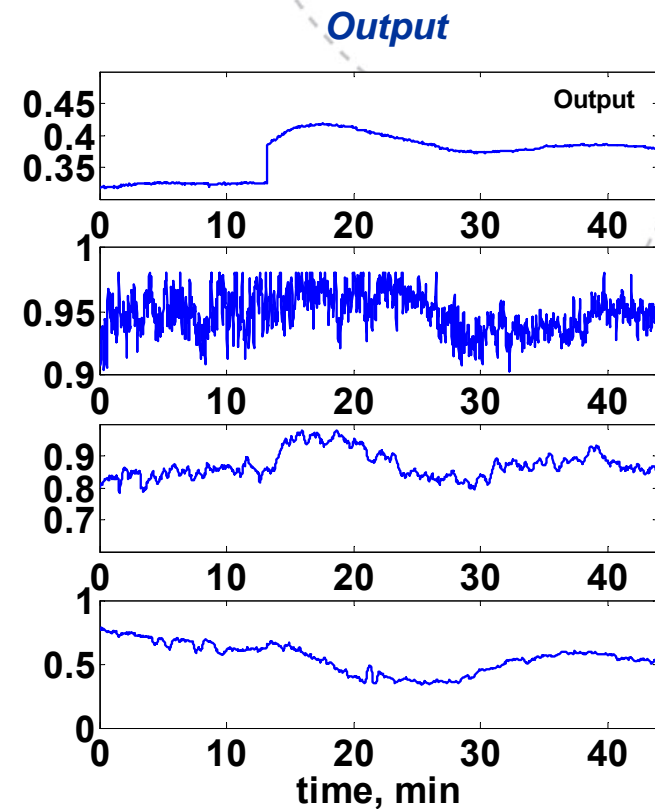
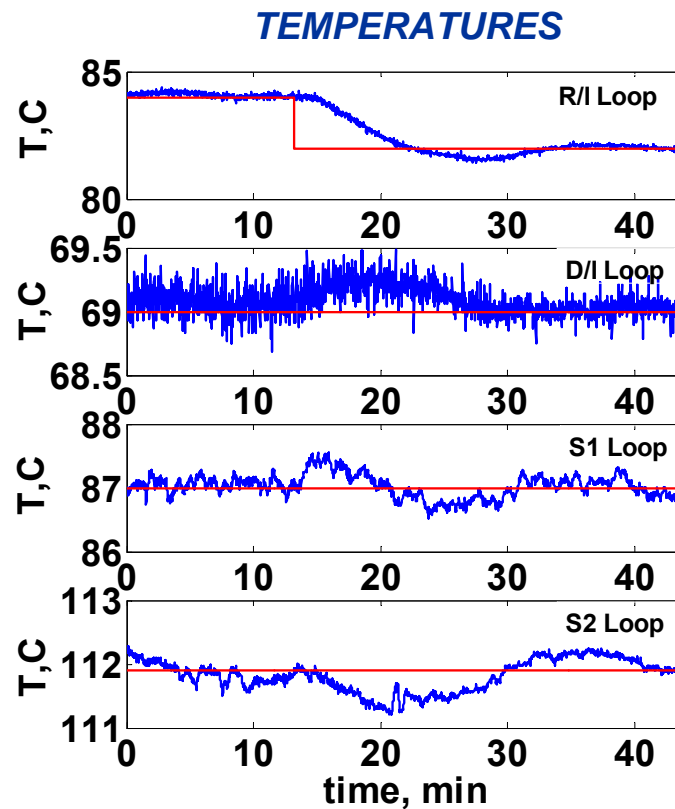
## Output



# Steady Profiles with 4 temperature loops..



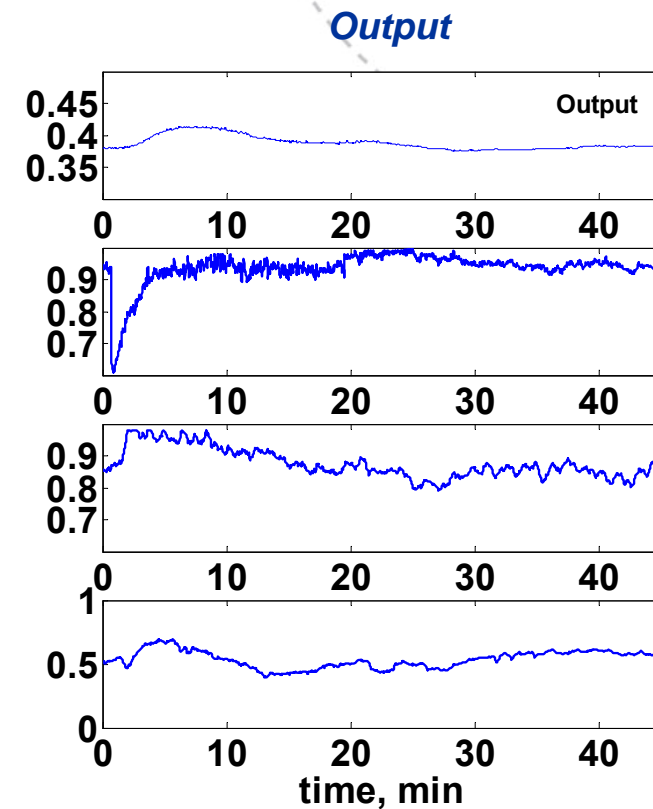
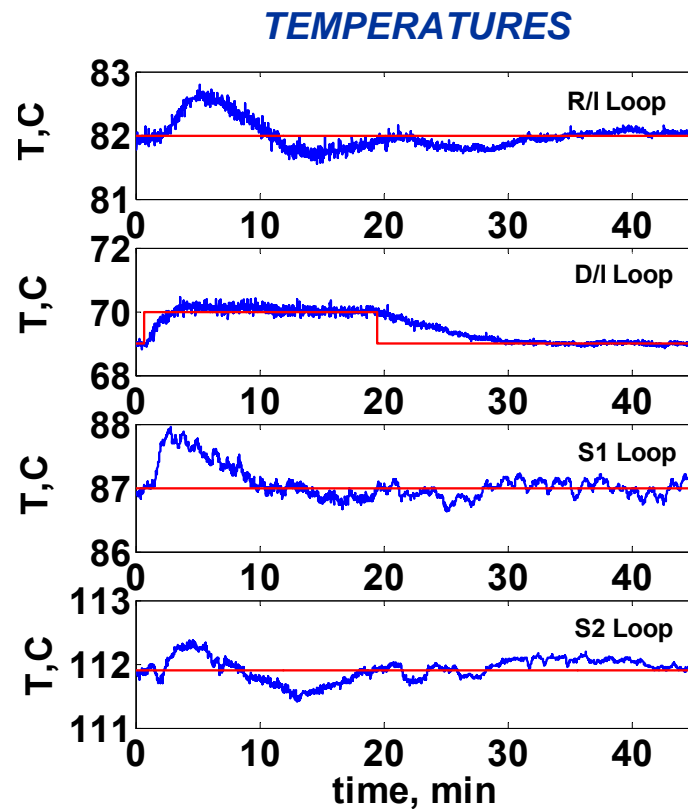
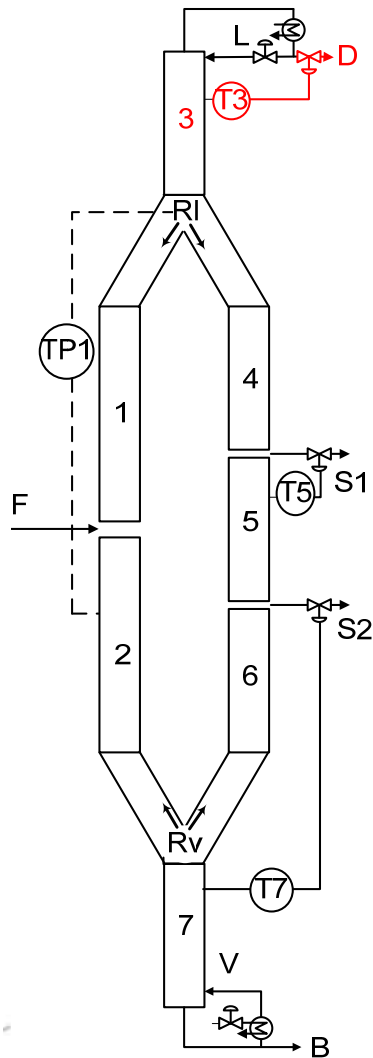
## Liquid Split Loop -2 C



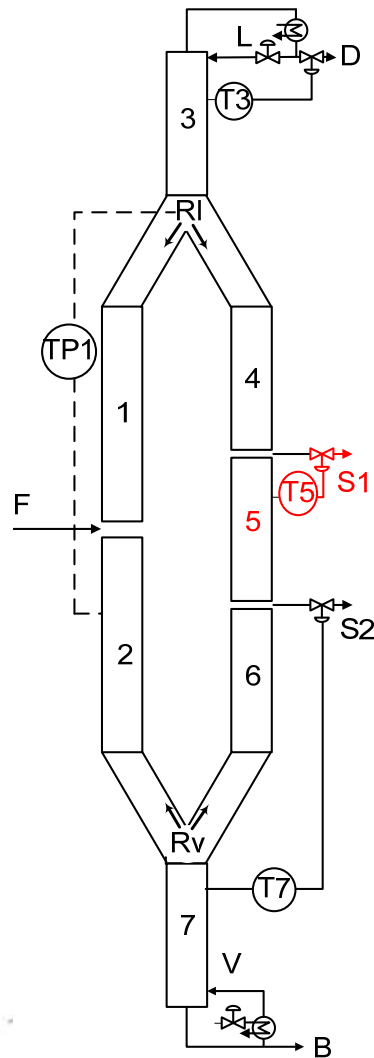


# Steady Profiles with 4 temperature loops..

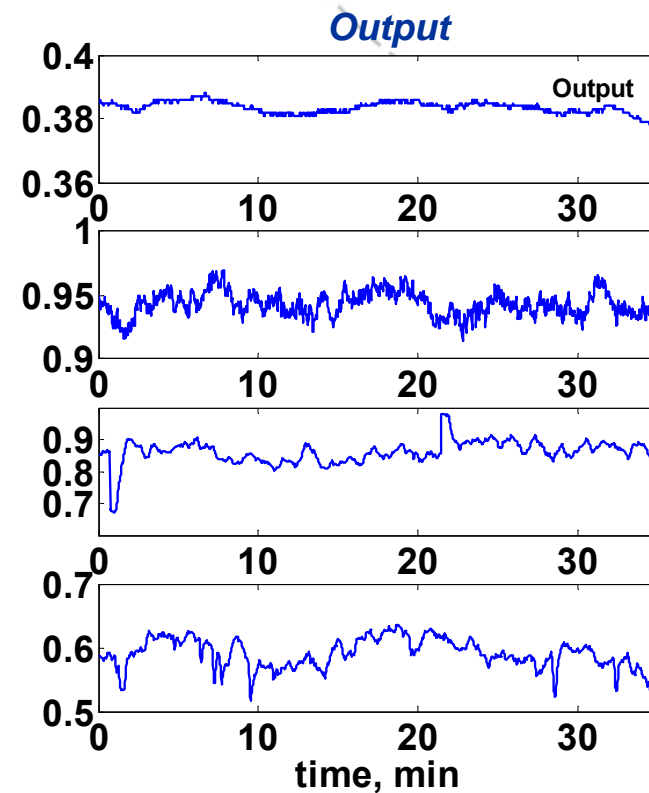
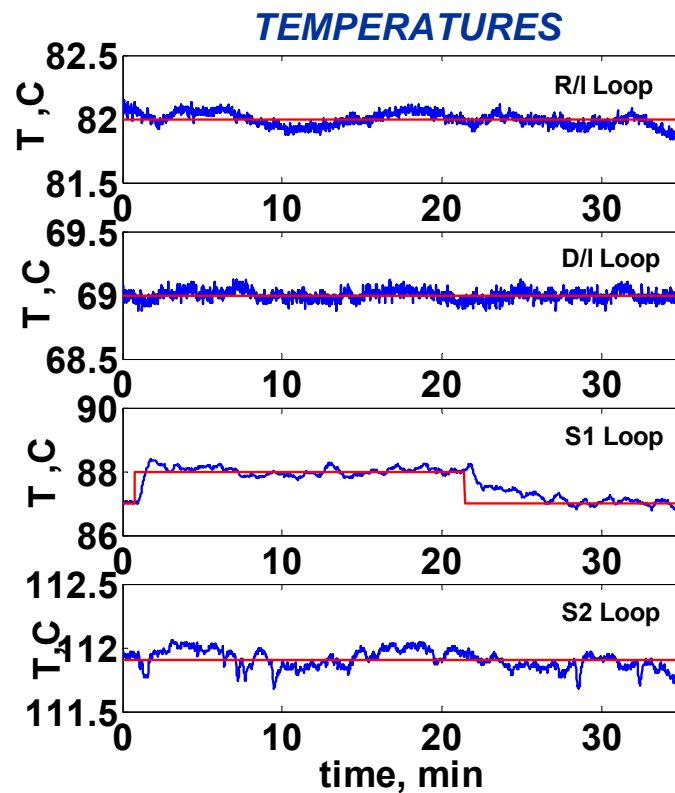
## Distillate Loop $\pm 1$ C



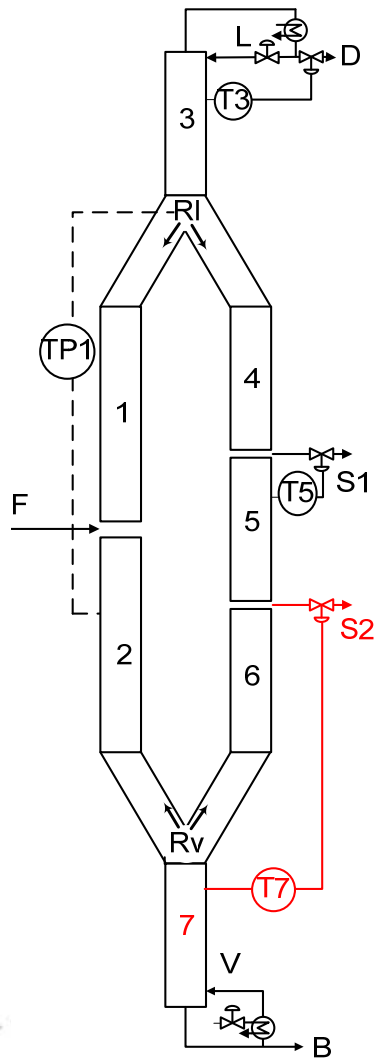
# Steady Profiles with 4 temperature loops..



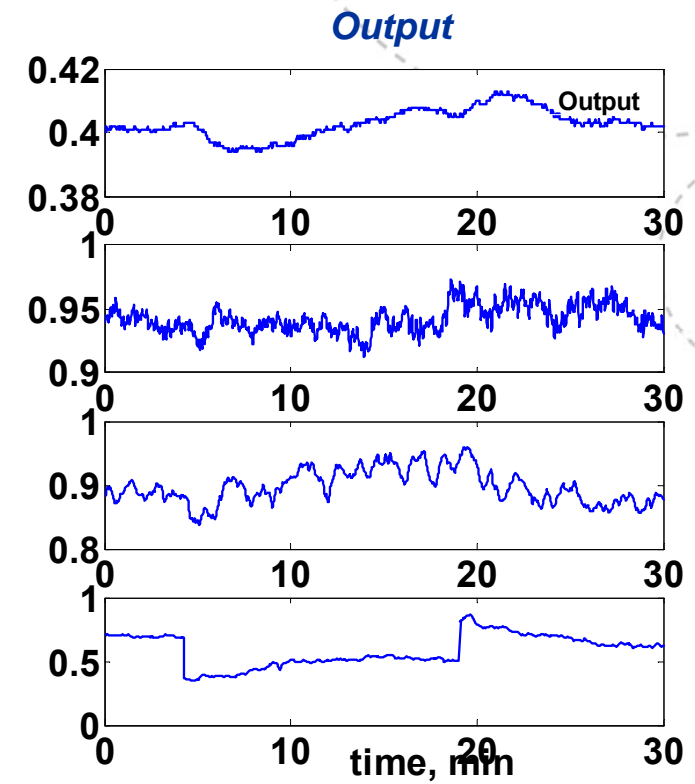
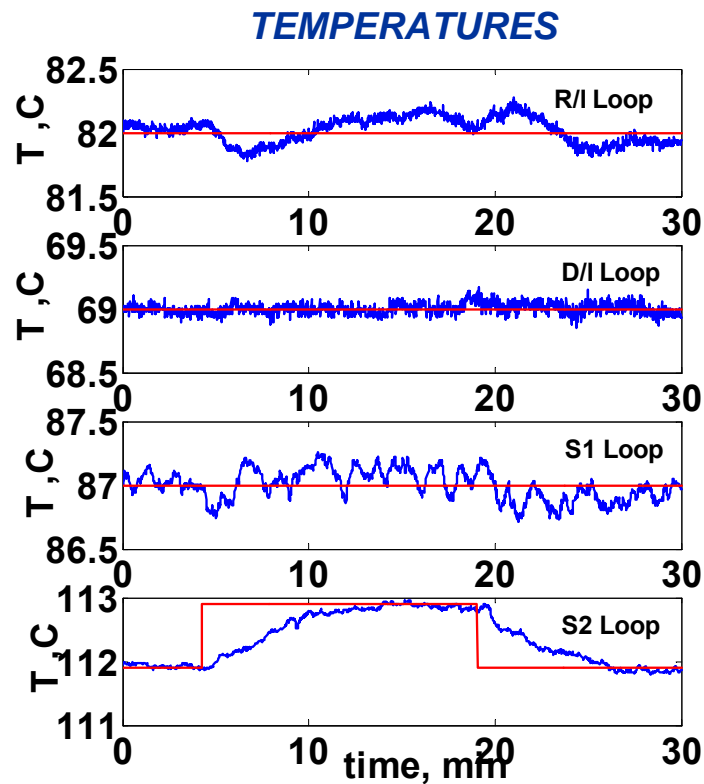
S1 Loop  $\pm 1$  C



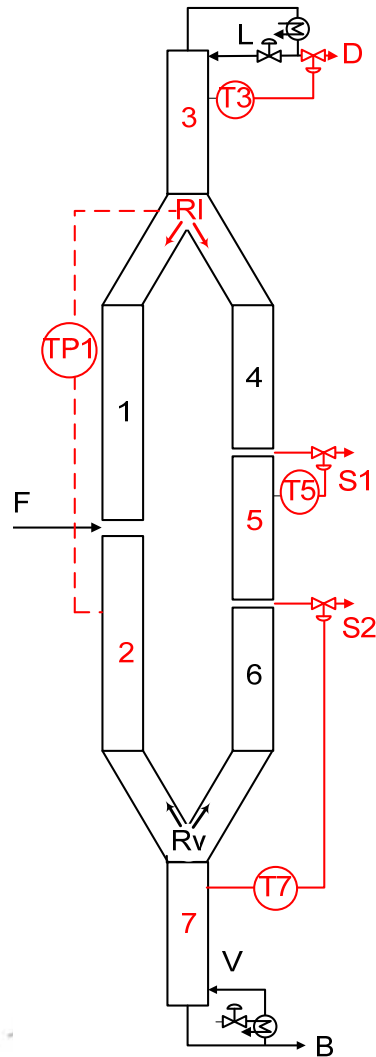
# Steady Profiles with 4 temperature loops..



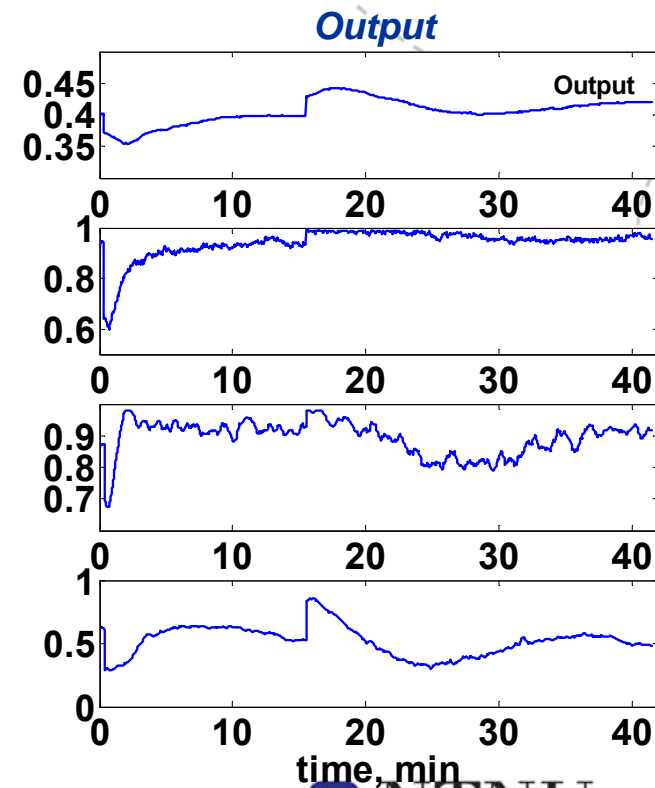
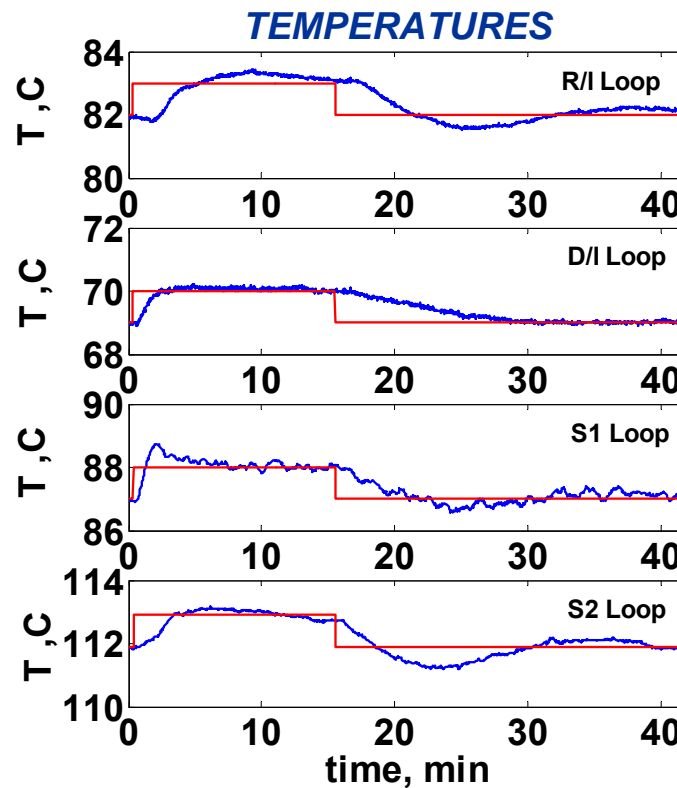
## S2 Loop $\pm 1$ C



# Steady Profiles with 4 temperature loops..



All Loops  $\pm 1$  C



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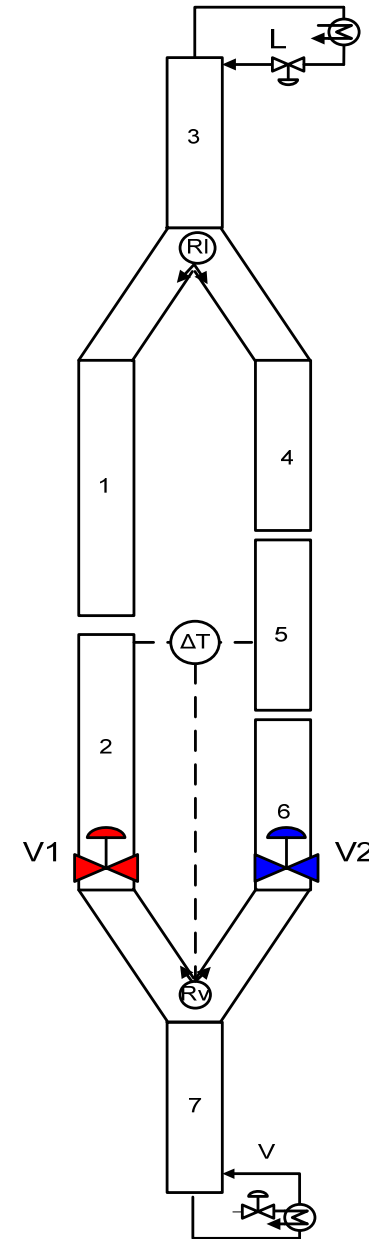
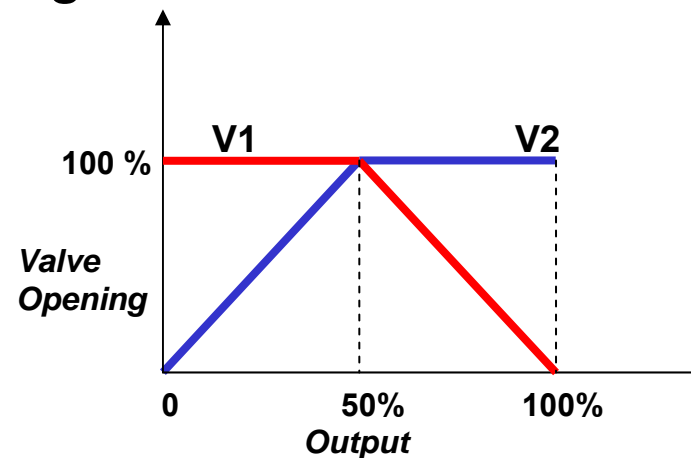
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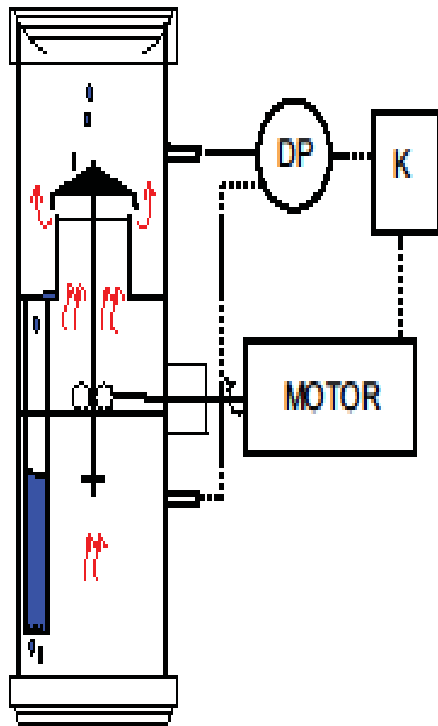
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# Vapor Split Experiment

- Total reflux operation
- Liquid Split Valve (R/I) in Manual
- Manipulated valve: Vapor Split Valve V1 & V2
- Controlled variable: T2-T5
- *Split Range logic*



# Vapor Split Experiment..



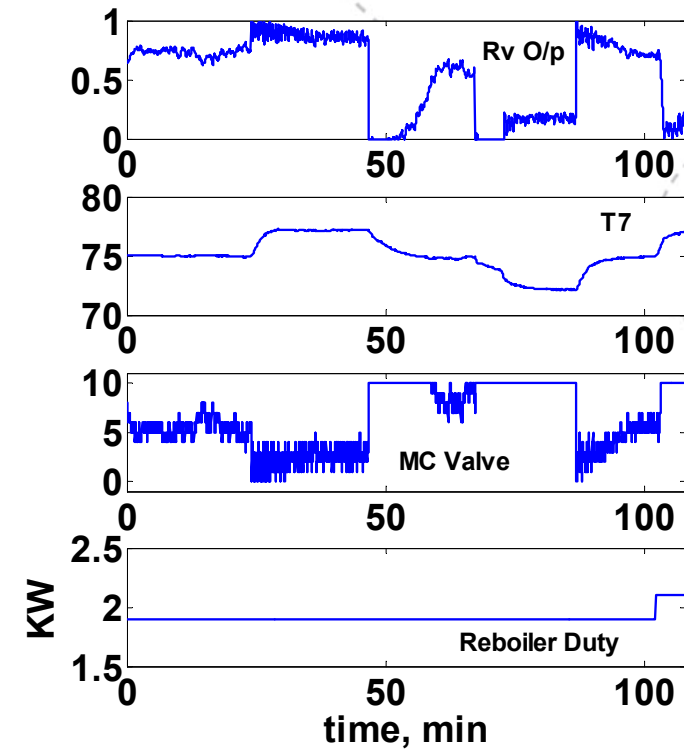
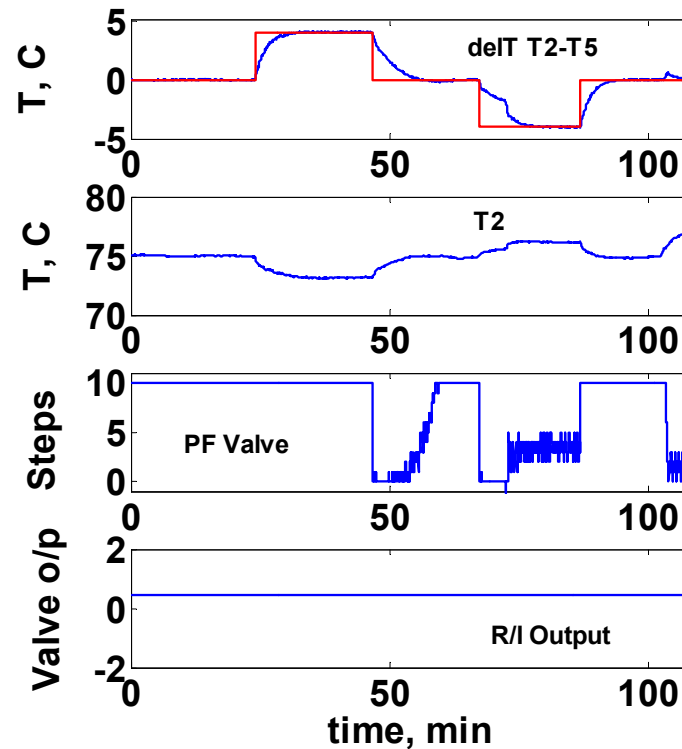
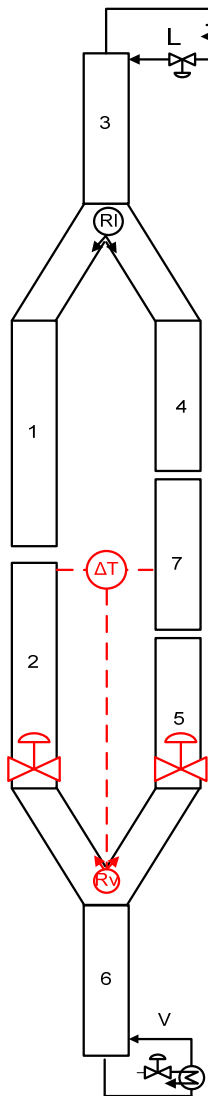
**Schematic of the vapor split valve**



**From top left: Valve in fully open position  
Top right: Rack and pinion arrangement.**

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# Vapor Split Experimental run (Total Reflux, two component)





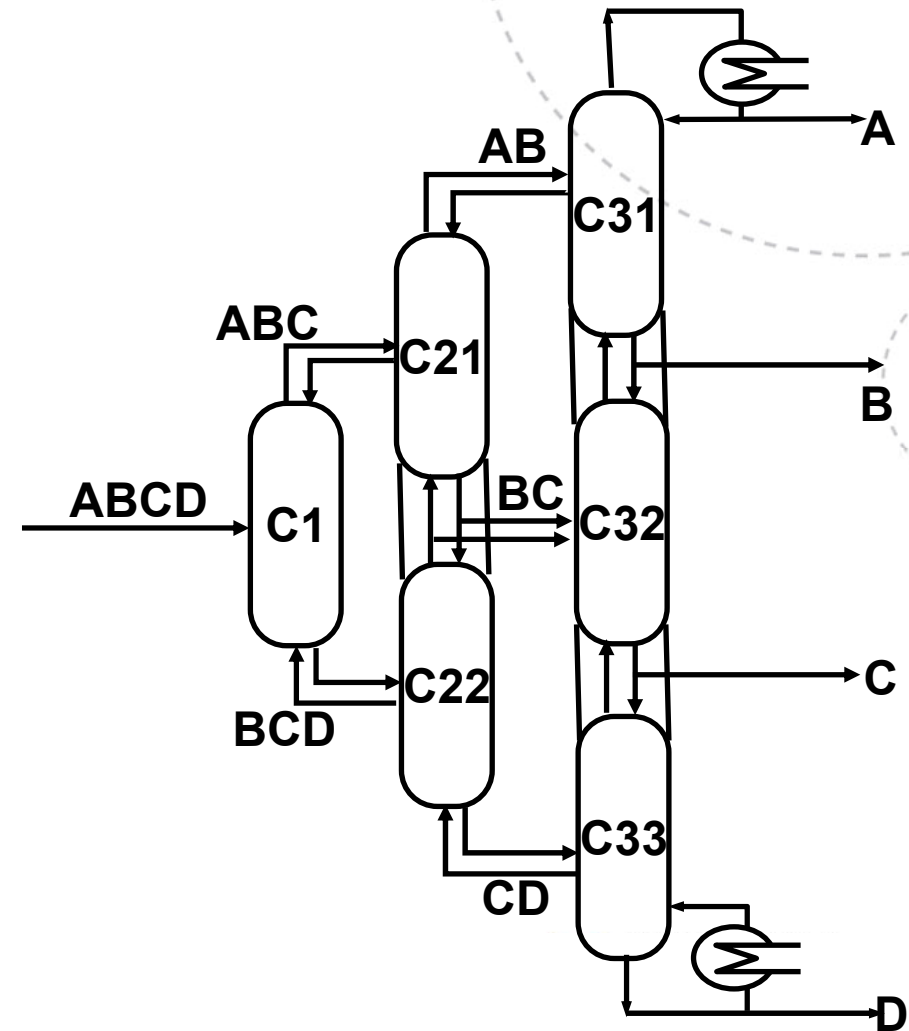
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# Petlyuk Arrangement- Model Details

## *Model Assumptions*

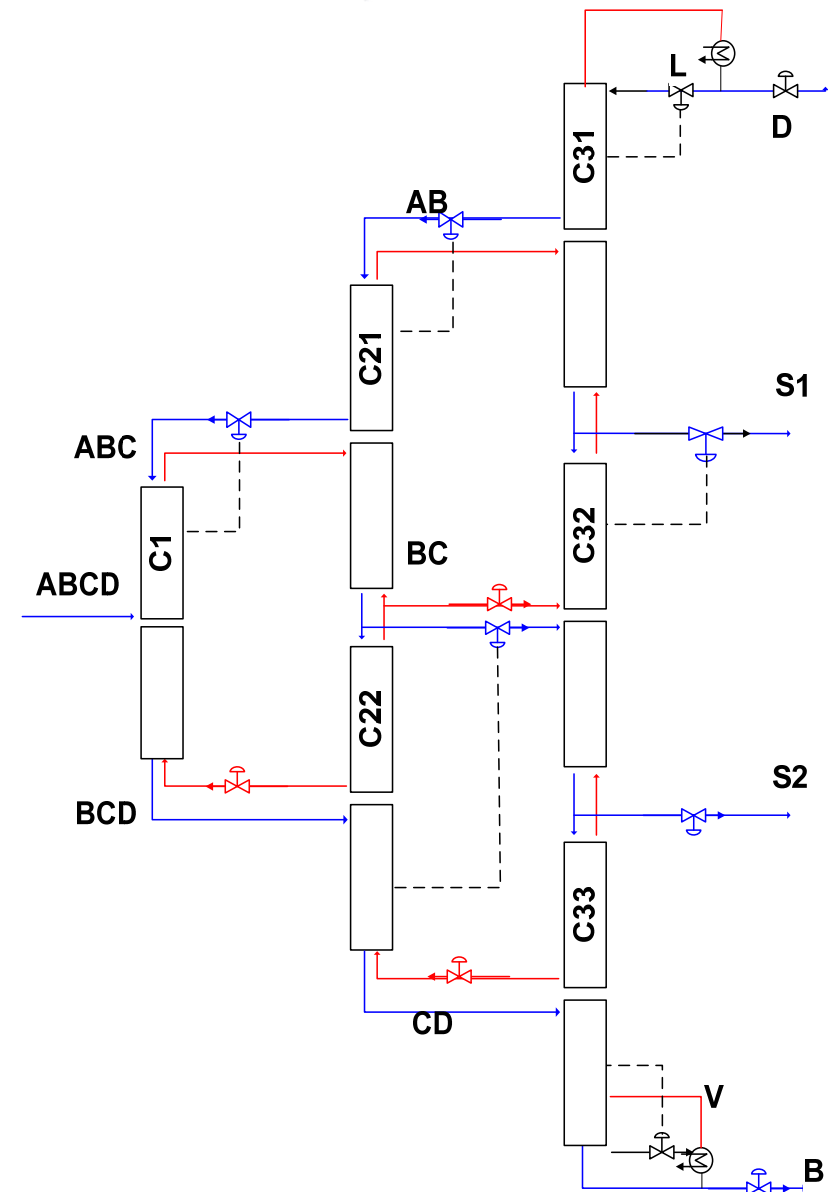
- Ideal vapor liquid equilibria
- 40 Theoretical stages in each column
- The base flows calculated from the  $V_{min}$  diagram\* which calculated the minimum



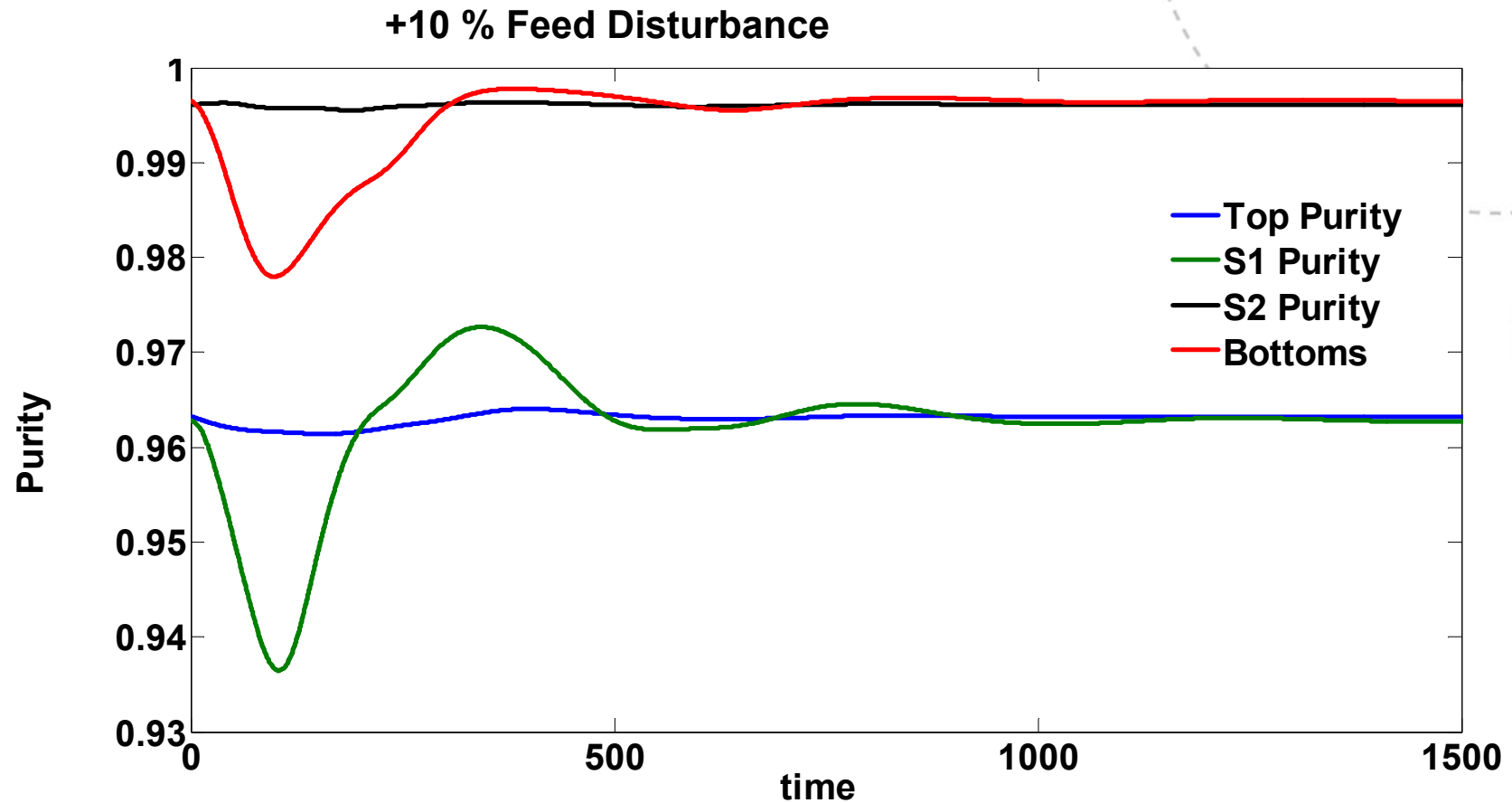
\* Halvosen, I.J. & Skogestad, S. (2003)

# Control Structure: Petlyuk Column

- Two Liquid Levels & 6 Sensitive Temperatures are CVs in Regulatory layer
- The loops were closed and tuned sequentially from left to right
- All loops tuned by the SIMC rules



# Close loop results: Petlyuk Column



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# Conclusion

- **4 – Product Kaibel Column**
  - **Experimental Studies Confirm Stable Profiles with 4 point temperature control**
  - **A lab scale prototype of vapor split valve effectively controlled vapor flow between prefractionator and main column**
  
- **4- Product Extended Petlyuk Column**
  - **Simulation studies suggest that 4-product extended petlyuk column can be controlled and operated with 6 point temperature control in the regulatory layer**

# Acknowledgements

- **Jens Strandberg for building the column**
- Prof Heinz Presig
- Dr Mohammad Shamsuzuhha
- Jon Anta Buljo Hansen
- Terje Mugaas
- Filip Voss

# References

- Halvorsen, I.J.; Skogestad, S; “Minimum Energy Consumption in Multicomponent Distillation. 3. More Than Three Products and Generalized Petlyuk Arrangements”, *Ind. Eng. Chem. Res.* 2003, 42, 616-629
- Kaibel, G. Distillation Columns with Vertical Partitions. *Chem. Eng. Technol.* 1987, 10, 92-98.
- Petlyuk, FB. Platonv, VM. Slavinskii, DM. (1965), Thermodynamically Optimal Methods for Separating Multicomponent Mixtures. *Int. Chem. Eng.* 1965, 5(3), 555.
- Strandberg, J., Skogestad, S., Stabilizing Operation of a 4-Product Integrated Kaibel Column. SYMPOSIUM SERIES NO. 152, Distillation & Absorption
- Ghadrdan, M., Halvorsen I.J., Skogestad, S., Optimal Operation of Kaibel Distillation Columns, *Chemical Engineering Research and Design* (2010), doi:10.1016/j.cherd.2011.02.007
- Kverland M, Halvorsen I.J., Skogestad. S,: Model Predictive Control of a Kaibel Distillation Column., *Proceed. of the 9th Intern. Symp. on Dynam. and Control of Process Systems (DYCOPS 2010)*
- Halvorsen, I.J., Skogestad, S. (2003) Minimum Energy Consumption in Multicomponent Distillation. 1. Vmin Diagram for a Two-Product Column, *Ind. Eng. Chem. Res.*, 2003, 42 (3), pp 596–604



**Thank you!!**